

Flow Chemistry Applications in Organic Synthesis

Jan. 24th, 2017

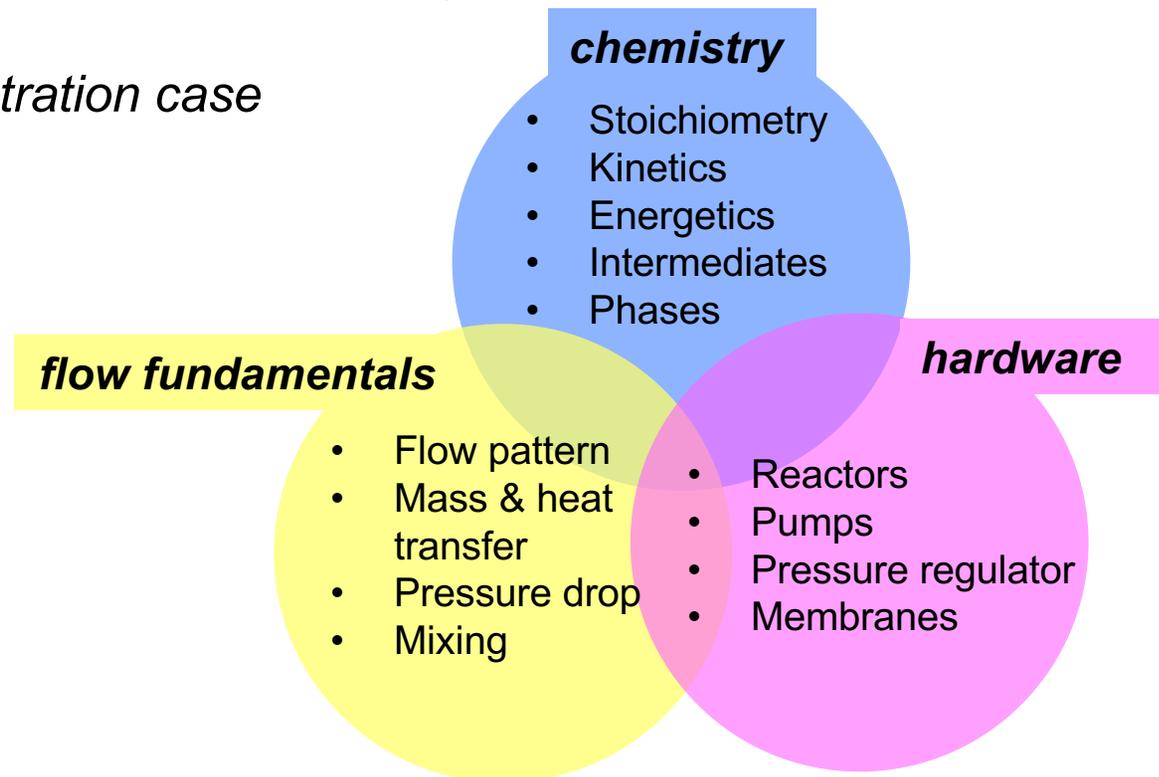
Malek Ibrahim

Group meeting

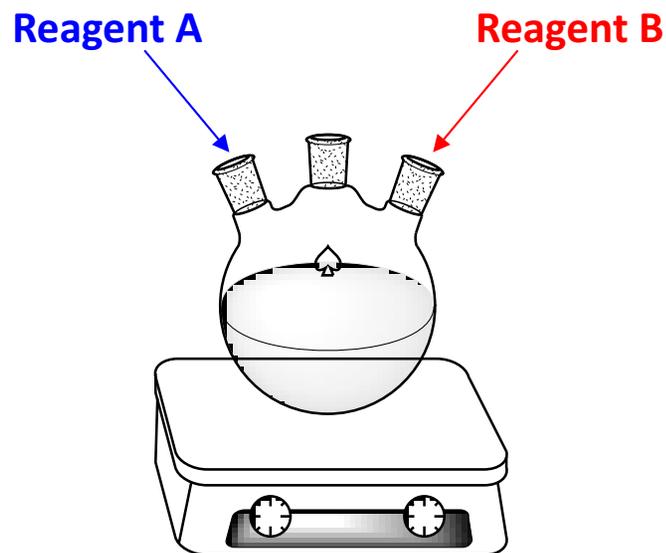


Outline

- *Batch vs. flow chemistry*
- *Advantages of flow chemistry*
- *Fundamentals of flow dynamics*
- *Pressure in flow chemistry*
- *Reactor Configurations*
 - *Tube-in tube gas reactor*
 - *Packed bed reactor*
 - *Microchannel reactor & Flash chemistry*
- *Solid handling*
- *Total synthesis demonstration case*



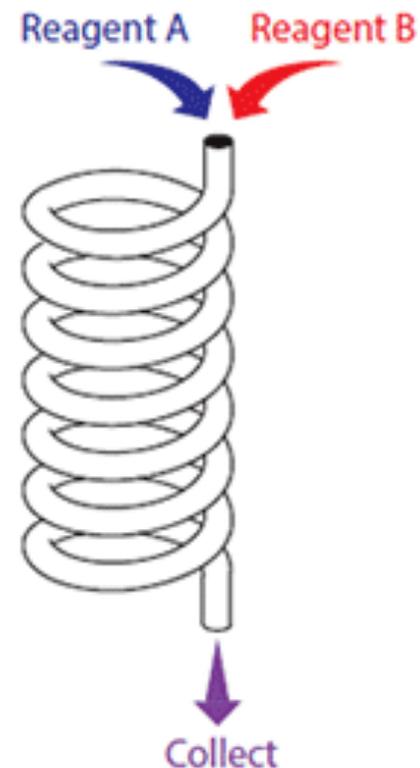
Batch vs. Flow Chemistry



Batch:

Instantaneous addition of reagents to a container (reactor) fitted with means of temperatures/pressure control and mixing

Mixing and conditions control are applied for the desired reaction time followed by workup

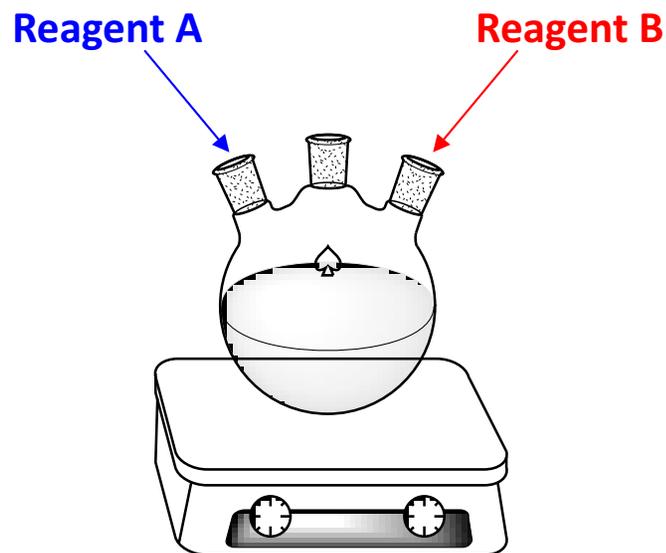


Flow:

Continuous addition of reagents to a reactor (tube, vessel, autoclave...) using pumps or compressors

Reaction time is the time the reaction medium spend inside the reactor (residence time)

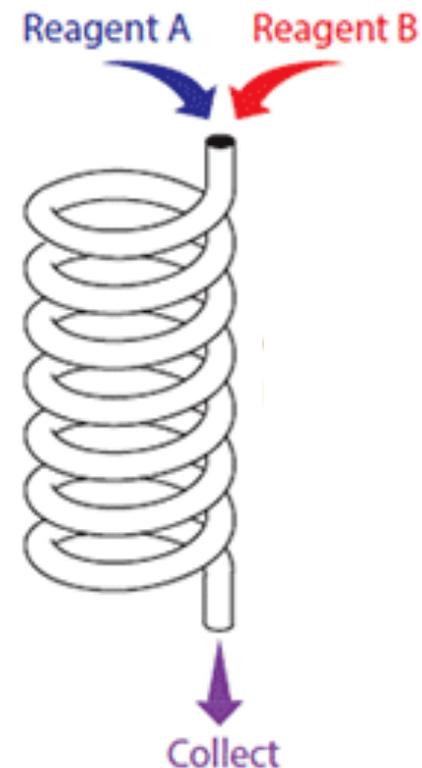
Batch vs. Flow Chemistry



Key factors:

- *mixing*
- *temperature*
- *time*

Variable parameters across time and space, unsteady state; concentration and temperature time gradient

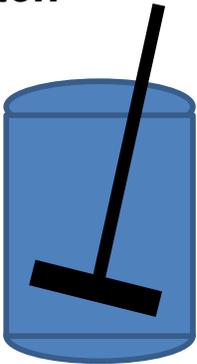


- *flow rate (or residence time)*
- *temperature*
- *pressure*

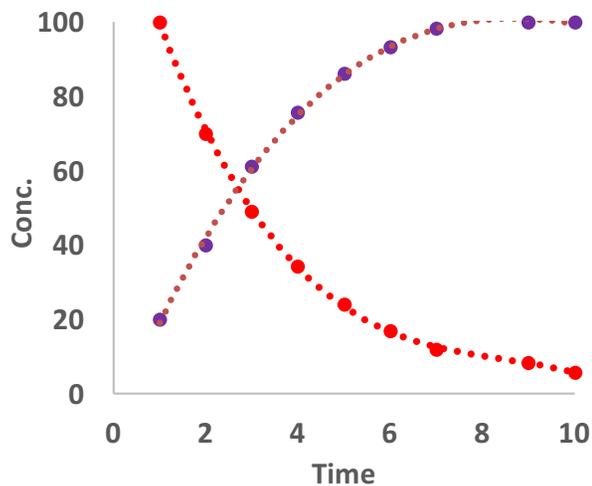
Steady state operation, constant parameters across reaction time, each molecule reacts under the same conditions

Reactor Models

Batch



- Variable concentration with time
- Variable reaction rate with time

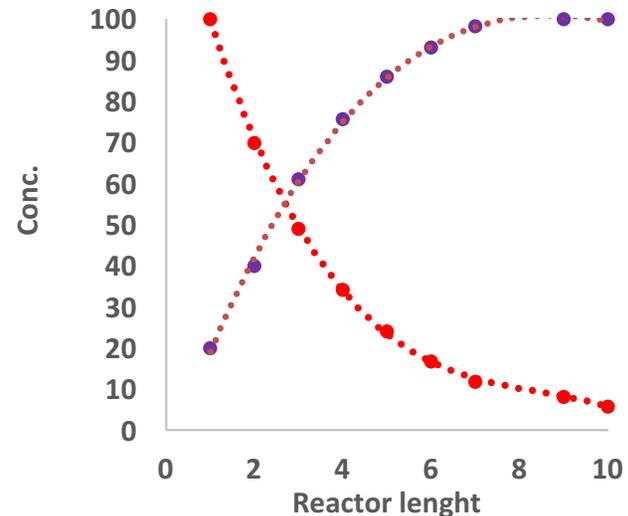


Plug flow reactor (tubular)

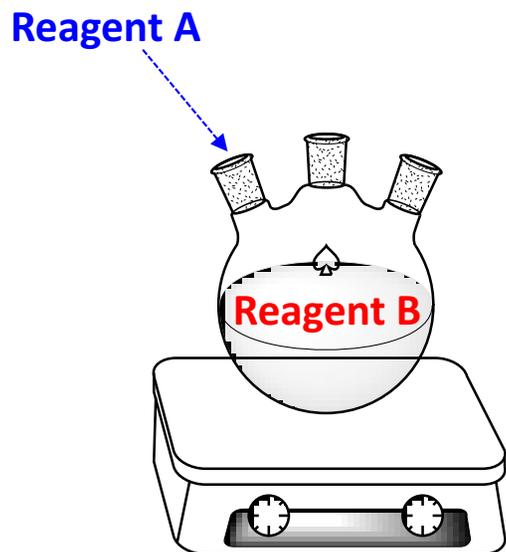


Plug Flow Reactor (tubular)

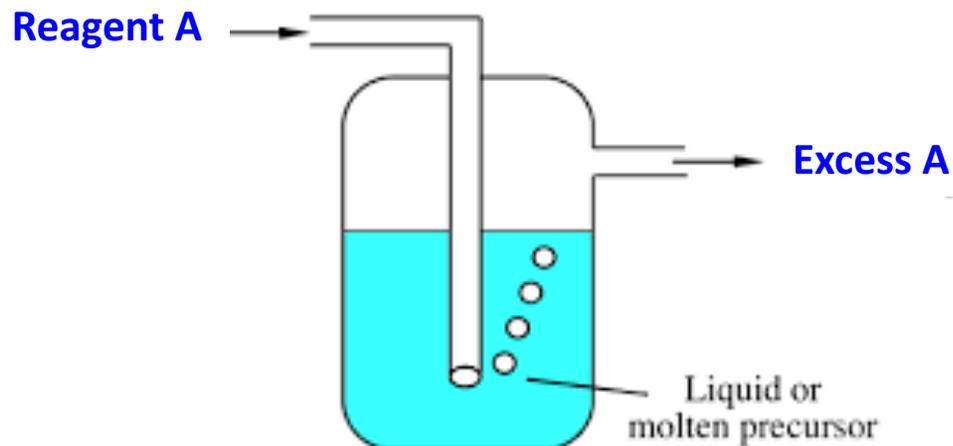
- Continuous flow
- Steady state
- Concentration changes across reactor length
- Neglects conc. gradient in axial direction and back mixing



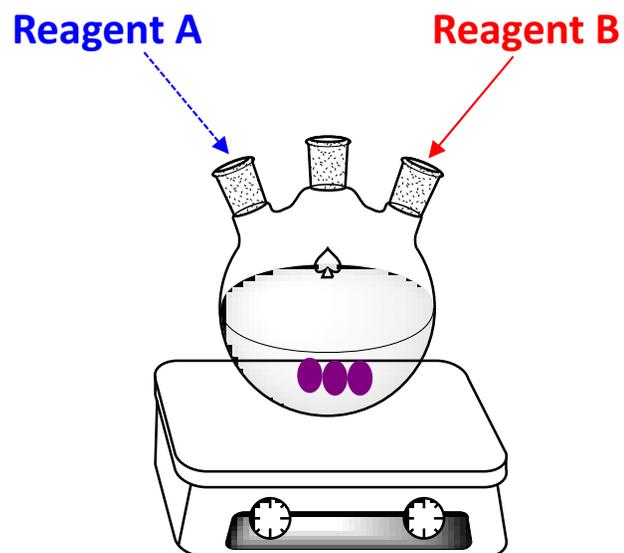
Special case: semi-batch chemistry



Slow liquid addition



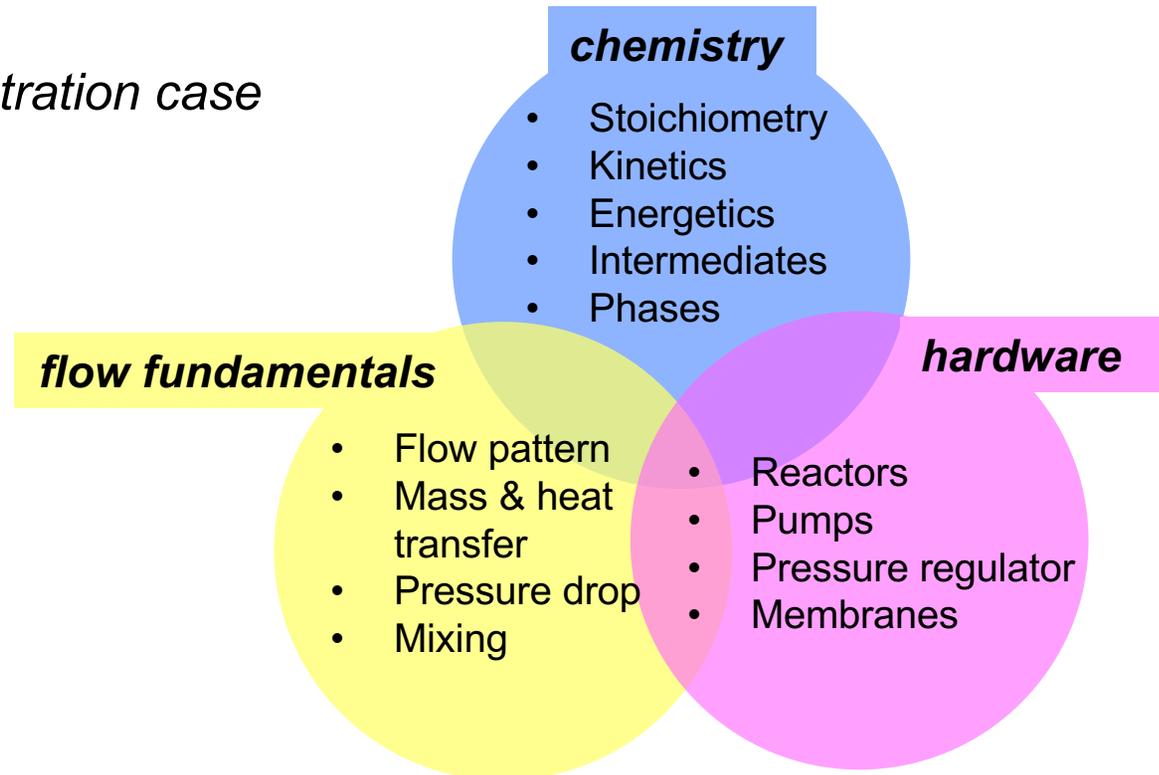
Gas bubbling



Slow solid dissolution or precipitation

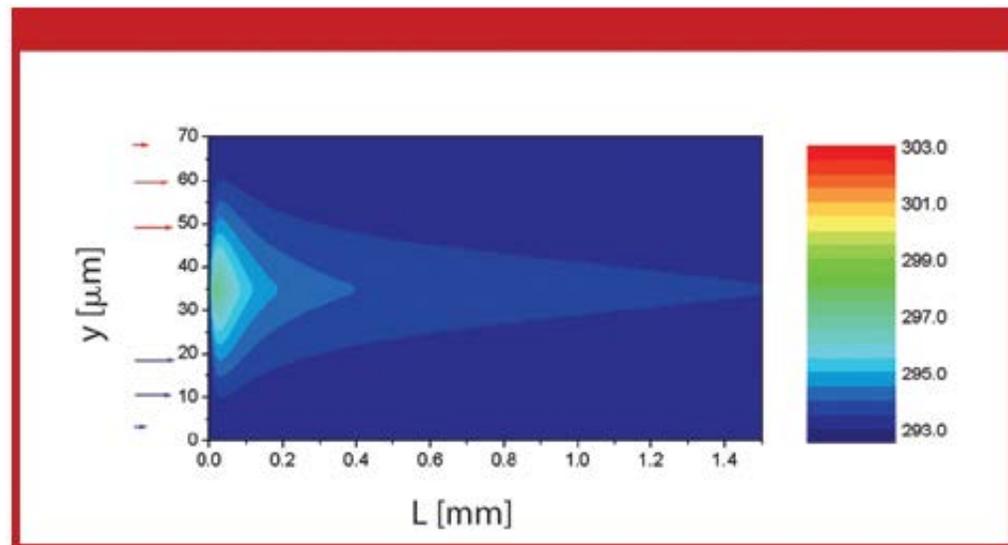
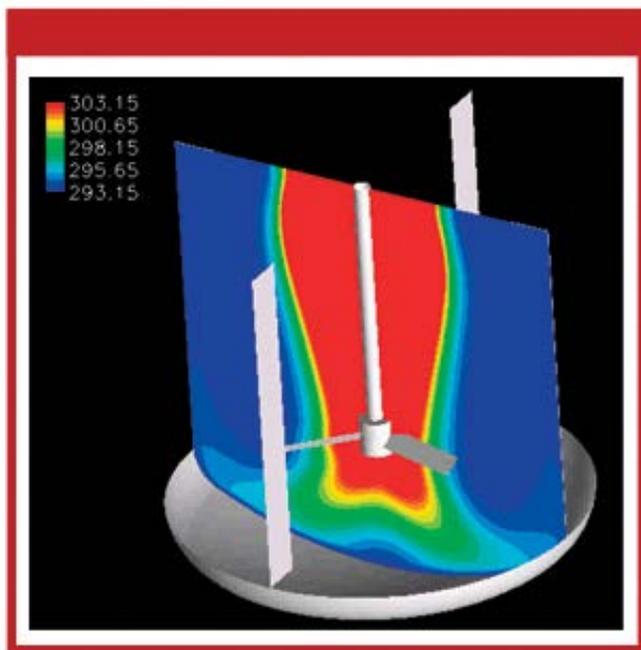
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- **Advantages of flow chemistry**
- *Fundamentals of flow dynamics*
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Advantages of flow chemistry

- Ionic liquid formation is highly exothermic
- Optimized batch operation had 10 °C gradient and yields brown product due to side reactions triggered by high temperature
- Enhanced mixing in PFR drastically mitigated the exothermic, less than 3 °C gradient

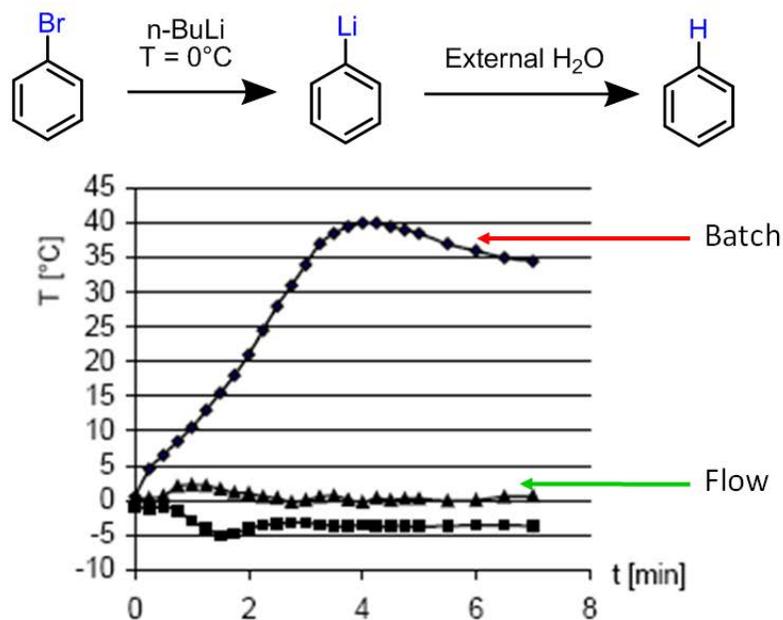


- Batch: <96% purity
- Plug Flow: >99% purity

Enhanced heat transfer: managing exothermic rxn

- Other exothermic reactions include lithiation, nitration, and ozonolysis
- Temperature runaway forms a safety and selectivity concern in these cases
- Lower than needed temperature ($-78\text{ }^{\circ}\text{C}$) is often applied to account for inefficient heat dissipation in batch mode

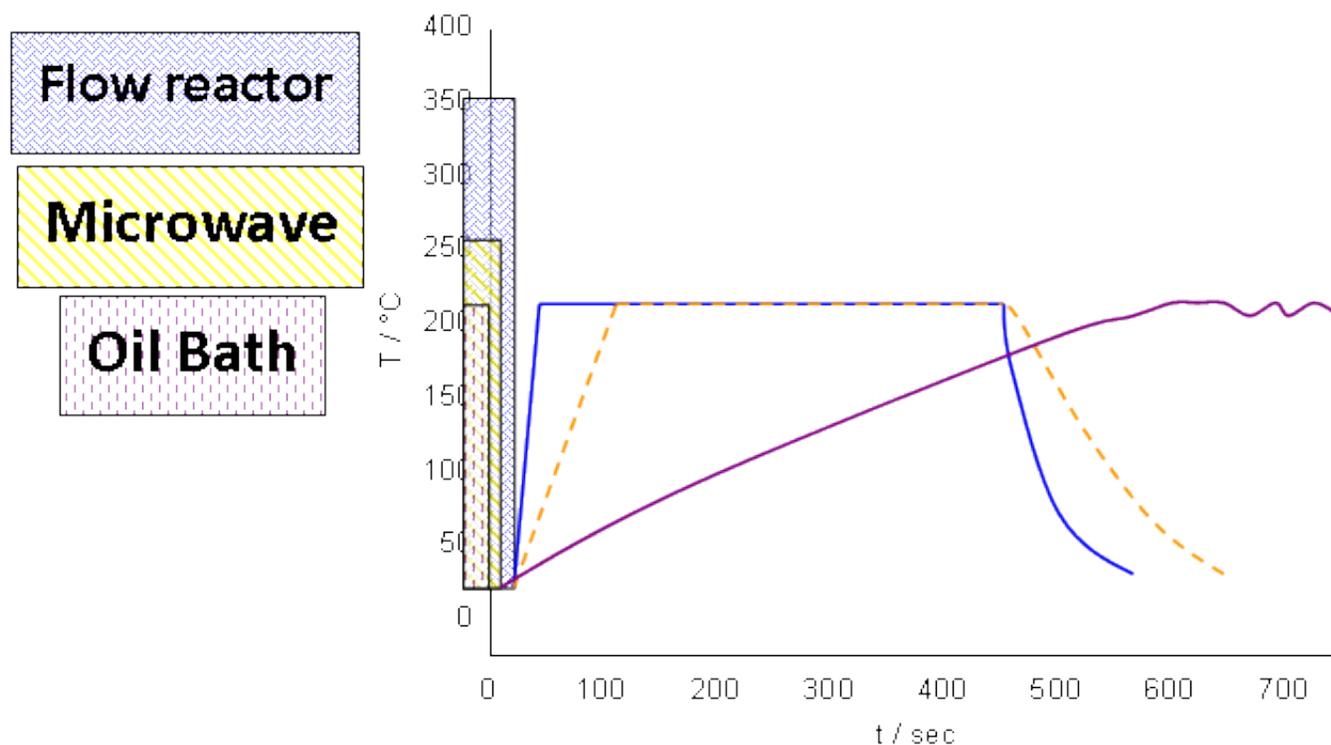
Heat out under batch and flow conditions



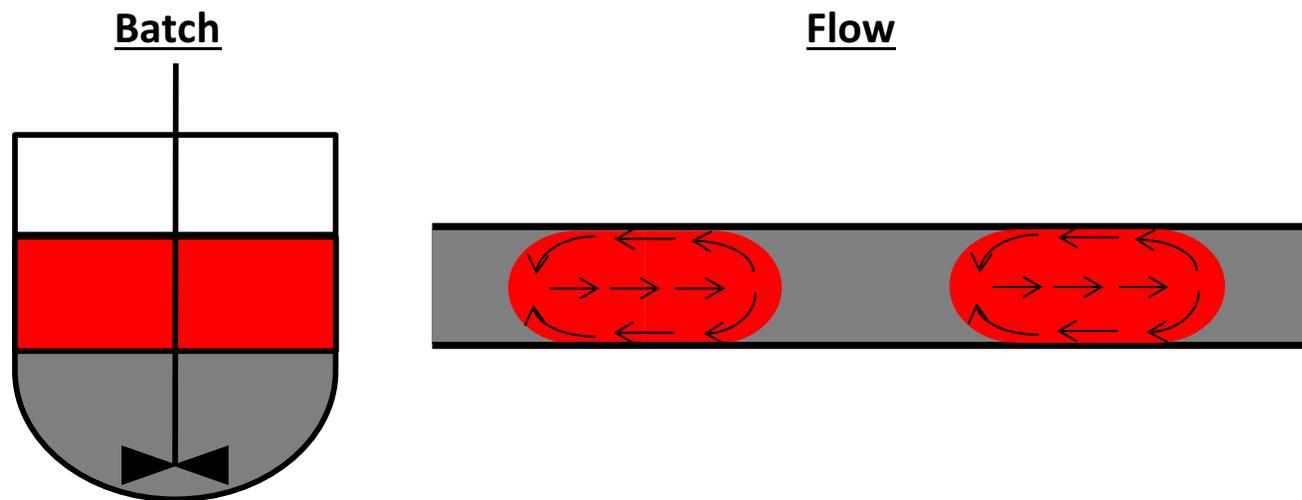
- Batch experiment shows temperature increase of 40°C .
- Flow shows little increase in temperature.

Temperature control

- Higher surface area/volume ratio in flow tubular reactor; better heat transfer
- Reactions cool down or heat up extremely rapidly (faster than a microwave)
- By pressurising, flow reactors can operate at temperatures above the typical boiling point of reactions
 - This enables easy superheating of reactions e.g. 100°C to 150°C above reflux temperatures



Biphasic reaction in batch vs. flow

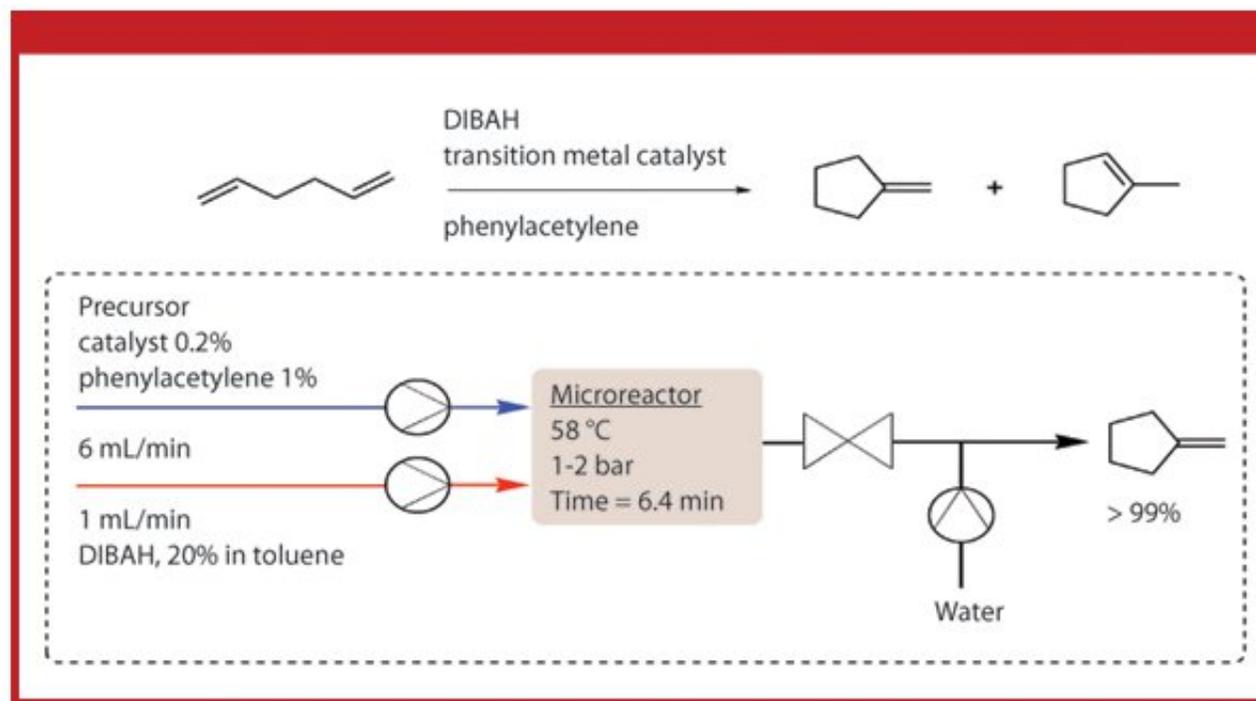


• Scaling	☹	☺
• Surface Area	☹	☺
• Gravity	✓	✗
• Mass transfer	☹	☺
• Emulsion	☹	☺

- Flow Chemistry is ideal for biphasic liquid reactions
- Flow Chemistry is very suitable for aqueous work-up

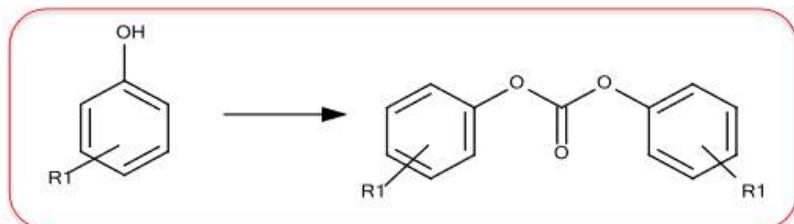
Pressure in flow chemistry

Ring closure in synthesizing exomethylenecyclopentane: advantage of additional pressure in flow chemistry



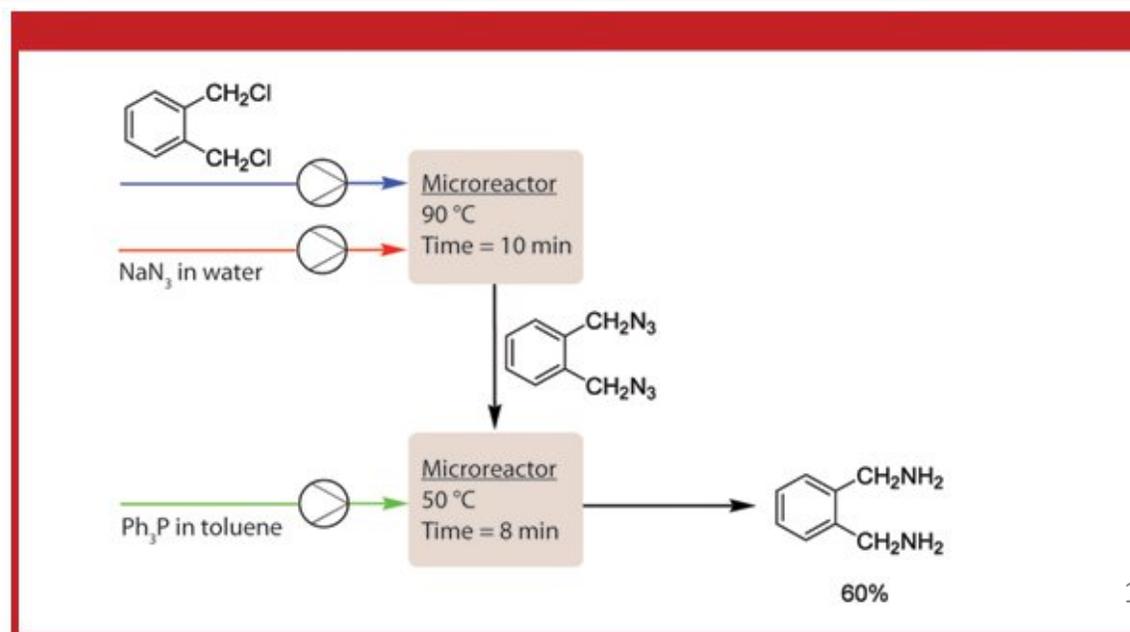
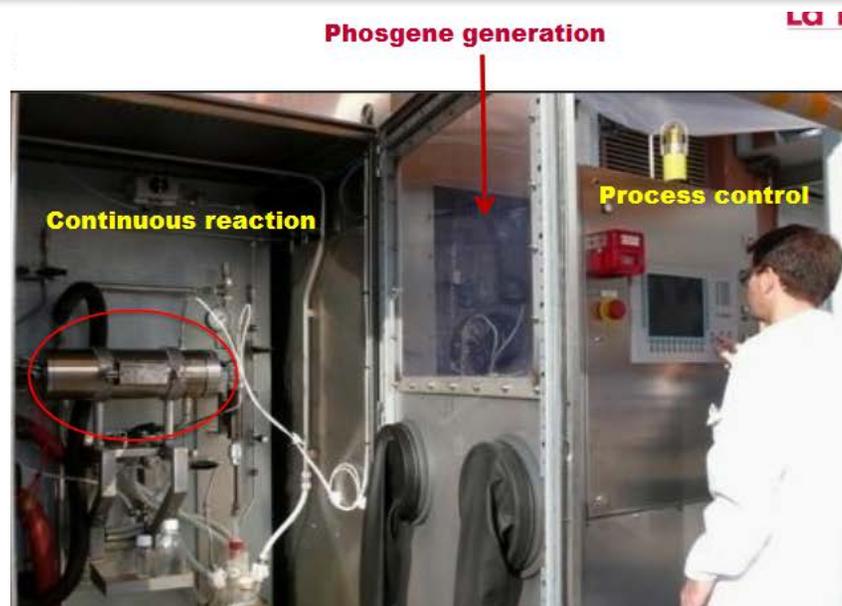
- Optimum operation temperature for catalyst activation is higher than s.m. boiling point (55 C at 1 atm)
- Pressurized higher temperature batch reactor gives a difficult to separate mixture of isomers
- Flow reaction under elevated pressure (2 bar) allows for smooth operation at >55 C >99% product selectivity at multikilogram scale

Handling dangerous reagents



Temperature	35-45°C
Pressure COCl ₂	0 bar
Phosgene Excess	5% mole
Residence Time	0.2min
Productivity	16 kg/h
Conversion	complete

<http://www.chemspeceurope.com>

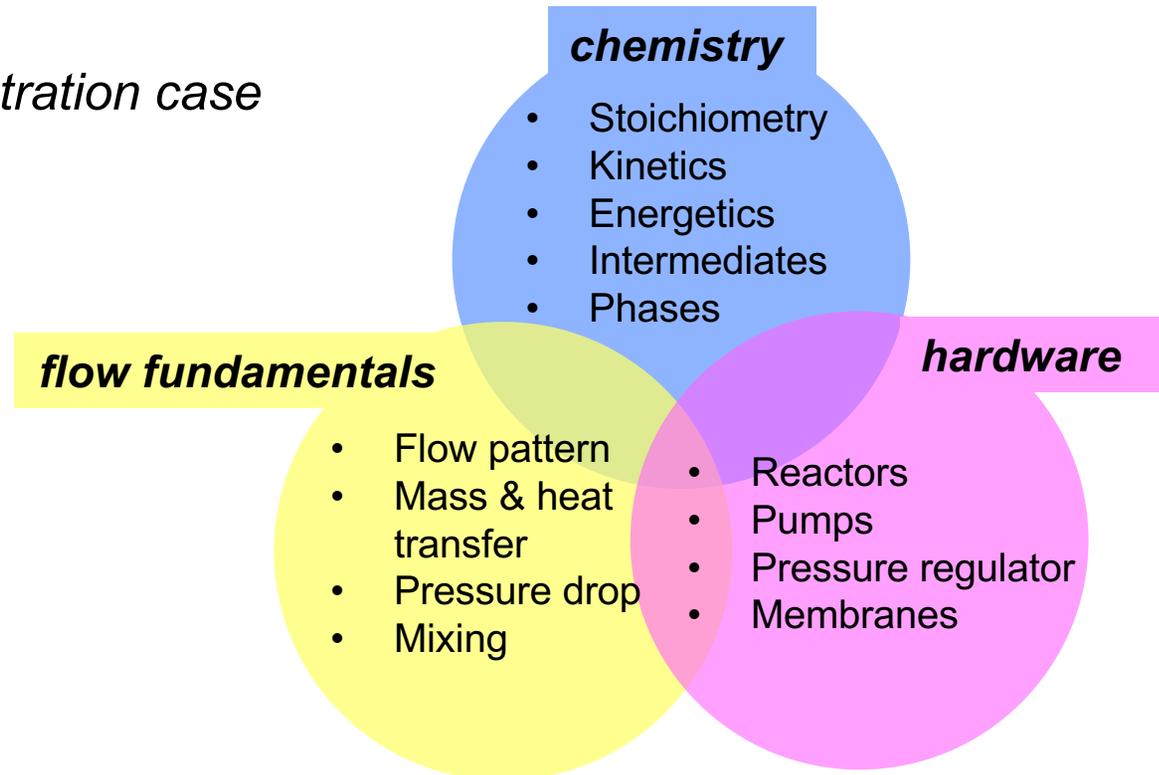


Advantages of flow chemistry

- Better mixing, enhanced heat and mass transfer
- Better conditions control
- Better reproducibility
- Easier automation
- Easier conditions screening & optimization
- Safer operation
- Quality control
- Less waste

Outline

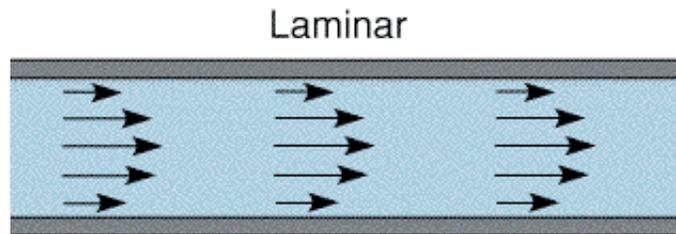
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Fluid Flow patterns: monophasic flow

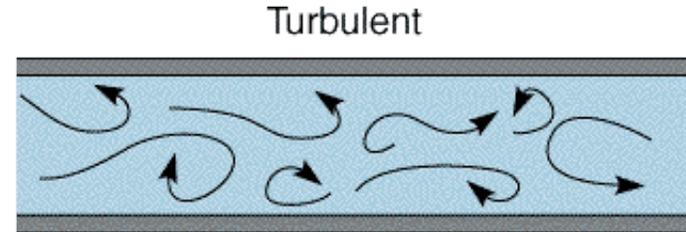
- Flow pattern depends on flow rate, density, viscosity and tube diameter
- Knowing flow pattern is essential for estimating pressure drop, and heat and mass transfer

Flow pattern can be determined from Reynold's number (dimensionless number) $Re = \frac{\rho V L}{\mu}$



$$Re < 2300$$

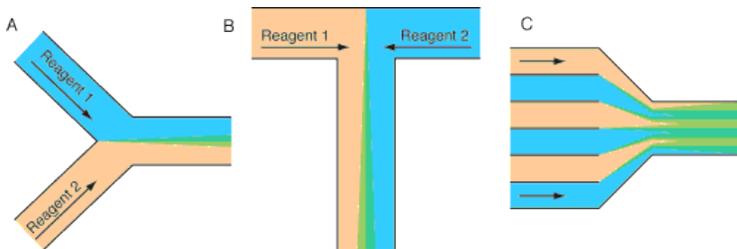
smooth, occurs when fluid flows in parallel lines, low velocity or high viscosity



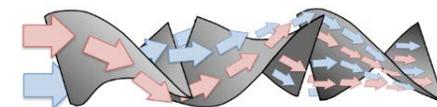
$$Re > 4000$$

Irregular, occurs when flow is characterized by eddies, high velocity

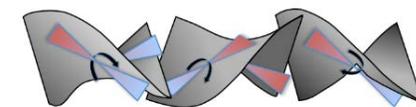
Mixing



Diffusion driven



Flow Division



Radial Mixing

Can be enhanced by static mixers

Factors affecting flow rate

$$\text{Residence Time} = \text{Reactor Volume} / \text{Flow Rate}$$

Residence time needs to be long enough to allow complete conversion, but...

- very low flow rate harms mixing and heat transfer efficiency
- very long reactor causes high pressure drop

Residence time, mixing and heat transfer, and pressure drop all need to be optimized to set flow rate and reactor dimensions for a system

Darcy's equation: $\Delta p = \lambda (l / d_h) (\rho v^2 / 2)$

Δp = pressure loss (Pa, N/m²)

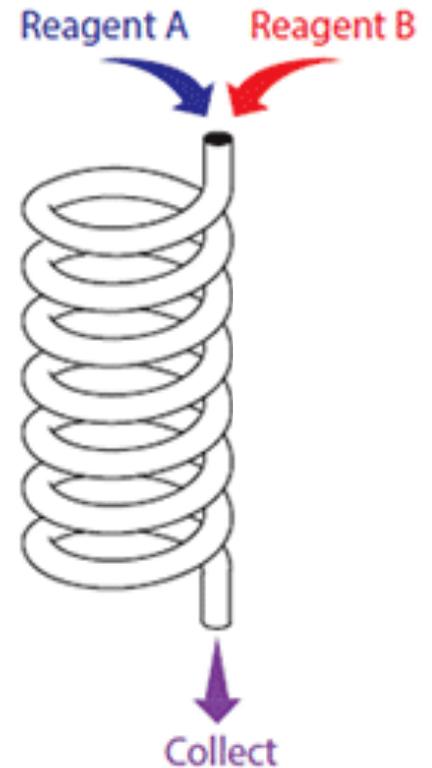
λ = Darcy friction factor

l = length of tube (m)

v = velocity (m/s)

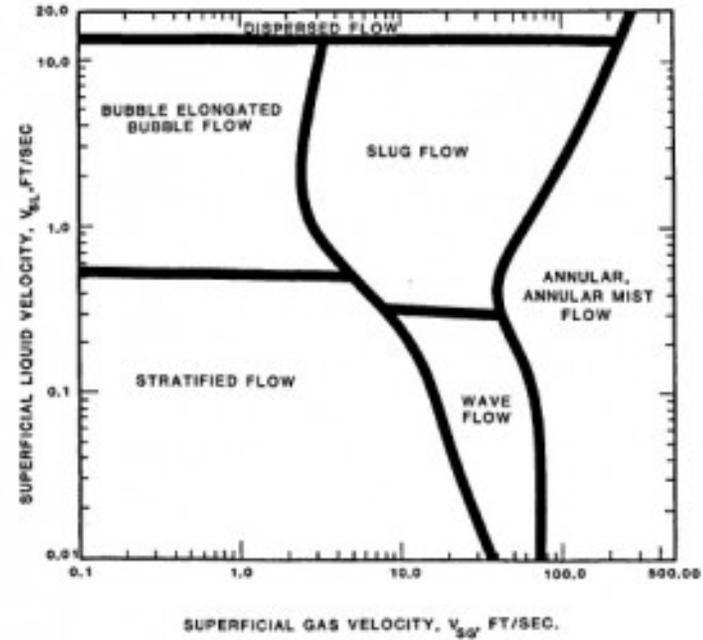
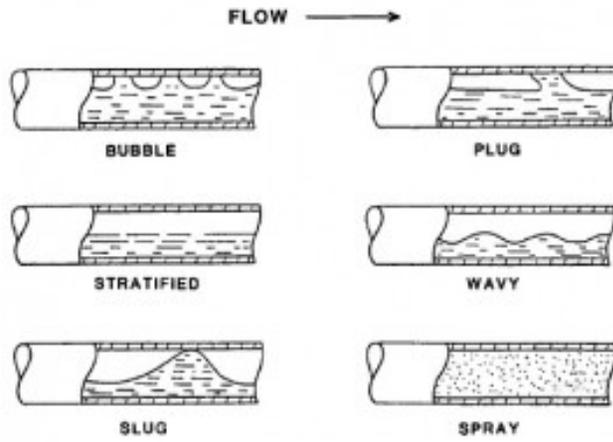
d_h = tube diameter (m)

ρ = density (kg/m³)

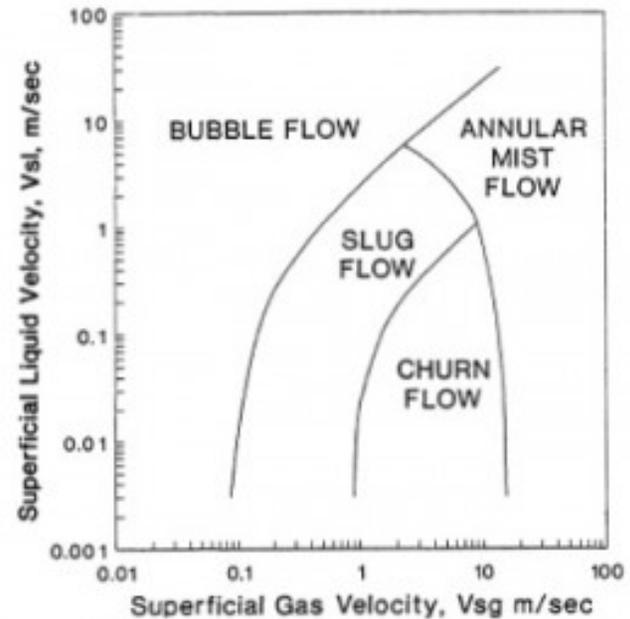
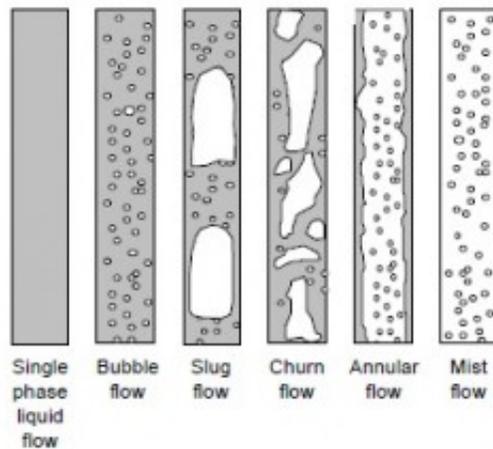


Fluid Flow patterns: biphasic flow

Horizontal pipe

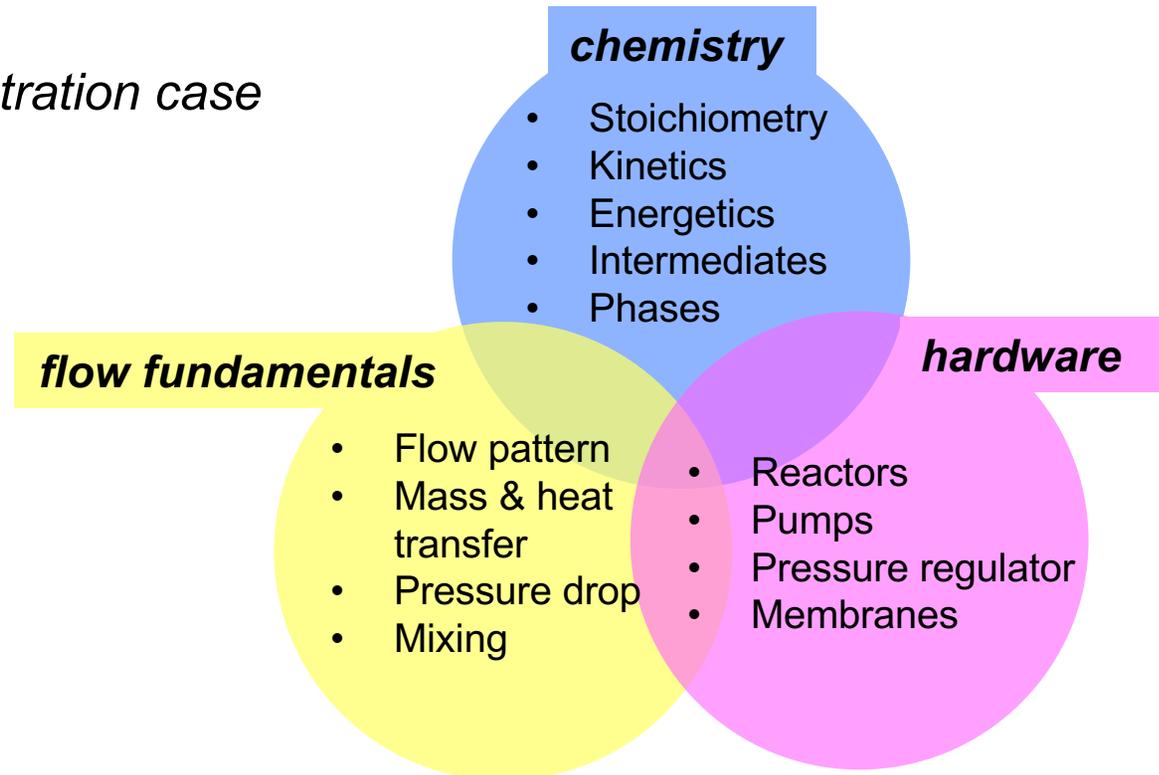


Vertical pipe



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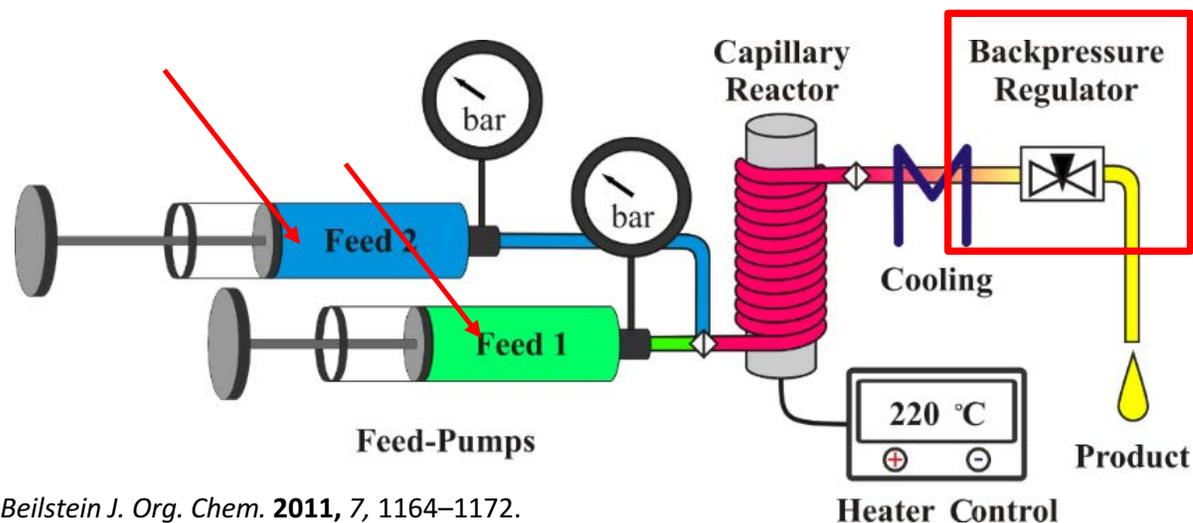
Pressure in flow chemistry

Pressure is needed to drive flow and overcome friction

Higher pressure can be applied to:

- prevent evaporation of volatile reagents
- operation above solvent bp
- enhance gas-liquid mixing
- increase gas residence time

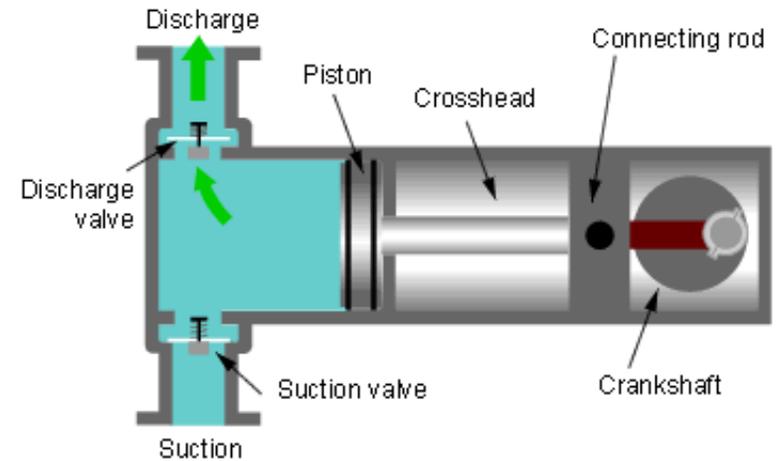
Pressure is provided through pumps or compressors and controlled via Back Pressure Regulator (bpr)



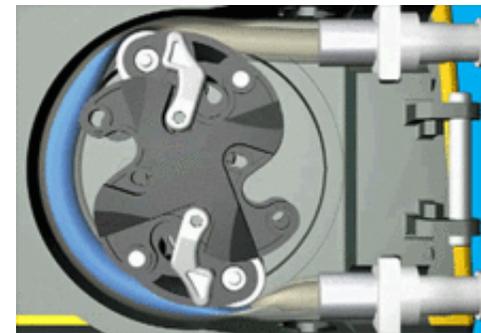
Pumps

Used to deliver reproducible quantities of solvents and reagents

- Reciprocating: single or dual acting
- Peristaltic pump
- Centrifugal pump
- Syringe pump



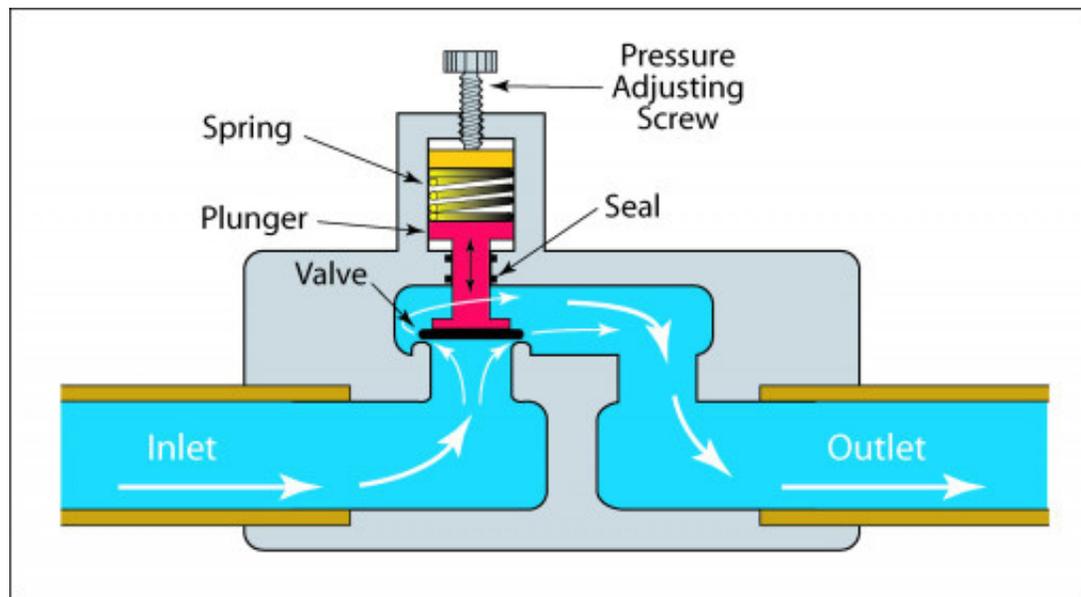
Pump selection depends on delivery pressure and material aggressiveness



Back Pressure Regulator

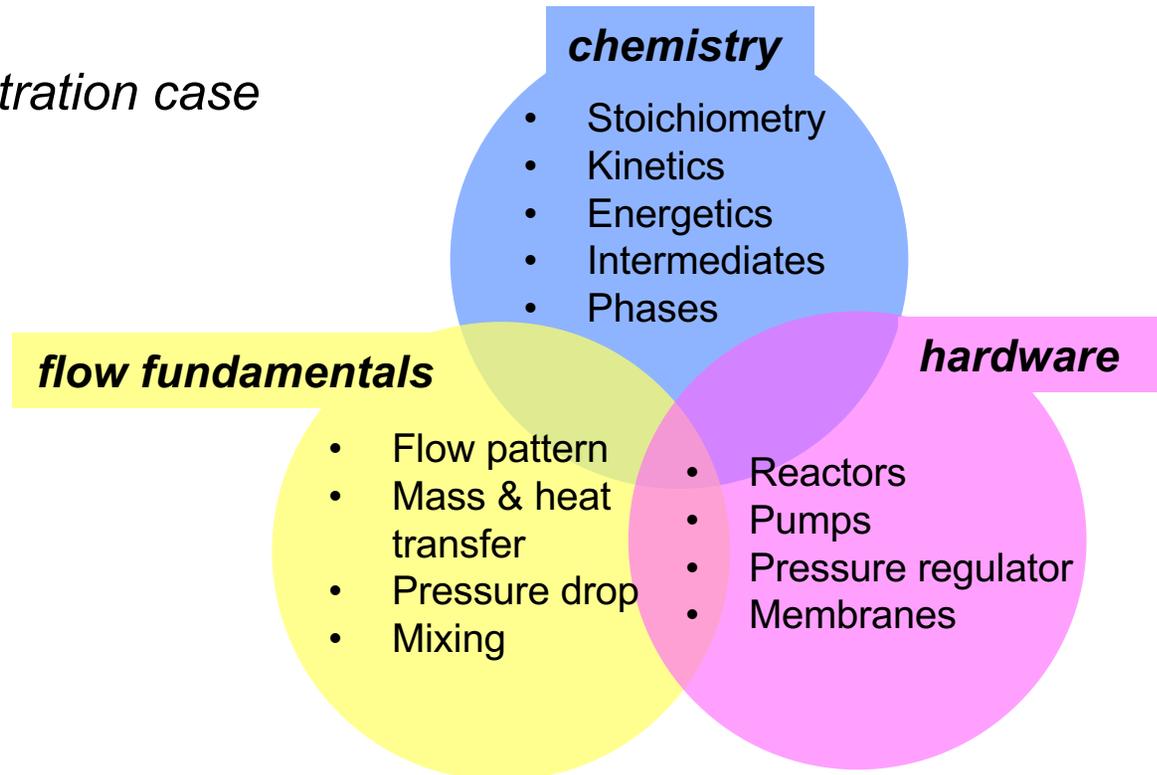
Unlike the more common pressure reducing regulators, the orifice opening of back pressure regulator is adjusted to control the inlet “upstream” pressure not the outlet

BPR can be controlled automatically to maintain constant pressure



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Design calculations

Help researcher B to design a tubular reactor for his chemistry:

- Flow rate 0.1 ml/min
- Fluid density 950 kg/m³, viscosity 0.92*10⁻³ Ns/m²
- Required residence time 5 min
- Knowing that researcher B wants to keep his flow turbulent for mass transfer reasons and has a pump with a maximum pressure delivery of 200 psi

Assume that pressure drop can be estimated $\Delta p = 0.01(v^2 (l / d))$

$$Re = \rho v d / \mu$$

Turbulent Re >4000

Δp = pressure loss psi

l = length of tube (m)

v = velocity (m/s)

d = tube diameter (m)

ρ = density (kg/m³)

μ = viscosity (Ns/m²)

Commercial bench scale flow Reactors



Gas reactor
(<http://www.cambridgereactordesign.com/>)



Trickle bed reactor
(<http://www.helgroup.com/>)



Microchip reactor unit
(<http://www.chemtrix.com/>)



Syringe pumps
(<http://syrris.com/>)



Gas reactor platform
(<http://www.thalesnano.com/>)



Reaction platform
(<http://www.uniqsis.com/>)



Cryogenic reactor unit
(<http://www.cambridgereactordesign.com/>)



Reaction platform
(<https://www.vapourtec.com/>)



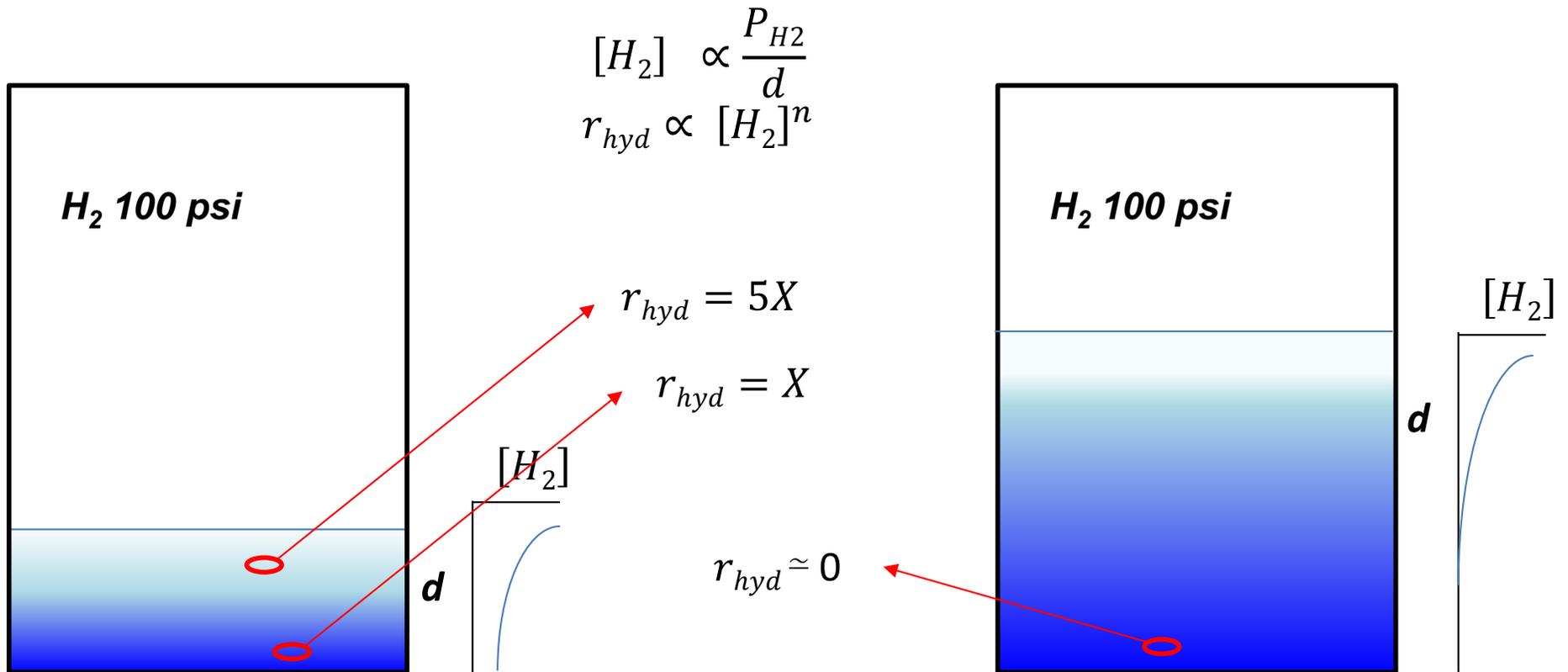
Reaction platform
(<http://www.amtechuk.com/>)

Rate of hydrogenation

...equals the rate at which the slowest step occurs

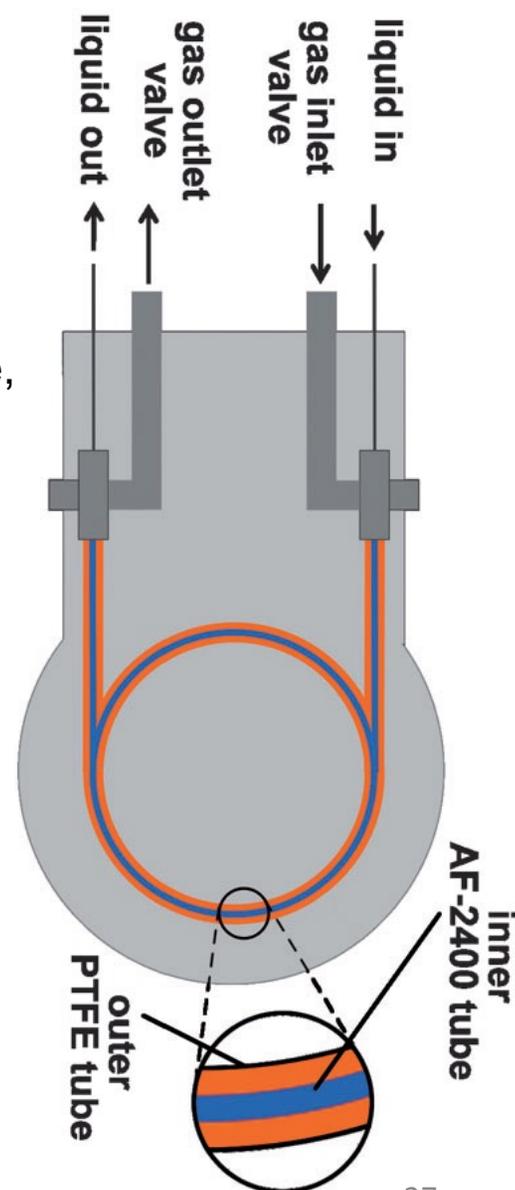
this step can be a chemical step (bond formation or breaking), or a mass transfer step.

In some cases the reaction can be limited by mass transport rendering the actual kinetics not relevant to the product formation rate



Gas Reactor: tube in tube with membrane

- Designed for enhanced gas-liquid mixing at minimum gas usage
- The inner tube is made of a gas-permeable material The membrane material needs to withstand swelling by solvent and chemical attack (silicon PDMS or Teflon AF 2400 membrane)
- The outer tube is made of a non-permeable rigid material
- Applications: ozone, hydrogen, carbon dioxide, carbon monoxide, ethylene, oxygen...

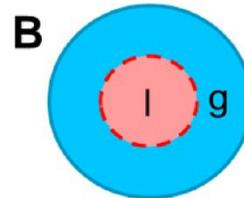
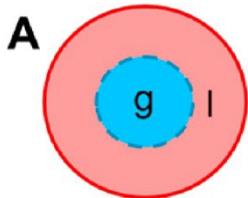


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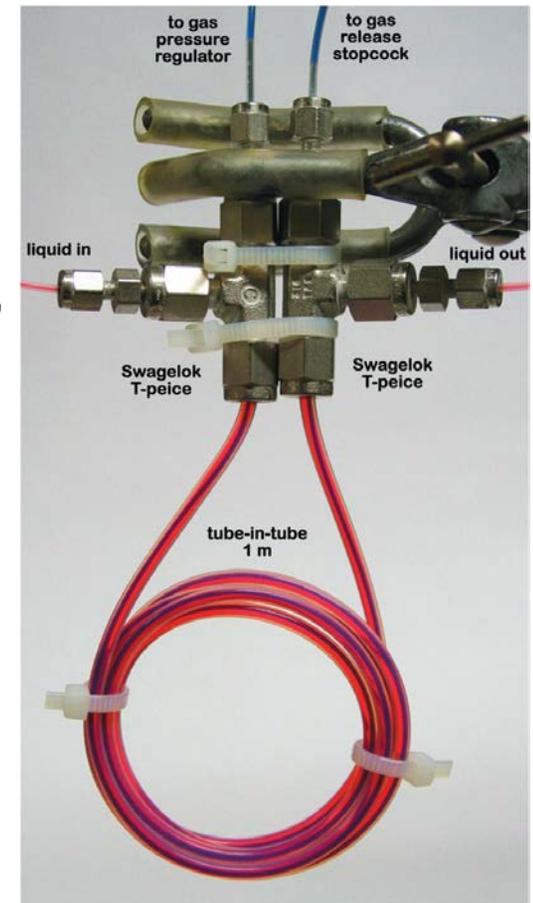
Four different flow configurations:

- Liquid flows through the inner or the outer tube
- Gas flows in the other tube co- or countercurrent with the liquid

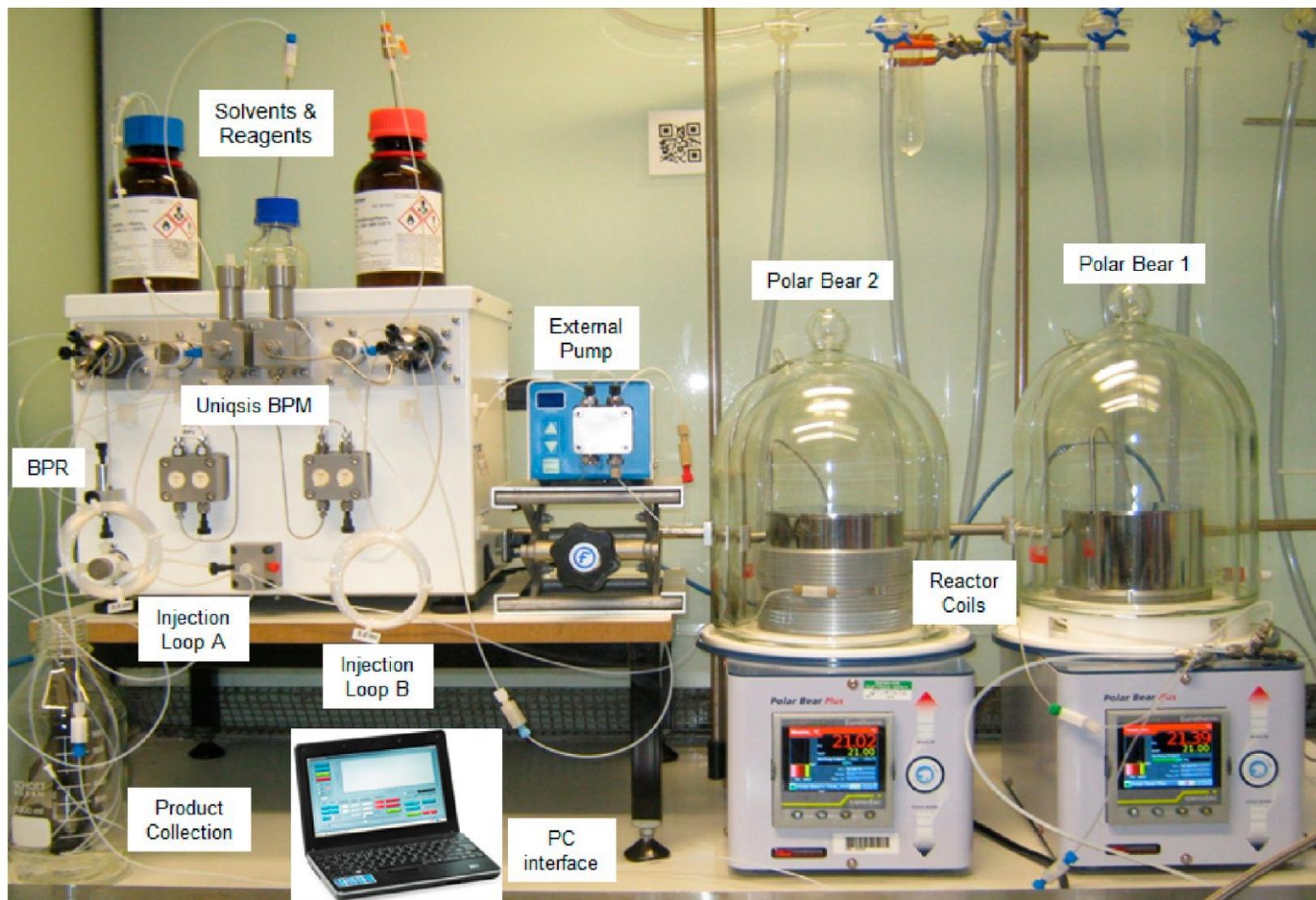


for 2 m length:

<p>volume of liquid = 2.45 cm³ volume of gas = 1.01 cm³ surface area of AF-2400 exposed to liquid = 62.83 cm² surface area of AF-2400 exposed to gas = 50.27 cm²</p>	<p>volume of liquid = 1.01 cm³ volume of gas = 2.45 cm³ surface area of AF-2400 exposed to liquid = 50.27 cm² surface area of AF-2400 exposed to gas = 62.83 cm²</p>
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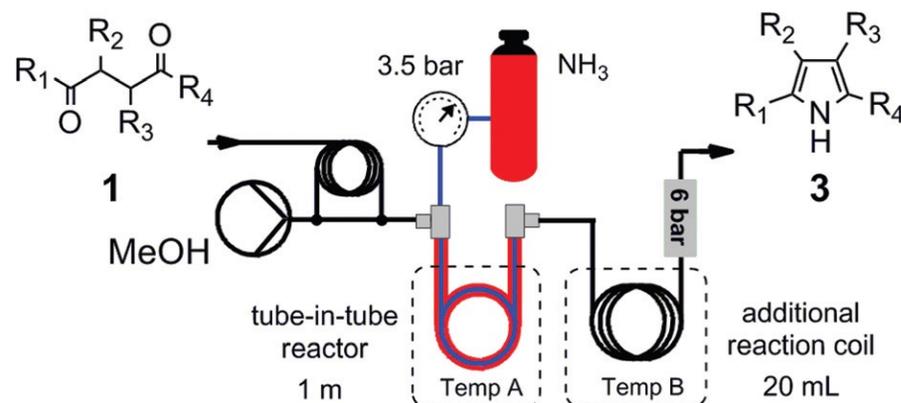
Gas Reactor: tube in tube with membrane



Tube in tube reactor: Teflon reactor for pyrrole synthesis

Paal-Knorr reaction of 1, 4 diketone with ammonia

- Volatility of ammonia makes heated batch reaction often not reproducible and inconvenient
- Gas flow through the inner membrane tube made of Teflon AF-2400
- High temperature is needed for reaction but low temperature is favoured for ammonia permeation
- Dual coil pressurized system



Entry	Temp A. ^a (°C)	Temp B. ^b (°C)	Flow rate (mL min ⁻¹)	Conversion ^c (%)
1	0	80	0.4	48
2	0	100	0.4	62
3	0	100	0.3	87
4	0	110	0.3	100
5	0	120	0.3	51 ^d
6	25	120	0.3	50

Tube in tube reactor: reaction with in-line purification

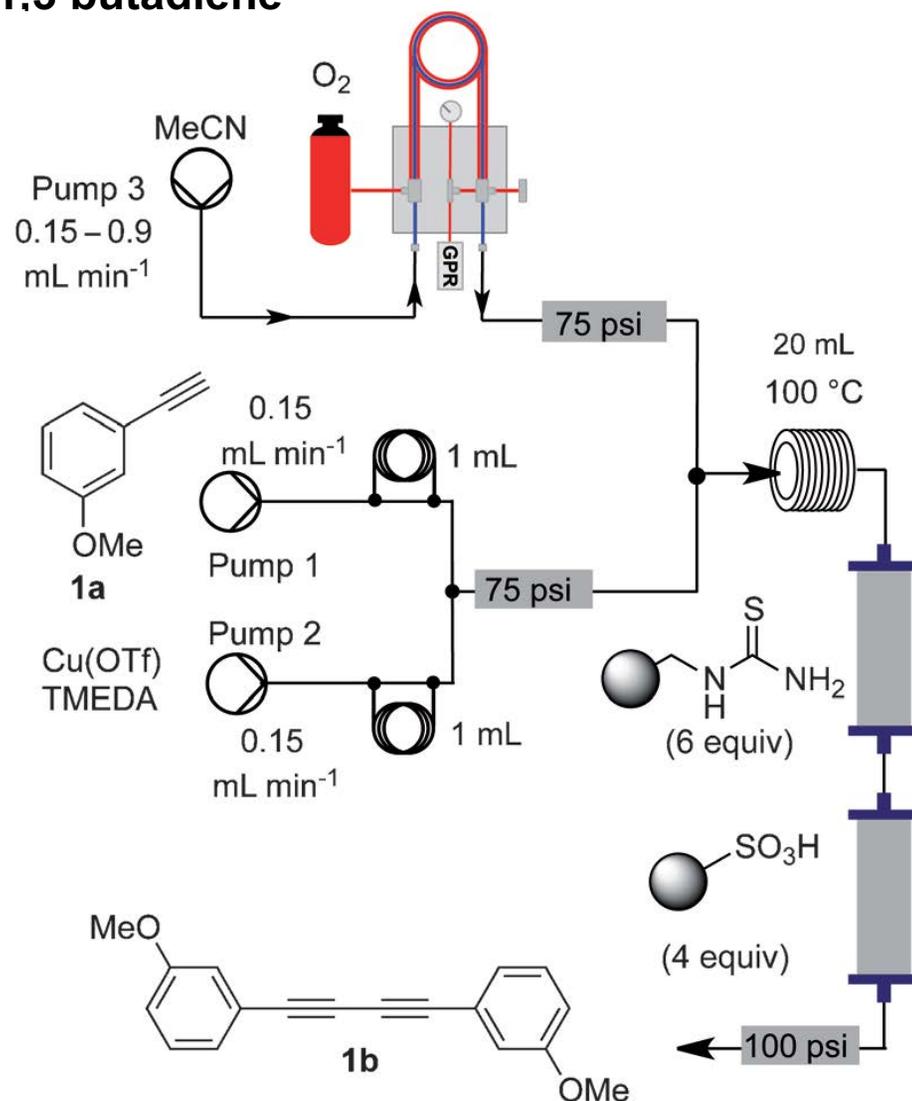
Oxygen assisted Glaser-Hey Coupling to afford 1.3 butadiene

- Three different injection pumps for substrate, catalyst, additive, and solvent
- Two different coiling at different temperatures for gas loading and reaction
- Two different packed columns downstream in series to remove catalyst and additive respectively

Table 1. Influence of reaction parameters on the Glaser-Hay coupling of 3-ethynyl anisole to afford 1.

Entry	<i>T</i> [°C]	<i>P</i> [bar]	Flow rate pump 1 [mL min ⁻¹]	Flow rate pump 2 [mL min ⁻¹]	Flow rate pump 3 [mL min ⁻¹]	Conv. ^[a] [%]
1	25	8	0.15	0.15	0.3	54
2	25	8	0.15	0.15	0.6	69
3	25	8	0.15	0.15	0.9	71
4	40	4	0.15	0.15	0.9	76
5	40	8	0.15	0.15	0.9	87
6	100	8	0.15	0.15	0.15	98
7	100	8	0.15	0.15	0.6	100

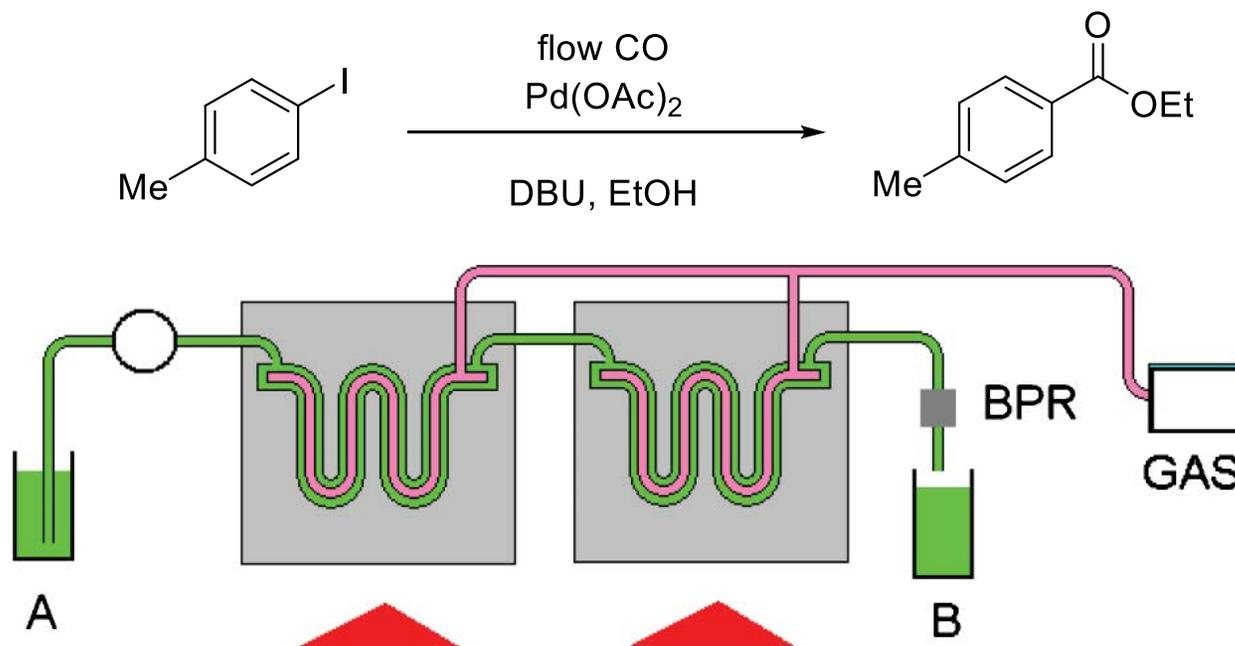
[a] Determined by ¹H NMR.



Tube in tube reactor: simultaneous gas and heat addition

Alkoxy carbonylation of aryl halide with CO at 120 °C

- Liquid flow in outer tube made of stainless steel for efficient heat supply and control
- Gas flow through the inner membrane tube
- Countercurrent flow of CO with two CO inlets at 180 psi allows for 97% yield with no excess CO being used
- Protocol was applied for other substrates and scaled up



Commercial bench scale flow Reactors



Gas reactor
(<http://www.cambridgereactordesign.com/>)



Trickle bed reactor
(<http://www.helgroup.com/>)



Microchip reactor unit
(<http://www.chemtrix.com/>)



Syringe pumps
(<http://syrris.com/>)



Gas reactor platform
(<http://www.thalesnano.com/>)



Reaction platform
(<http://www.uniqsis.com/>)



Cryogenic reactor unit
(<http://www.cambridgereactordesign.com/>)



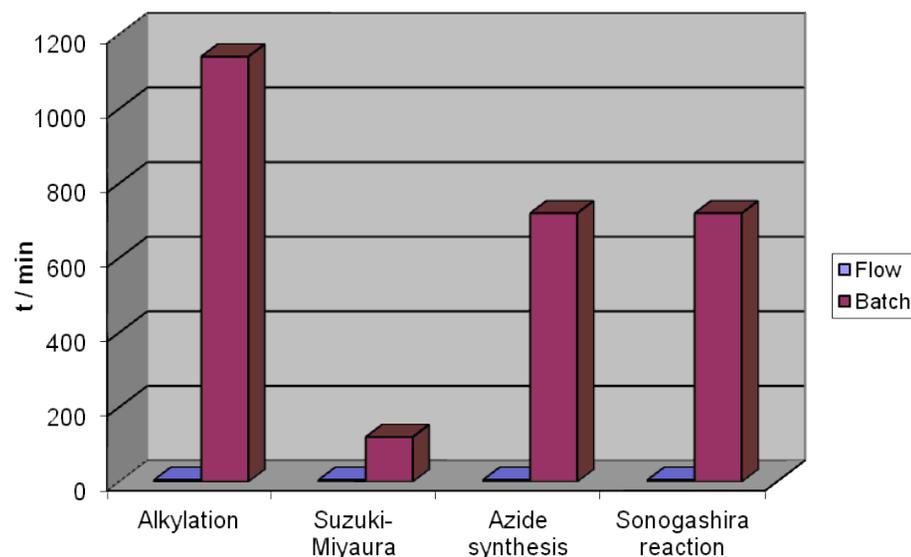
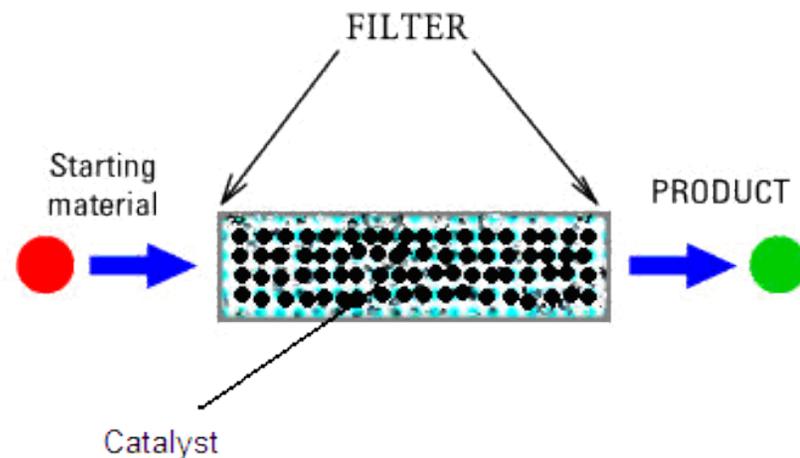
Reaction platform
(<https://www.vapourtec.com/>)



Reaction platform
(<http://www.amtechuk.com/>)

Packed bed reactor: solid-liquid reactions

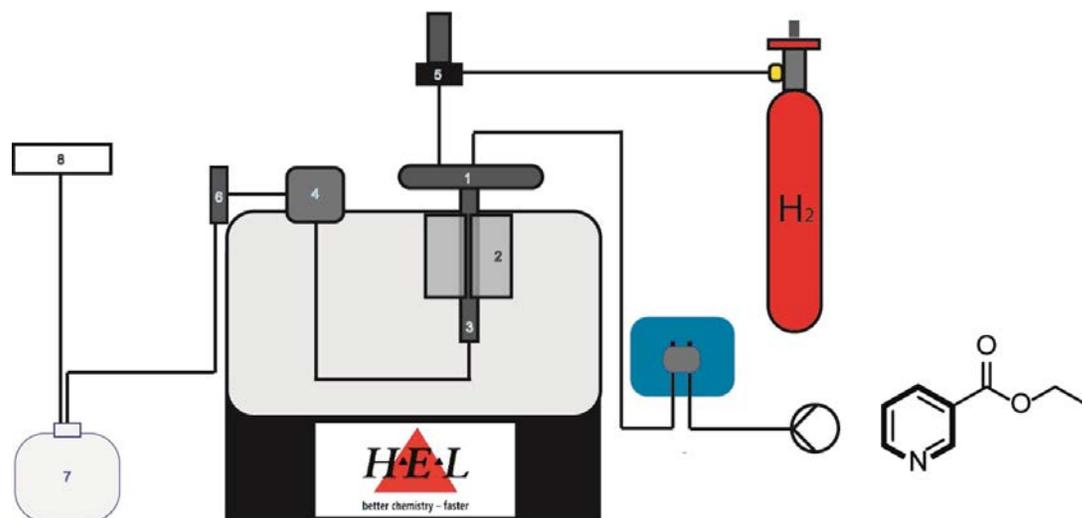
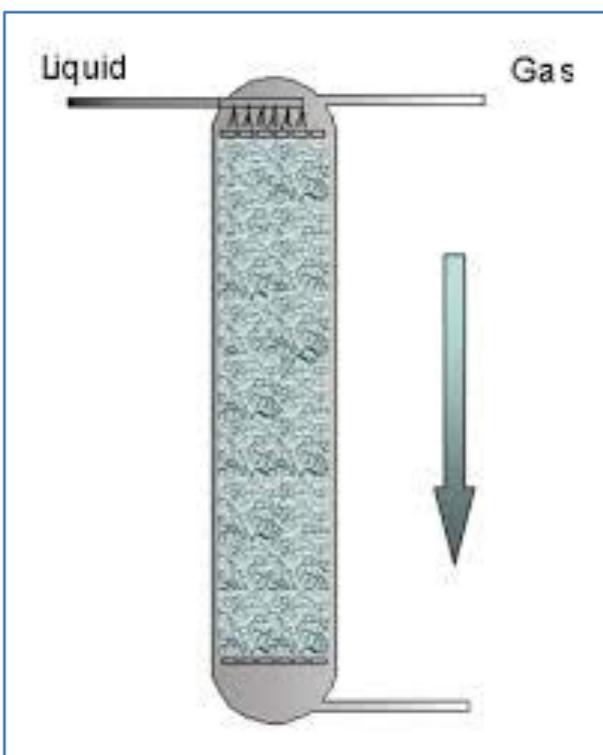
- Reactants flow through a fixed bed of solid heterogeneous/immobilized catalyst or reagent
- Much higher catalyst concentration when compared to batch for the same amount of catalyst
- Forcing the fluid reagent to flow through catalyst particles drastically enhances catalyst/reactant mixing
- Increase in rates by orders of magnitude
- Shorter reaction time, less temperature or catalyst loading can be achieved



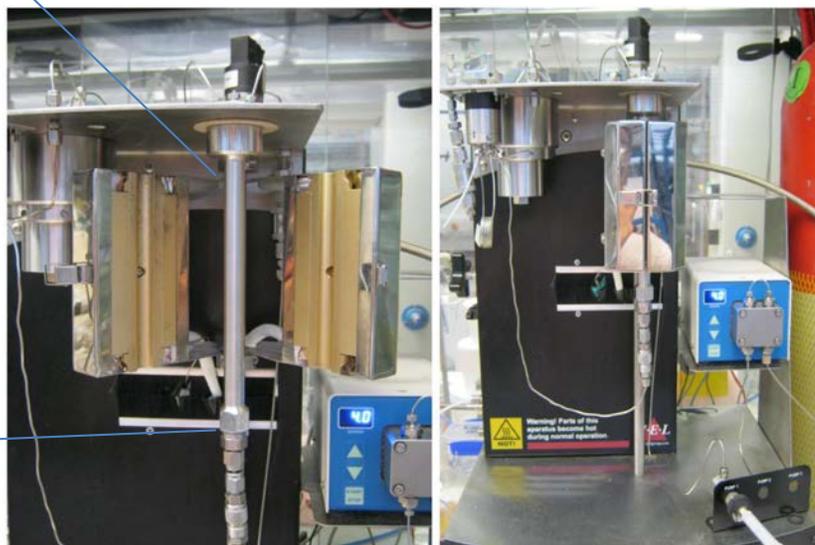
Trickle bed reactor: triphasic reactor

Gas-solid-liquid reactions

- Catalyst solid bed is confined in reactor
- Liquid flows from top to bottom by gravity
- Gas can flow co- or countercurrently w.r.t liquid



- | | |
|---------------------------|---------------------------|
| 1. Liquid/gas mixing zone | 5. Mass flow controller |
| 2. Heating jacket | 6. Pressure release valve |
| 3. Trickle bed | 7. Collection vessel |
| 4. Liquid/gas separator | 8. H ₂ Venting |

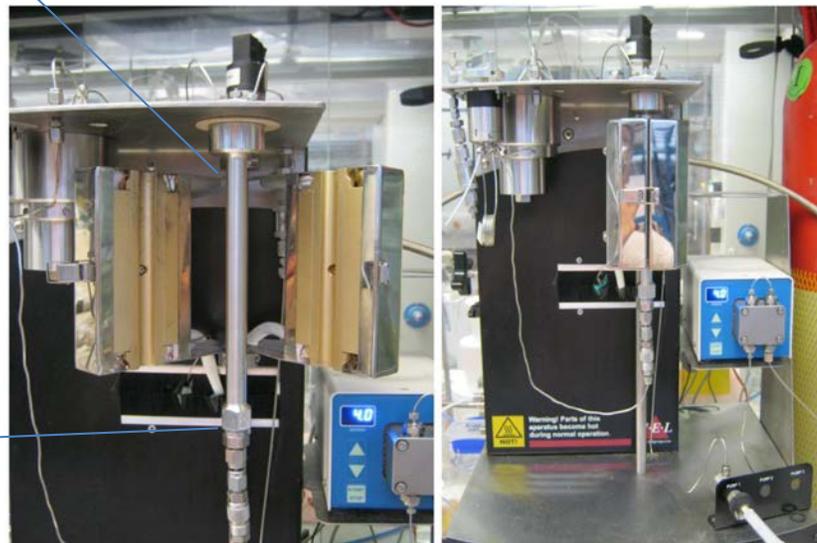
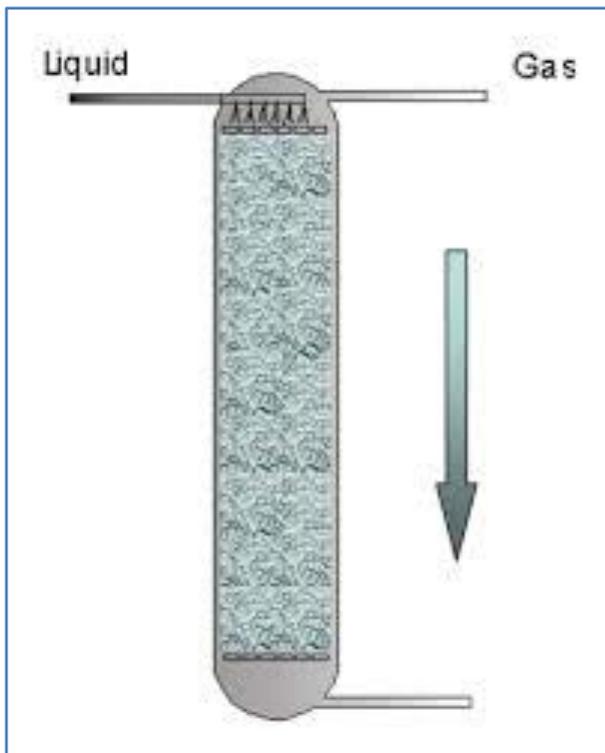


Trickle bed reactor: triphasic reactor

Gas-solid-liquid reactions

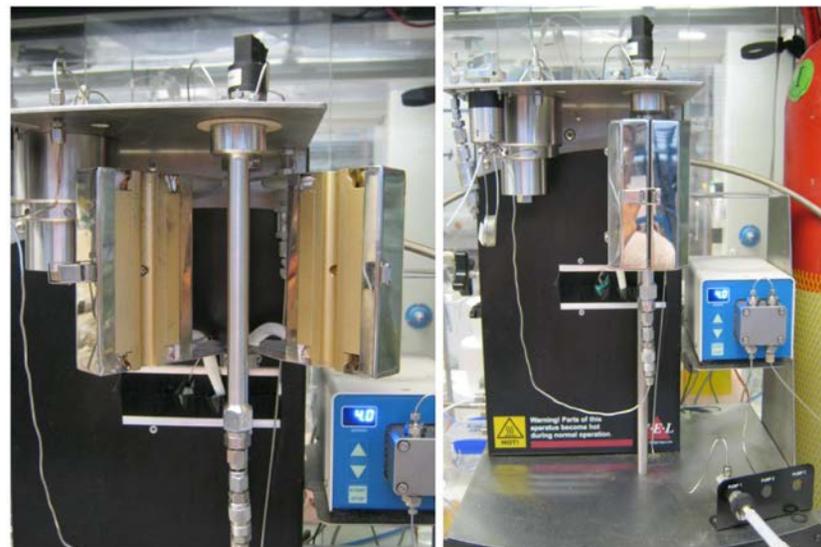
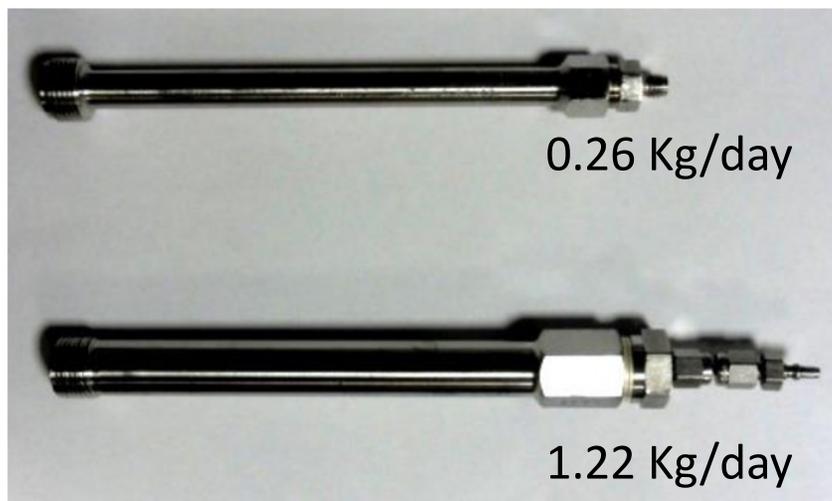
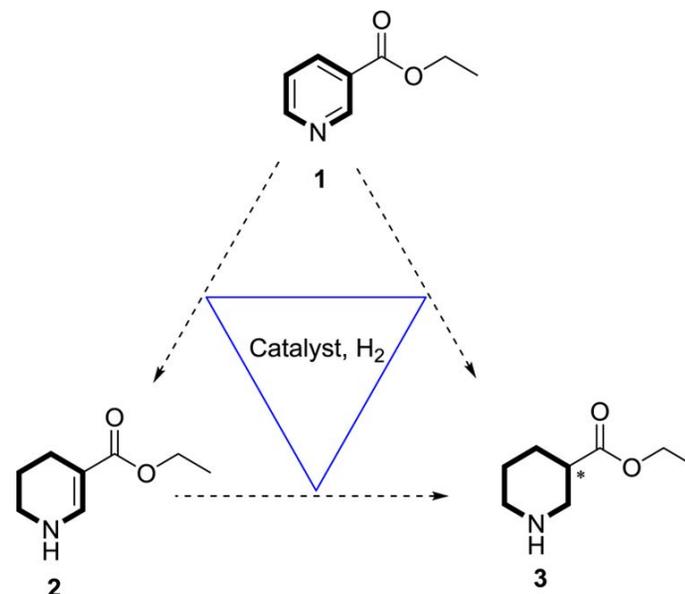
- Catalyst solid bed is confined in reactor
- Liquid flows from top to bottom by gravity
- Gas can flow co- or countercurrently w.r.t liquid

The catalyst particle size plays a crucial role in reactant mixing and flow pattern
Particles smaller than 0.1 mm dia causing flow blockage while particles bigger than 0.25 mm dia causing flow channelling



Trickle bed reactor: selective hydrogenation

- Batch reactor at 100 psi hydrogen and 38 h: 74% yield of **2** maximum
- TBR reactor at 300 psi hydrogen and minutes reaction time: 90% yield of **2**
- Efficient scale up was achieved by simply using a larger diameter reactor
- Increasing temperature above 100 C and hydrogen pressure to 1500 psi switches product selectivity to 90% yield of **3** without further modifications



Commercial bench scale flow Reactors



Gas reactor
(<http://www.cambridgereactordesign.com/>)



Trickle bed reactor
(<http://www.helgroup.com/>)



Microchip reactor unit
(<http://www.chemtrix.com/>)



Syringe pumps
(<http://syrris.com/>)



Gas reactor platform
(<http://www.thalesnano.com/>)



Reaction platform
(<http://www.uniqsis.com/>)



Cryogenic reactor unit
(<http://www.cambridgereactordesign.com/>)



Reaction platform
(<https://www.vapourtec.com/>)

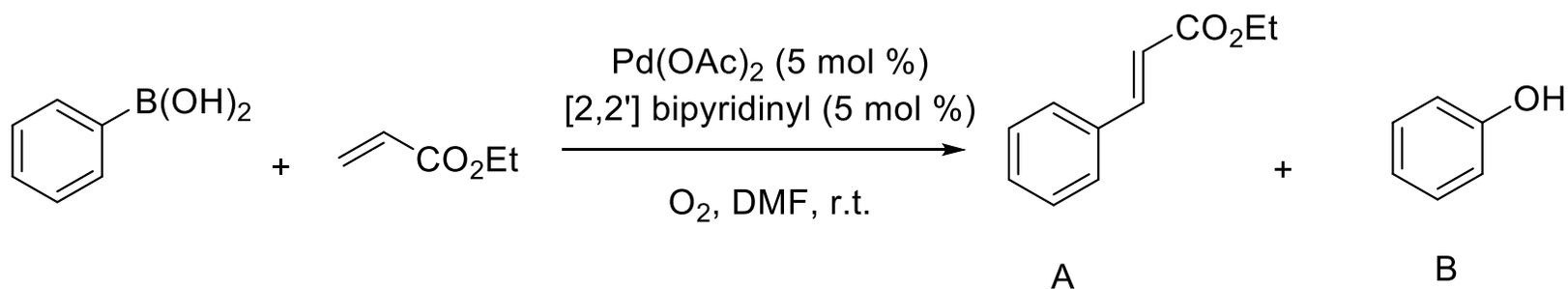
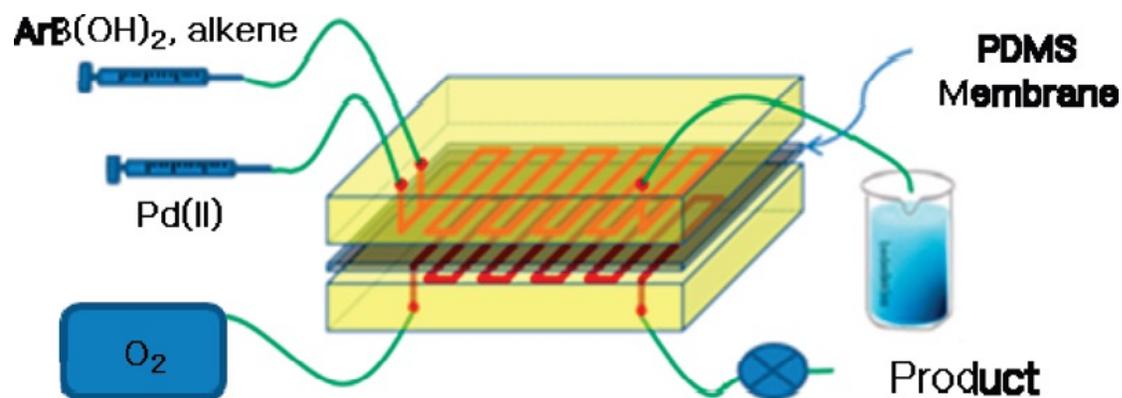


Reaction platform
(<http://www.amtechuk.com/>)

Dual Channel microreactor: oxidative Heck reaction

A thin gas permeable membrane is sandwiched between two PDMS slabs, the engraved microchannel in each of the slabs facing the other microchannel across the thin PDMS membrane. The microchannel in one of the slabs is used for liquid flow, while the other microchannel across the thin membrane is used for gas flow.

- Better gas-liquid contact
- Enhanced control of gas flow
- Difficult to fabricate reactor



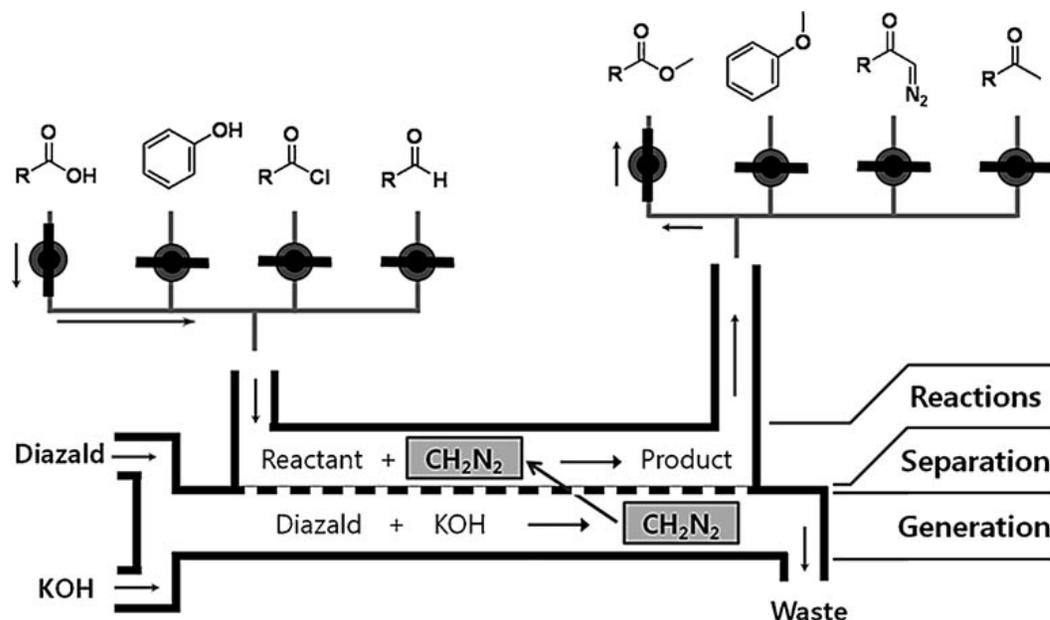
	12 h batch	30 min DC
Yield A:B %	69:24	82:8

Dual Channel microreactor: handling diazomethane

- Diazomethane is odourless, toxic, carcinogenic, and explosive gas
- Insitu generation of diazomethane mitigates problems associated with its handling
- The use of DC reactor with PDMS membrane allows for insitu generation of anhydrous diazomethane from aqueous solution without dangerous distillation or drying
- Suitable for wide range of applications even the moisture sensitive Arndt-Eistert synthesis

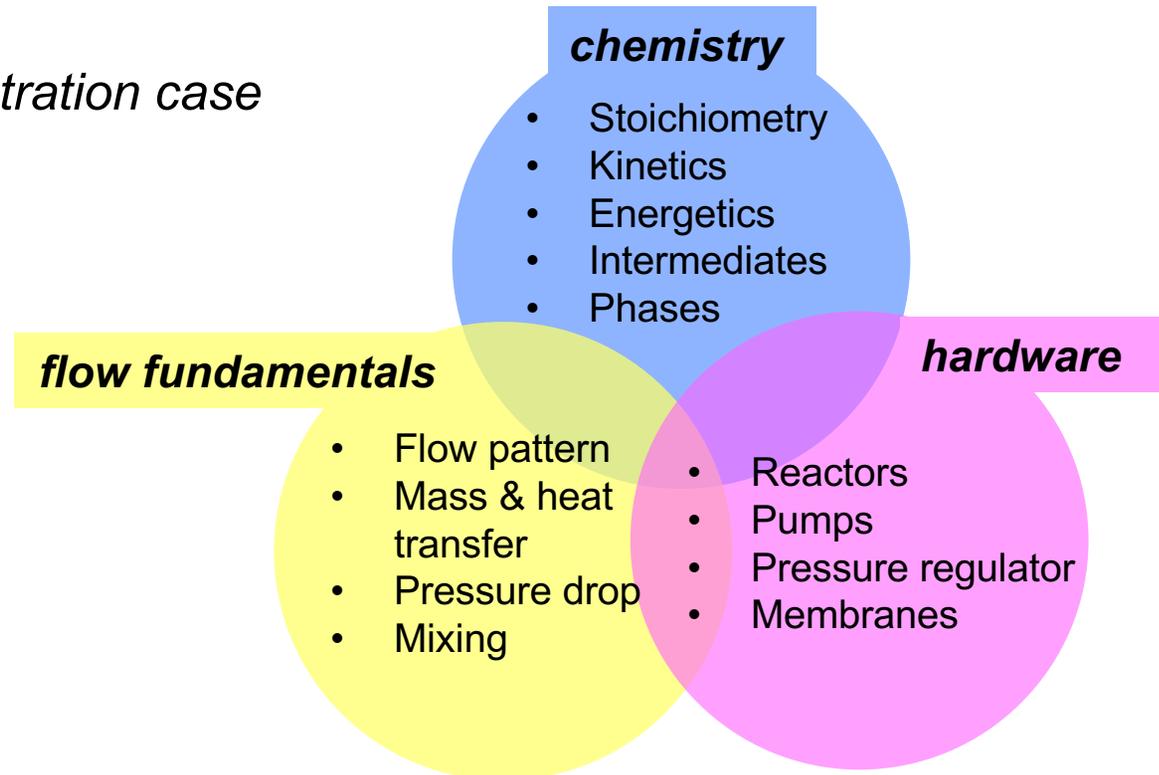
Entry	Substrate	Flow rate [$\mu\text{L min}^{-1}$]	KOH + Diazald flow rate [$\mu\text{L min}^{-1}$]	Product	Yield [%] ^[b]	Daily output [mmol]
1		4	10		> 99	2.88
2		1	4		> 99	0.72
3		1	4		81	0.58
4 ^[c]		1	4		90	0.65

[a] Diazomethane was generated in the bottom channel by flowing solutions of diazald (1.0 M in DMF) and KOH (2.0 M in water containing 0.01 % aliquat 336) with the same flow rate. Substrates were introduced to the top channel in DMF (0.5 M solution). [b] Yields were determined by GC/MS analysis using an internal standard. [c] Arndt-Eistert synthesis.



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 - *Microchannel reactor & **Flash chemistry***
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- *Total synthesis demonstration case*



Flash Chemistry: capture the unstable intermediate

- Extremely fast reactions (millisecond reaction time) leading to unstable intermediates could be carried out effectively with high resolution reaction time control
- Microreactors are needed to minimize mixing to reaction time ratio and allow for precise reaction time control in Flash chemistry

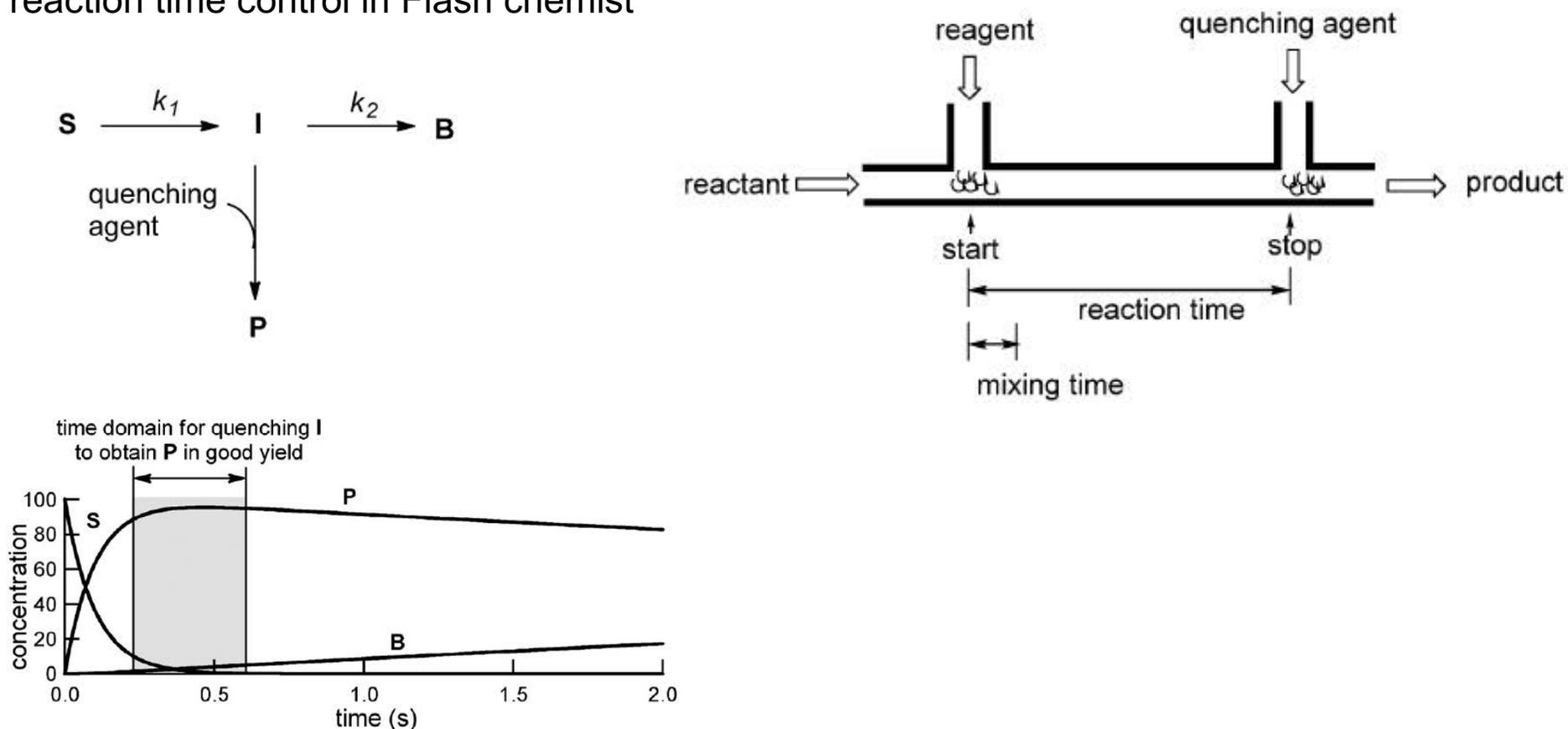
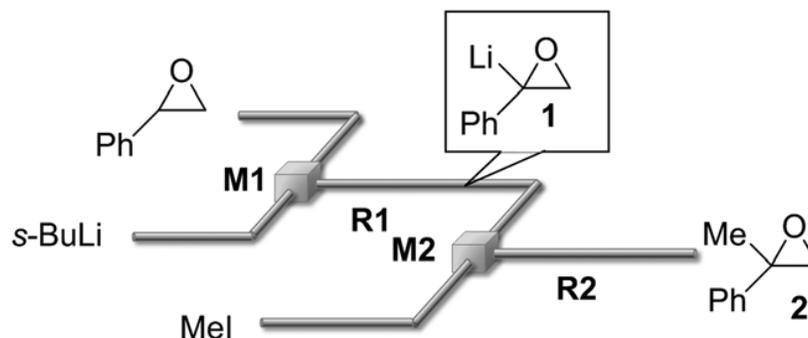


Fig. 6 A variation of the concentrations of reaction components against time ($k_1 = 10 \text{ s}^{-1}$ and $k_2/k_1 = 0.01$).

Flash Chemistry: capture the unstable intermediate

- In a conventional batch reactor the use of *s*-BuLi in the absence of TMEDA caused decomposition even at -98 °C.
- A flow microreactor enables us to conduct the transformation at higher temperatures such as ca. -70 °C.



- By choosing an appropriate residence time for quenching (addition of iodomethane), the methylated product was obtained in a high yield.

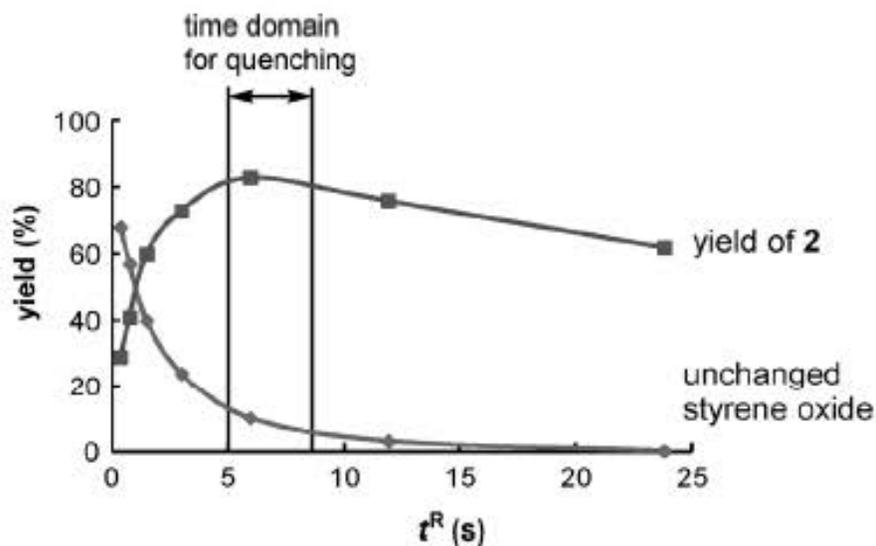
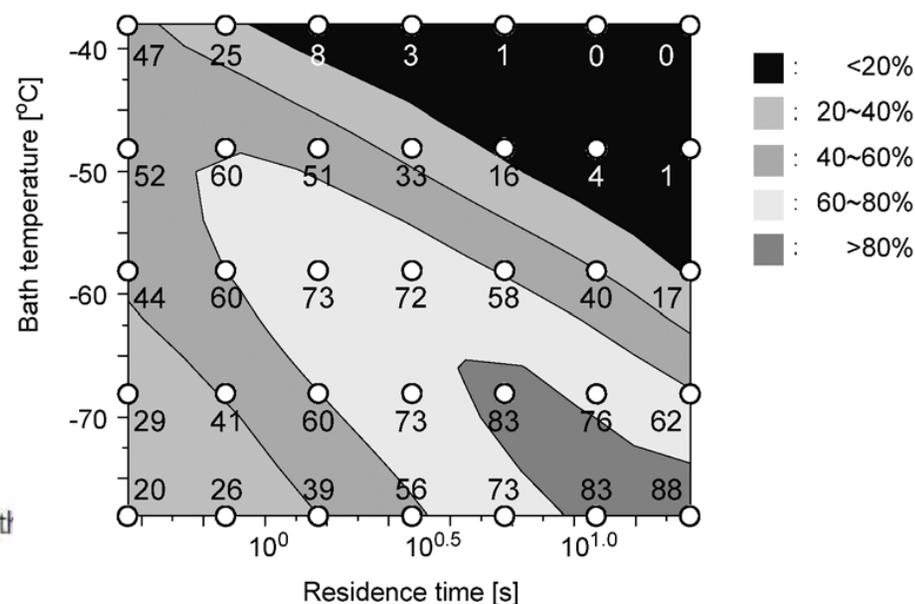
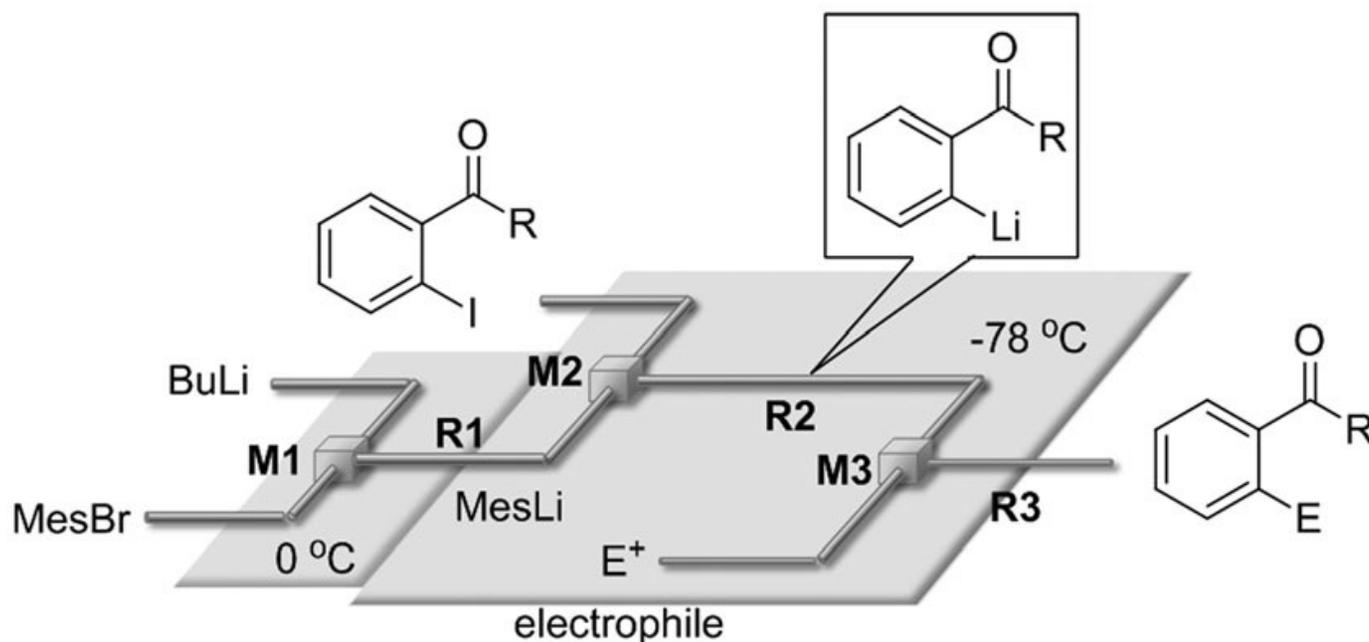


Fig. 8 Plots of the amount of unchanged styrene oxide and the yield of the methylated product against the residence time (t^R) at -68 °C.

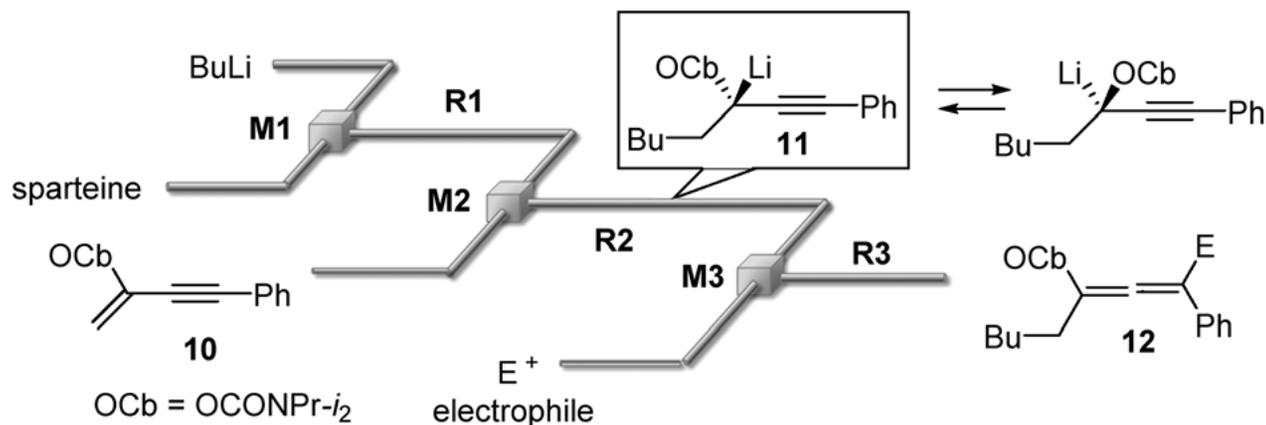


Flash Chemistry: Protecting group-free synthesis

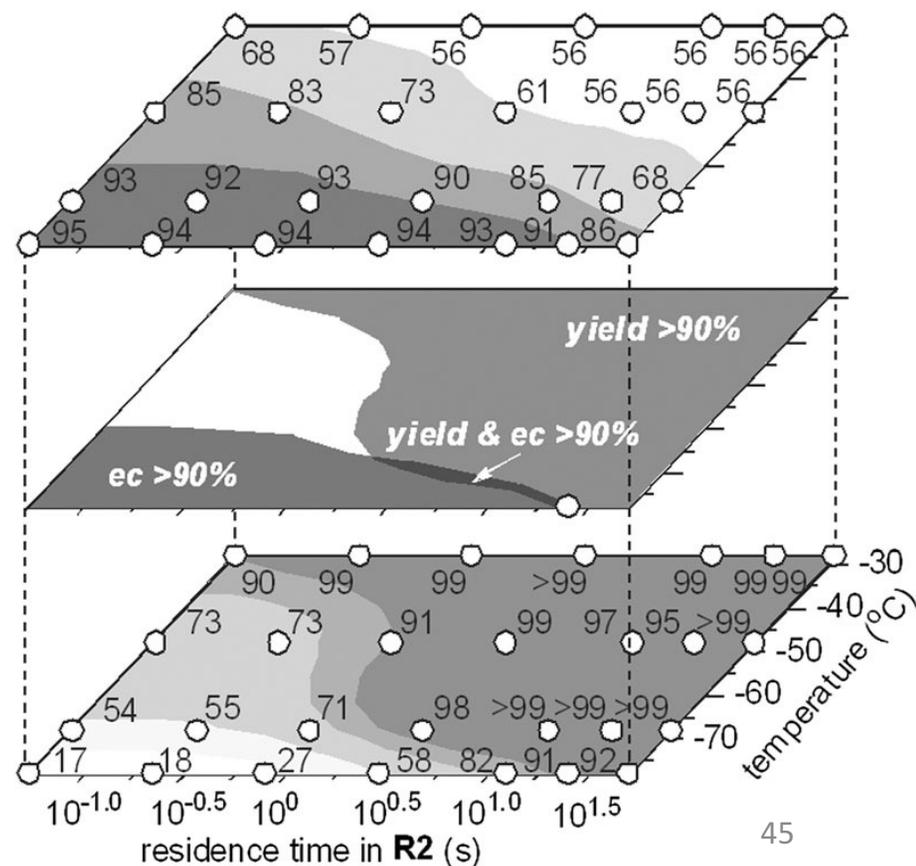
- Unprotected ketone carbonyl groups can potentially survive in organolithium reactions within a very short reaction time
- Efficient reaction of electrophiles including aldehydes, chloroformates, and isocyanates with lithiated unprotected ketones was achieved at residence time of 0.003 s or less.
- Longer residence times lead to decomposition of the aryllithium species to give by-products such as dimeric compounds.



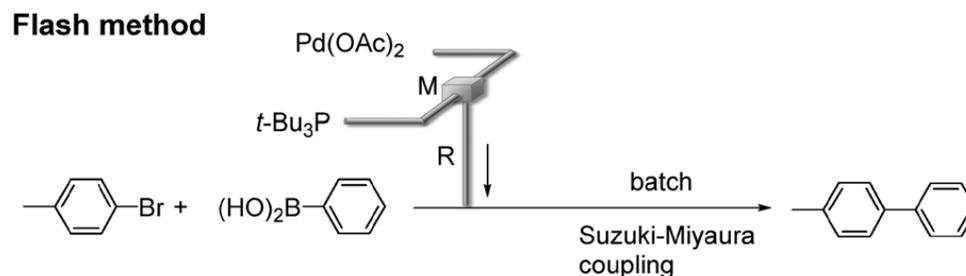
Flash Chemistry: asymmetric synthesis



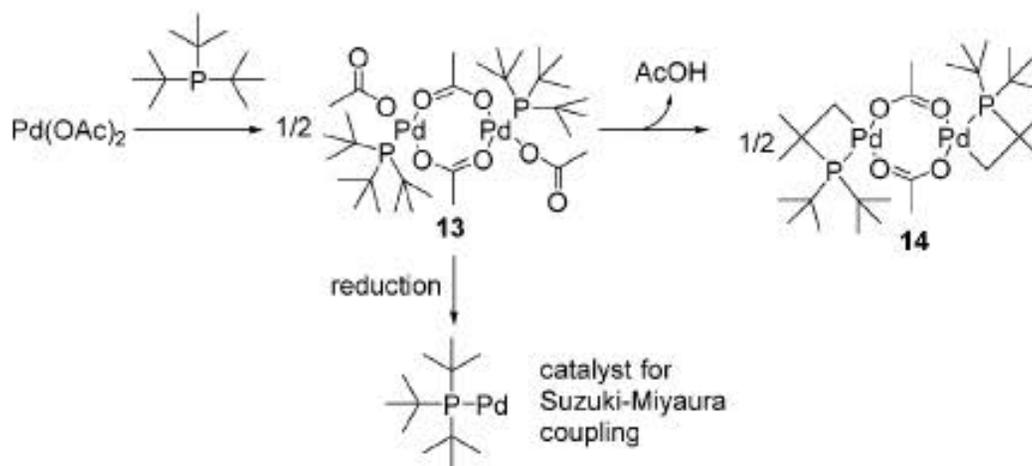
- Flow microreactor systems enable the rapid generation of configurationally unstable organometallics...
- and allow their reaction with electrophiles before they epimerize
- 91% yield and 91% ee vs 60% max. ee in batch



Flash Chemistry: catalyst generation

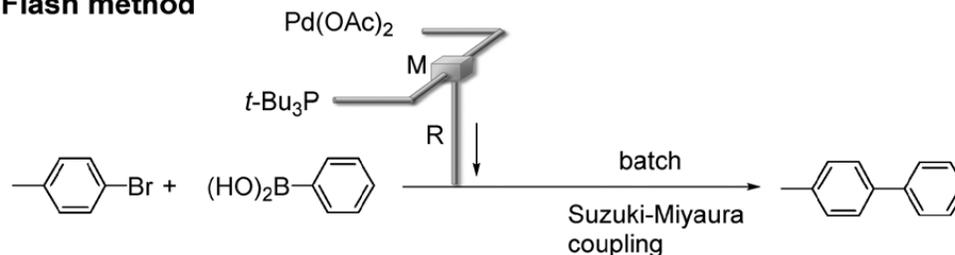


- Coordinatively unsaturated $[\text{Pd}(0)\text{L}]$ species are highly reactive towards oxidative addition of aryl halides (ArX) to produce $[\text{Pd}(\text{Ar})\text{X}(\text{L})]$, a key intermediate in the Suzuki-Miyaura coupling
- $[\text{Pd}(0)\text{L}]$ is highly unstable and its generation at high concentrations is very difficult.
- The flash method involving 1 : 1 mixing of $\text{Pd}(\text{II})$ and L in a flow microreactor enables the generation of $[\text{Pd}(\text{II})\text{L}]$ species in the absence of coupling substrates.
- $[\text{Pd}(\text{II})\text{L}]$ species is transferred, before it decomposes, to a reaction vessel for coupling reactions, where it may be reduced to give highly reactive $[\text{Pd}(0)\text{L}]$. $R_t = 0.65$ s



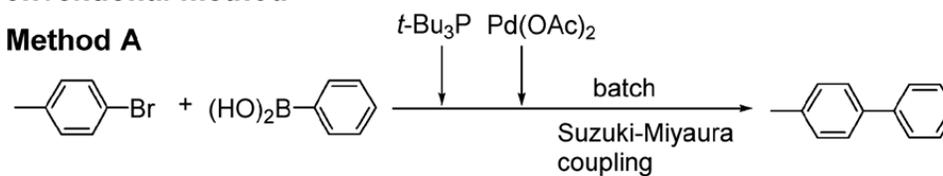
Flash Chemistry: catalyst generation

Flash method

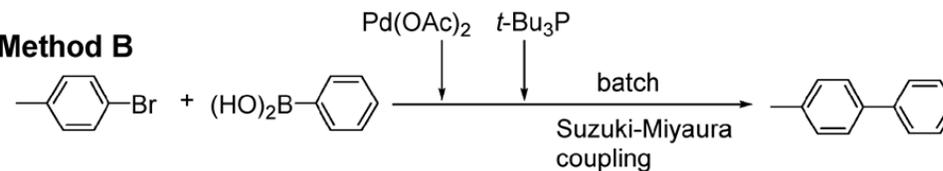


Conventional method

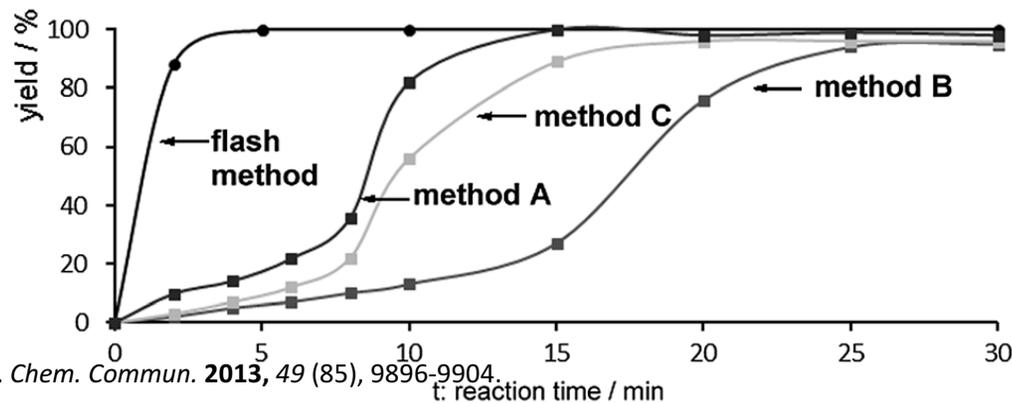
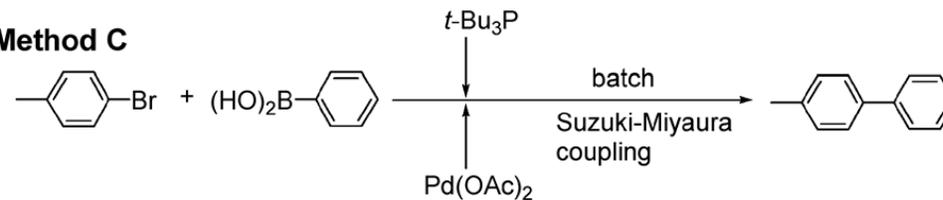
Method A



Method B

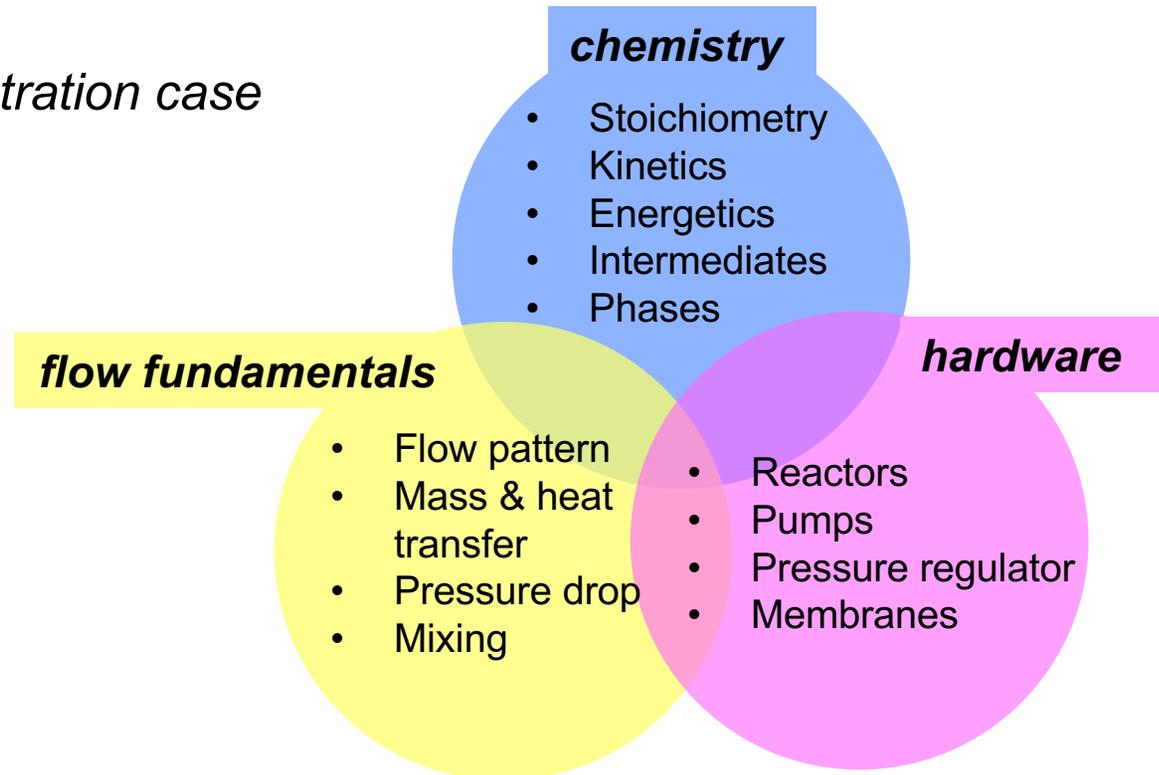


Method C



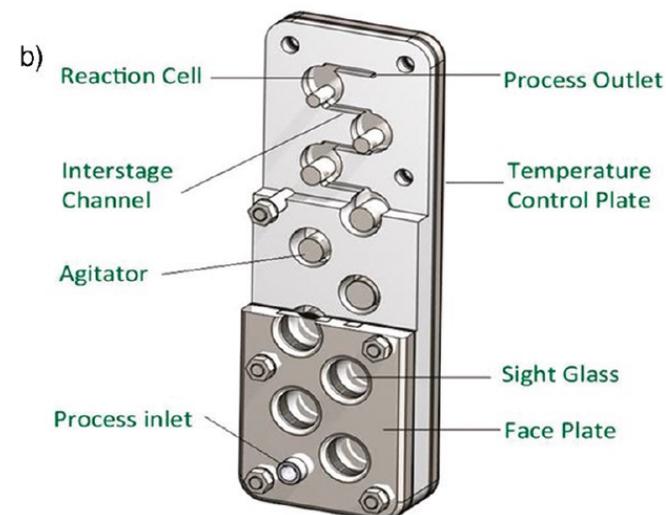
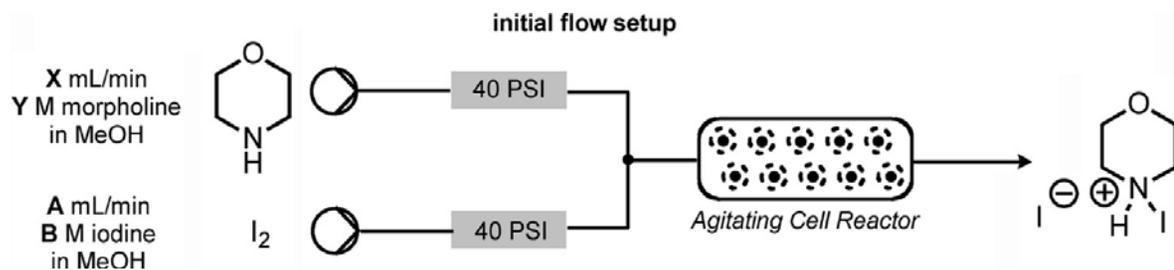
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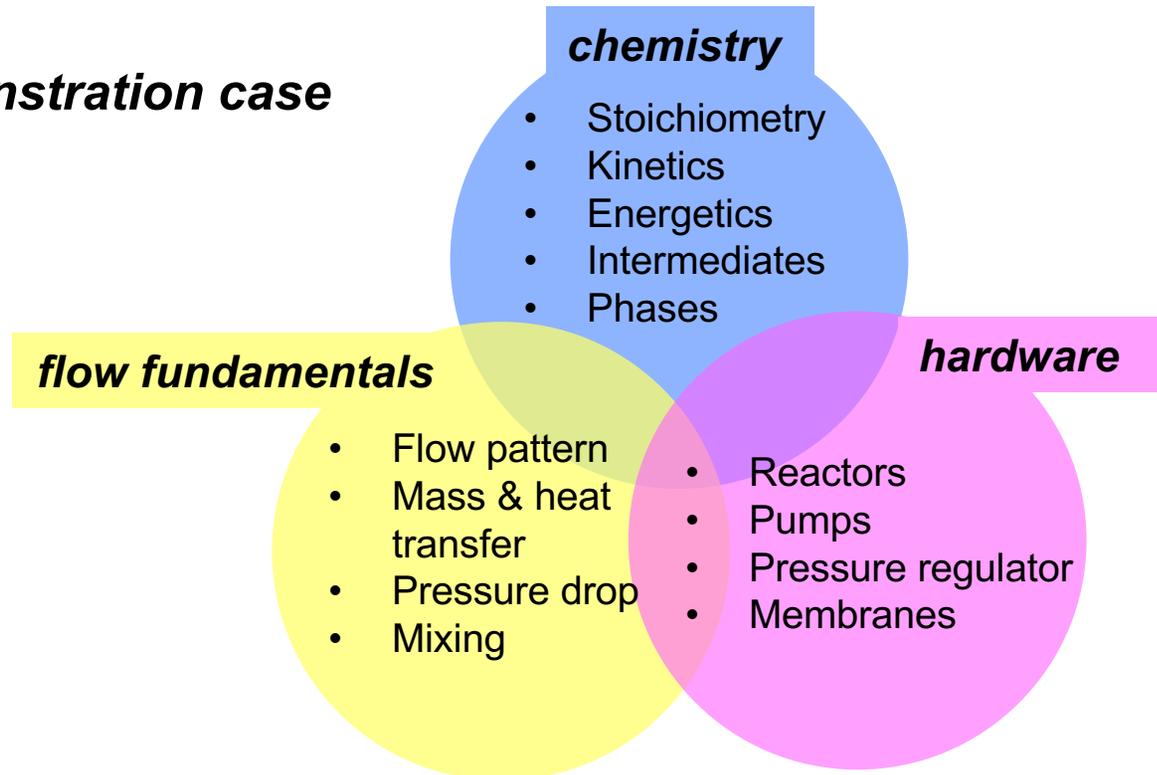
Common drawback: solid formation

- Solids in flow reactors cause blockages
- The ability to tolerate solids varies greatly
 - ratio between channel diameter and particle size
 - velocity of the reaction
- The use of solid reagents is typically easiest by isolating them in a “column” and flowing the reaction in solution through the packed column
- Solution to solids issues is often a chemistry solution:
 - Add co-solvents to increase solubility of products
 - Reduce concentrations of reaction
- Or use of specially designed reactors

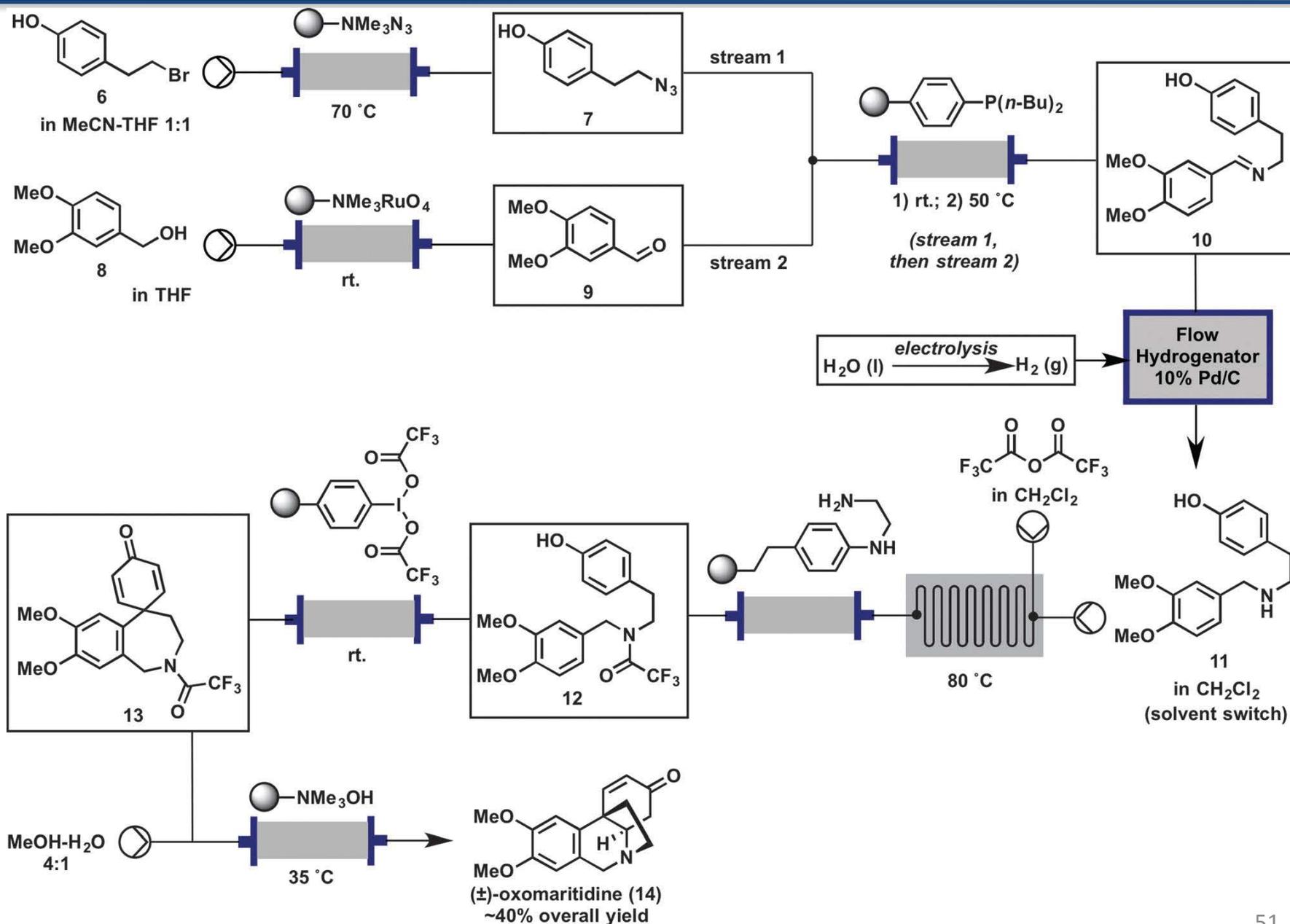


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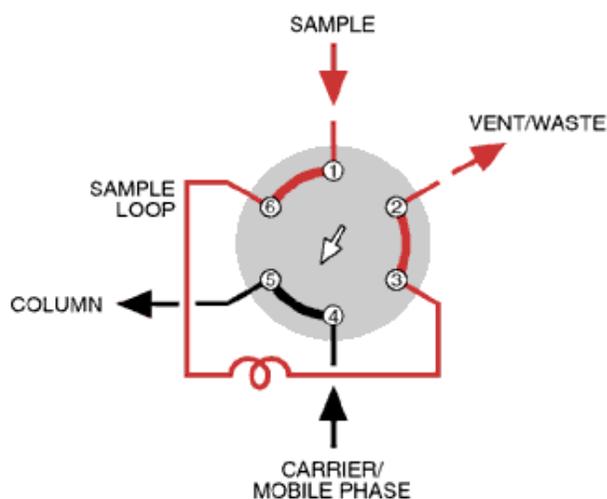


Natural Product Synthesis: Oxomaritidine



Analytical techniques in flow chemistry

- Several analytical methods can be integrated for online measurements such as IR, Uv-vis...
- Automated sampling valves used to deliver samples to other methods; GC, MS, IR



<http://www.vici.com/support/app/app11j.php>



http://www.siphotonics.com/Pages/UV_Vis_Spectrophotometer_Flow_Cells.html



http://www.mt.com/in/en/home/products/L1_Autoc hemProducts/ReactIR/flow-ir-chemis.html

Conclusion

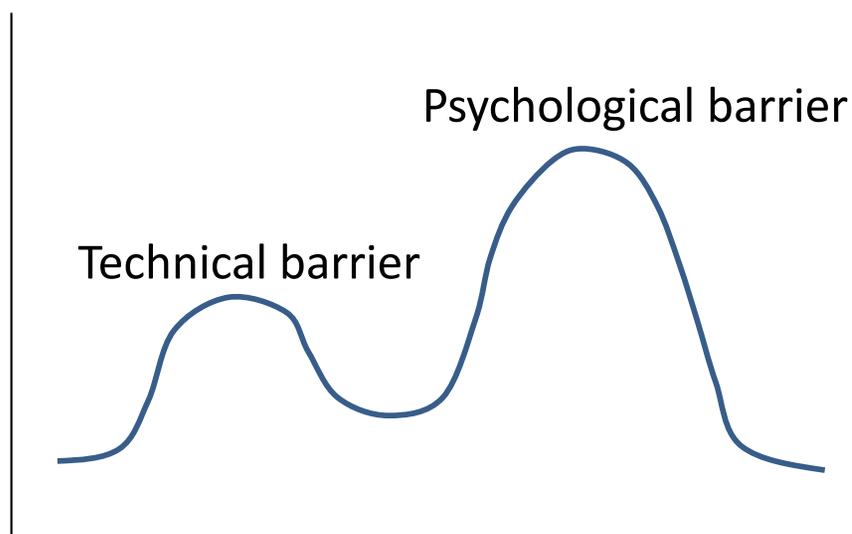
Flow Chemistry:

- Better mixing, enhanced heat and mass transfer
- Better conditions control, efficient handling of unstable intermediates
- Better reproducibility, easier scale-up

Several reactor designs for different reactive systems

Demonstrated to effectively perform multistep total synthesis

Disruptive technology, not meant to replace a skilled organic chemist but to allow more time for experiment design and analysis



Useful resources

Societies and Forums:

<http://www.flowchemistrysociety.com/>

http://www.flowchemistrysociety.com/journal_of_fc.php

<http://www.flowchemistrytks.com/index.html>

Research groups:

Ley Group, Univ. of Cambridge

<http://www.leygroup.ch.cam.ac.uk/>

Kappe Group, Uni Graz schafft Fortschritt

<https://homepage.uni-graz.at/de/oliverkappe/>

Yoshida Group, Kyoto University

<http://www.sbchem.kyoto-u.ac.jp/yoshida-lab/en/index.php?research>

Jamison Group, MIT

<http://web.mit.edu/chemistry/jamison/Research/>

Technology providers:

<http://syrris.com/>

<http://thalesnano.com>

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