

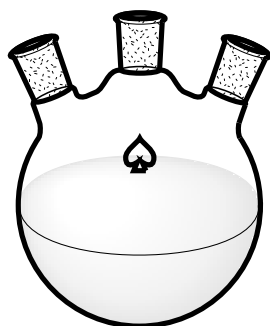
Andrew Zahrt
Denmark Laboratories
University of Illinois, Urbana-Champaign

***Autonomous Optimization of Chemical
Reactions in Flow***

Denmark Lab Group Meeting
February 12, 2019

Batch vs. Flow

Batch Reactors



Advantages

Most Laboratory Scale,
Literature Procedures
are in Batch

Easy to use stoichiometric
solid reagents / deal with
solid byproducts

Easy to Optimize
Discrete Variables

Disadvantages

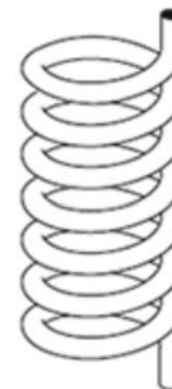
Temperature Gradients

Mass / Phase Transfer
can be problematic

Mixing is not uniform

Larger Scale necessitates
Larger Reactor

Flow Reactors



Advantages

Efficient Heat Transfer

Efficient and Uniform
Mixing

Pressure control

Easily Scalable

Safely use with
Hazardous Substances

Easy to optimize
continuous variables

Disadvantages

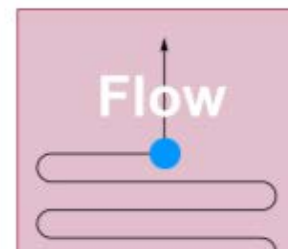
Few examples of optimized
systems accessible to
the synthetic chemist

Dealing with solids reagents
or byproducts (NOT catalysts)
can be challenging

Optimization of discrete
variables is a an
active area of research

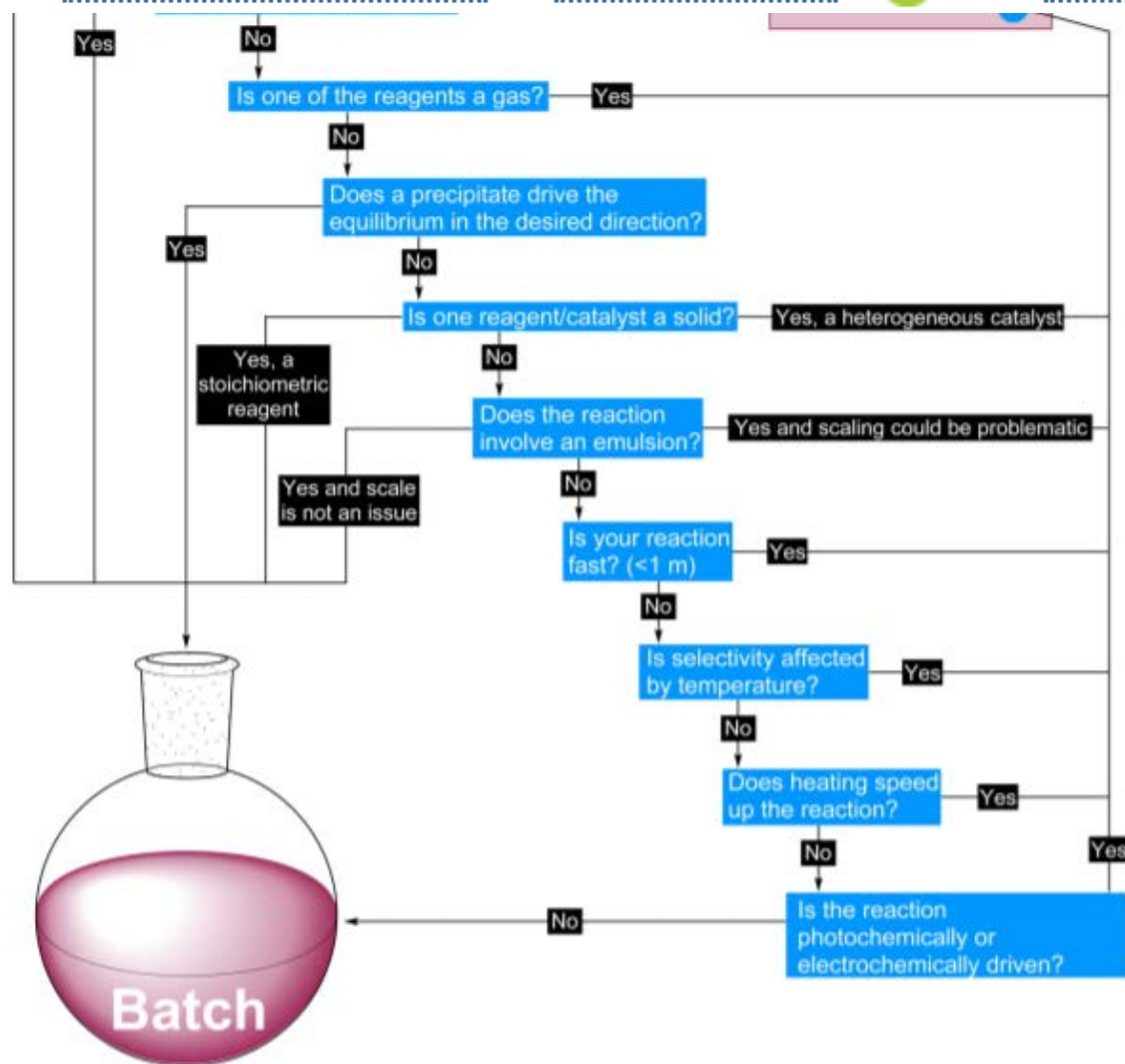
CHEMICAL REVIEWS

answer to the ultimate question
verse, and everything?



The Hitchhiker's Guide to Flow Chemistry ||

Matthew B. Plutschack[†], Bartholomäus Pieber[†], Kerry Gilmore^{*†} , and Peter H. Seeberger^{*†‡} 



Outline Slide

Anatomy of Flow Chemistry

Optimization of Continuous Variables

Optimization of Discrete Variables

Outline Slide

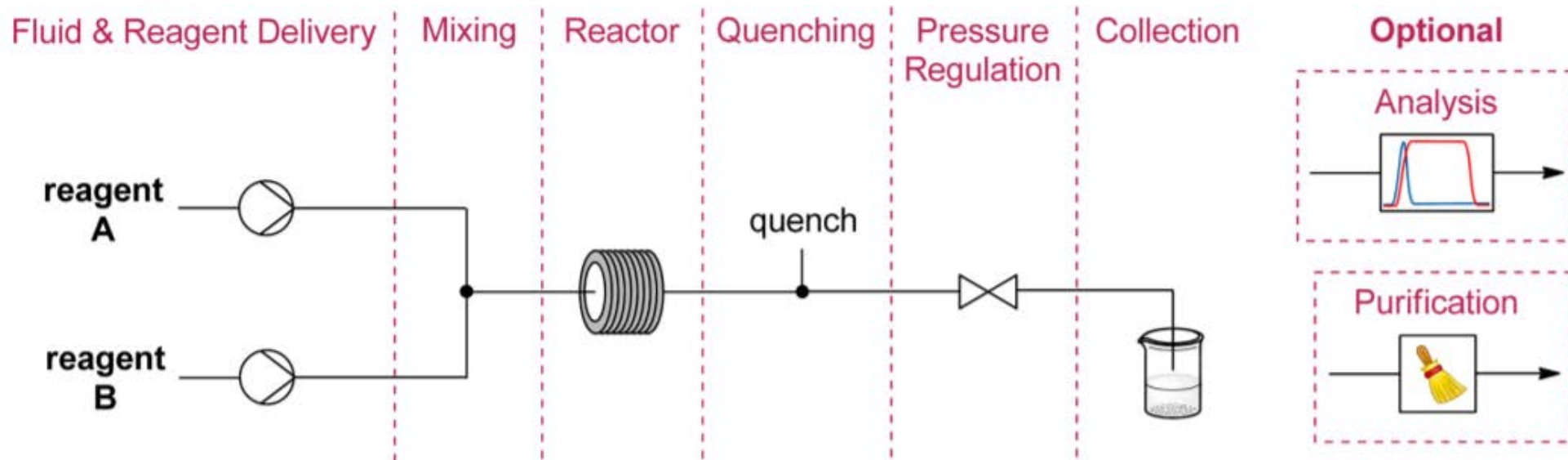
Anatomy of Flow Chemistry

Optimization of Continuous Variables

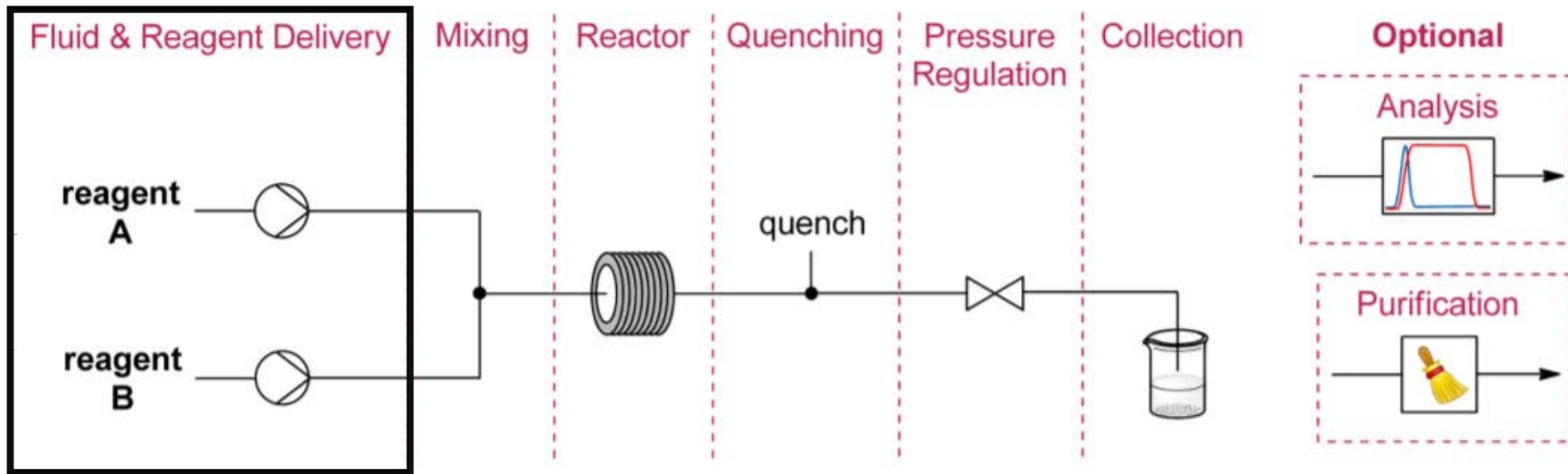
Optimization of Discrete Variables



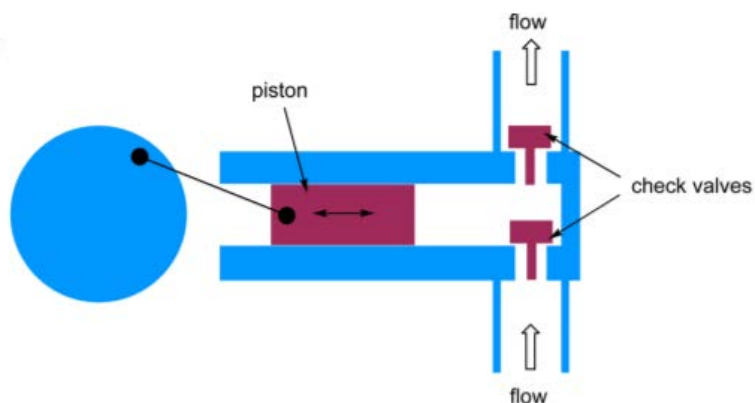
Anatomy of Flow



Anatomy of Flow: Reagent Delivery

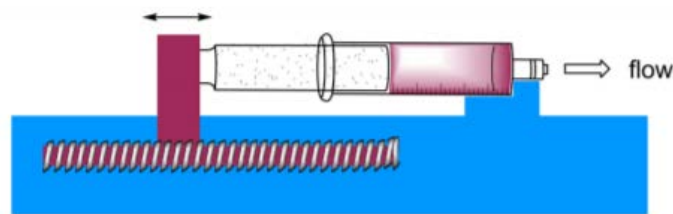


HPLC pumps



Flow rates > 0.1 mL / min
Suitable for high pressures

Syringe pumps



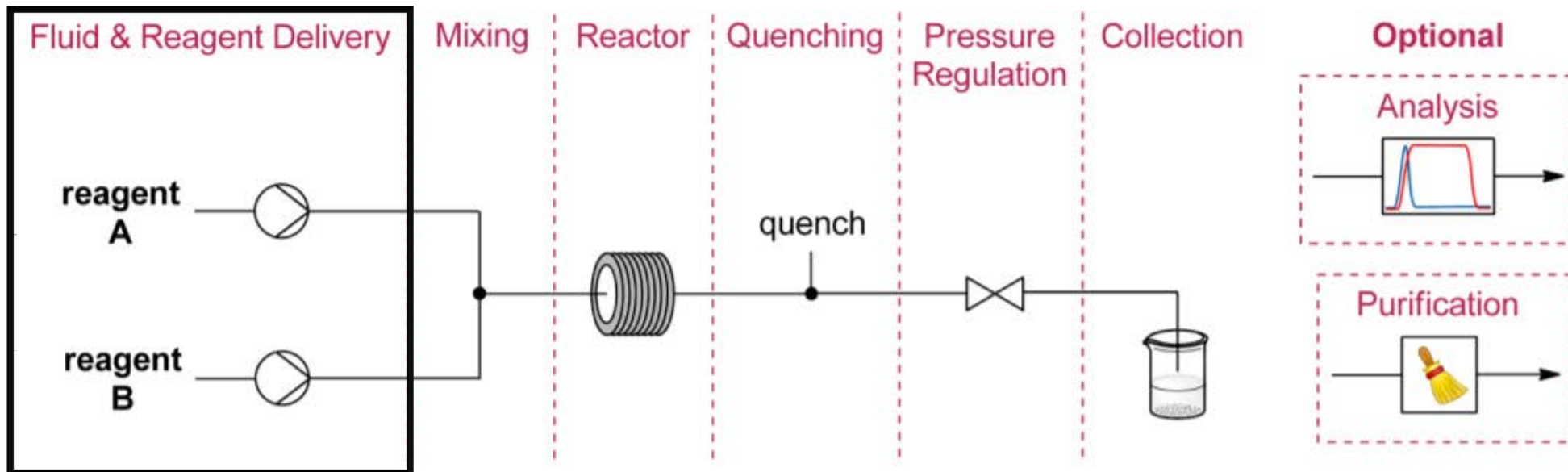
Lower Flow Rates
Constant Pressure
Usually Cheaper

Peristaltic pumps

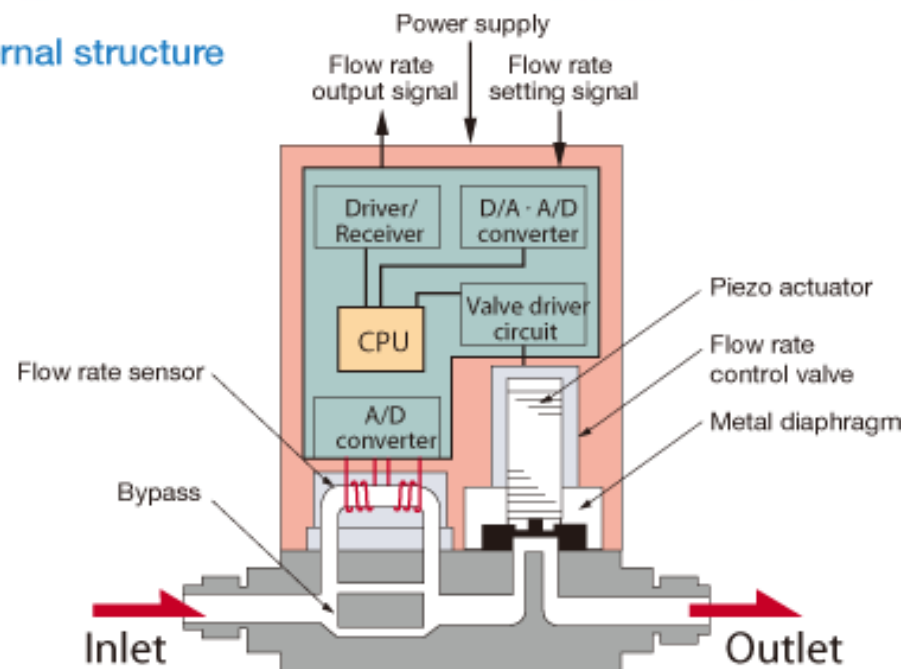


Generally more robust
Can pump well-suspended slurries

Anatomy of Flow: Reagent Delivery



Internal structure

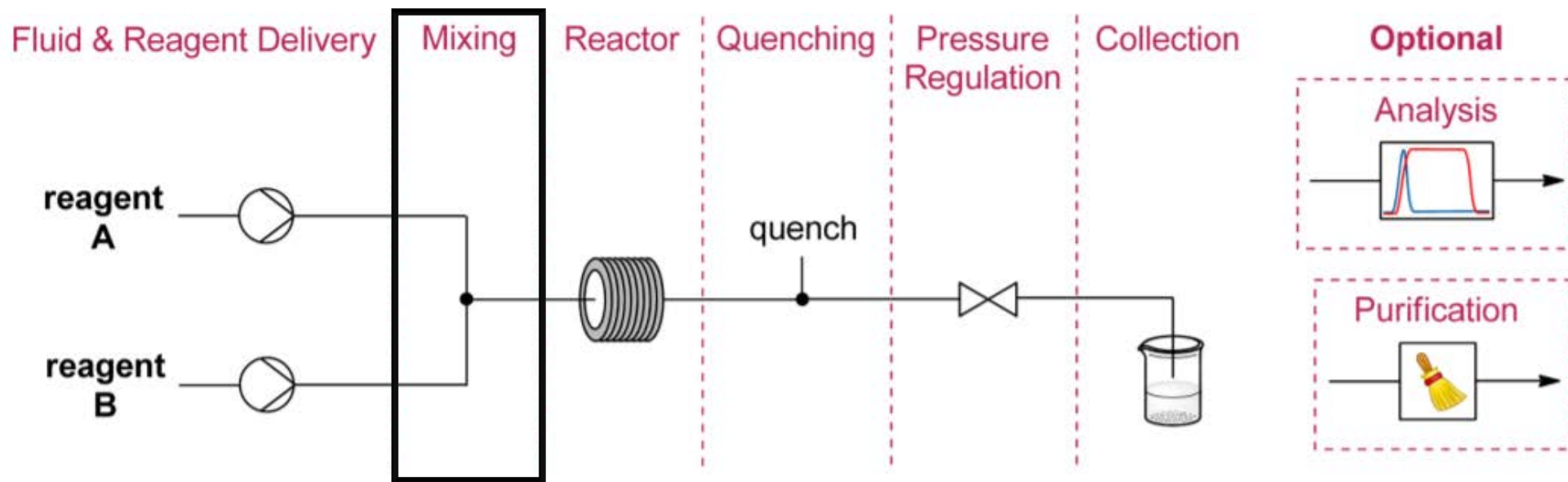


Gas Delivery:

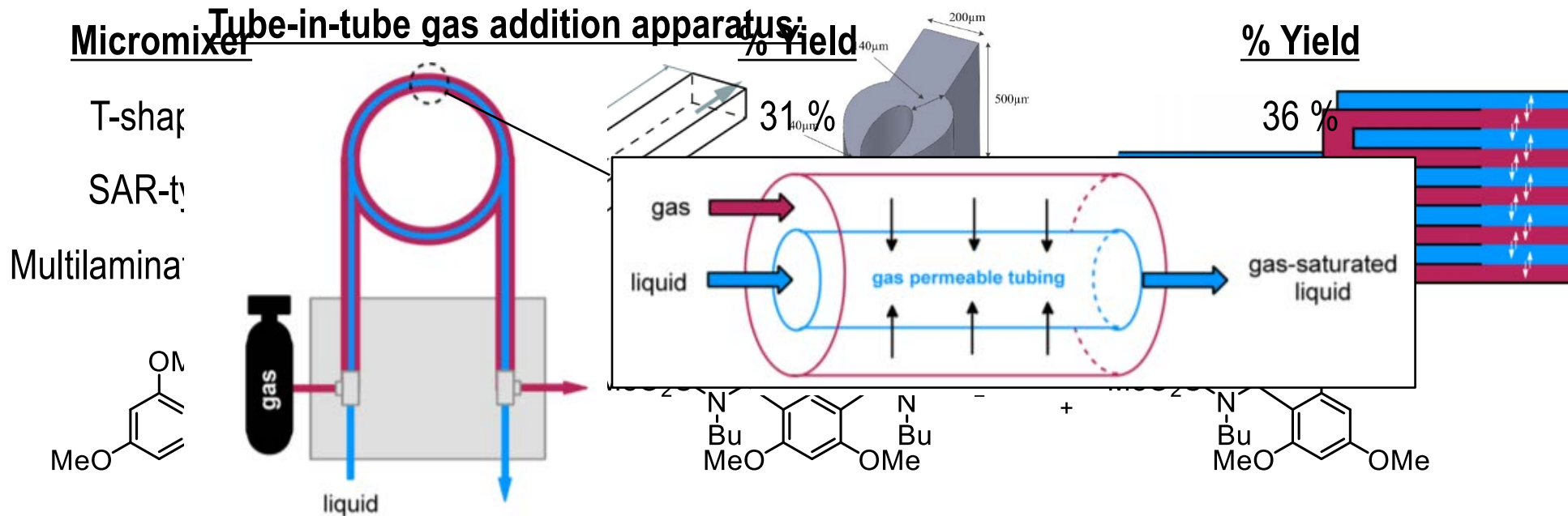
- 1) *Directly from tank*
- 2) *Precise delivery regulated by thermal mass flow controllers*

Solids are typically avoided!

Anatomy of Flow: Mixing

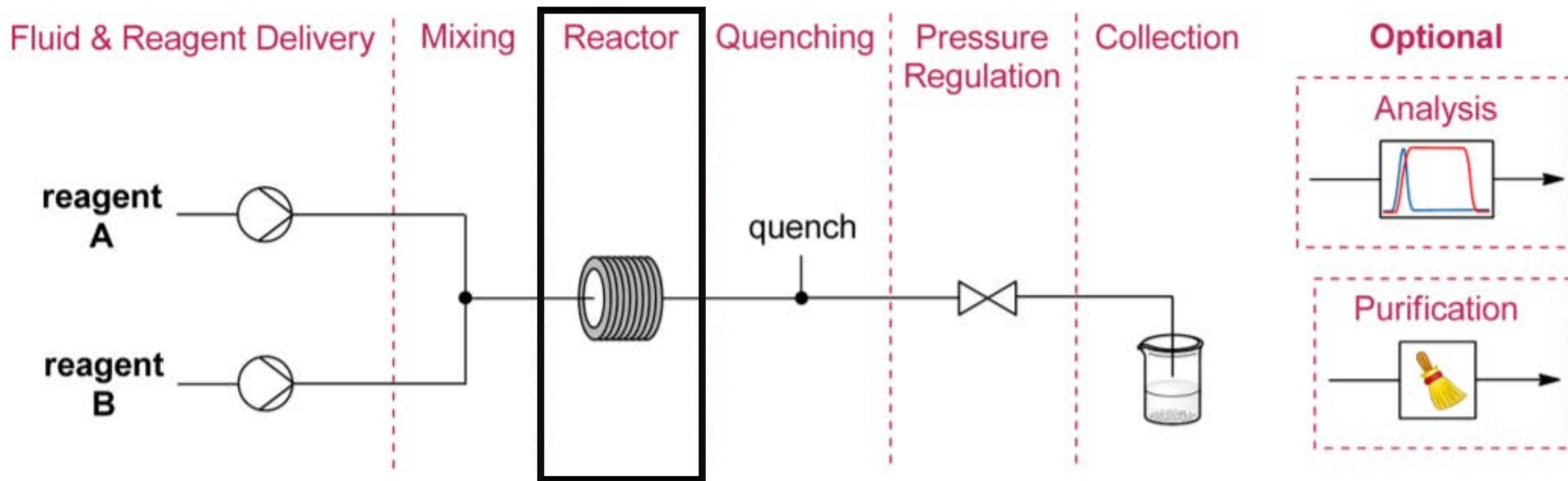


Micromixer Tube-in-tube gas addition apparatus:

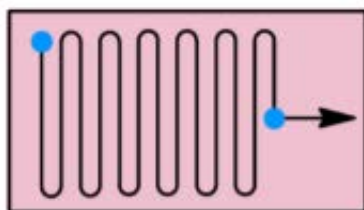


Nishino *et al.* *Lab Chip*. **2013**, 13, 1515-1521. Yoshida *et al.* *J. Am. Chem. Soc.* **2005**, 127, 11666-11675.

Anatomy of Flow: Reactors

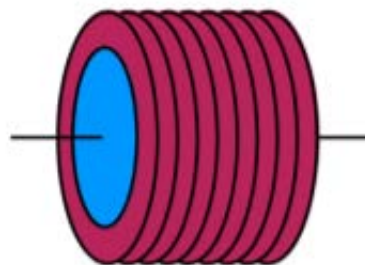


Chip Reactor



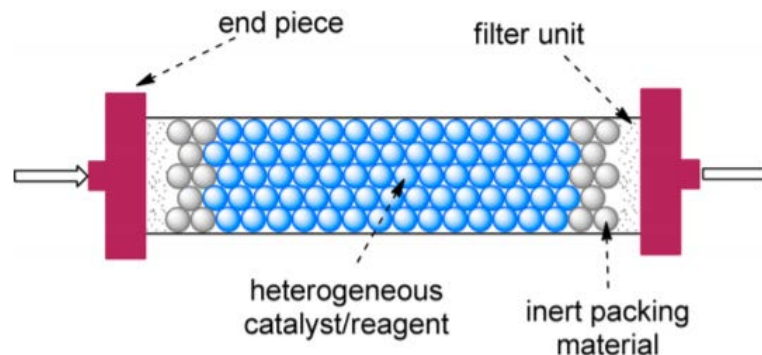
*Best Heat Transfer
Efficient Mass Usage
Tendency to Clog / Expensive*

Coil Reactor



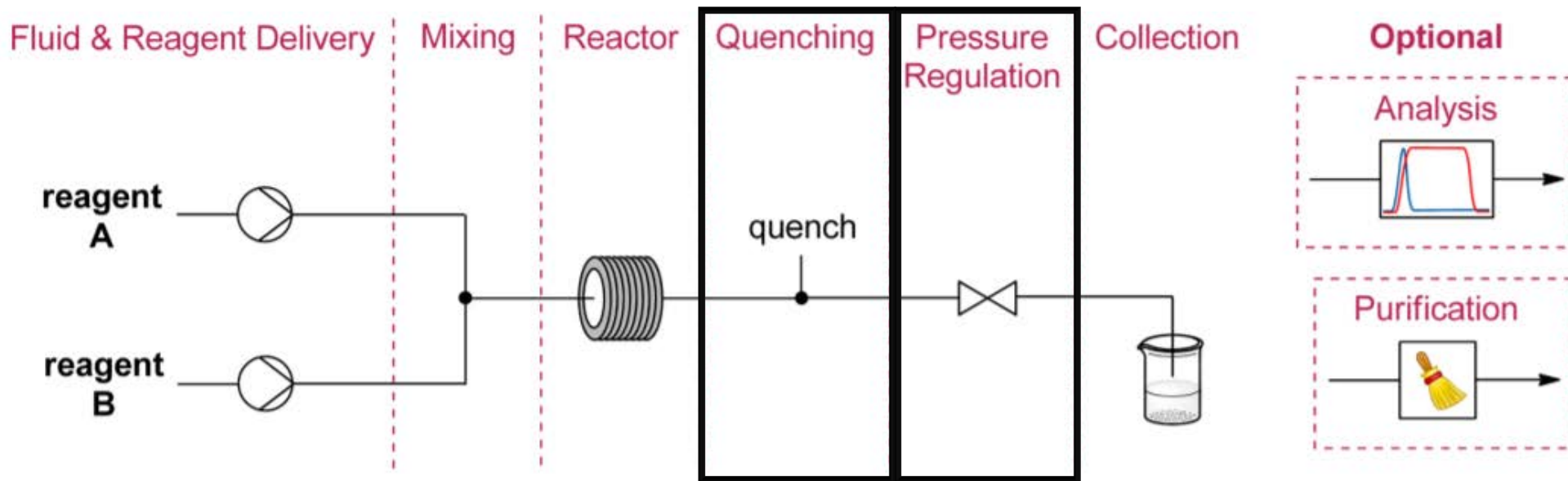
Made from readily available materials

Packed Bed Reactor



Heterogeneous Catalysis

Anatomy of Flow: Quenching and Pressure Regulation



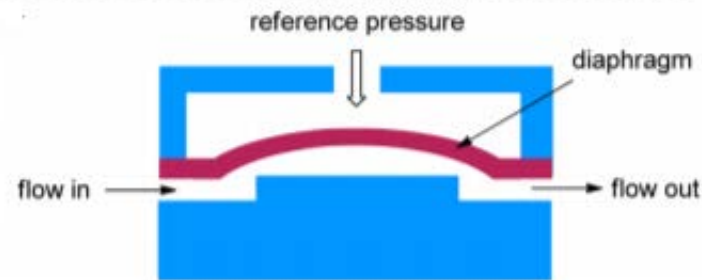
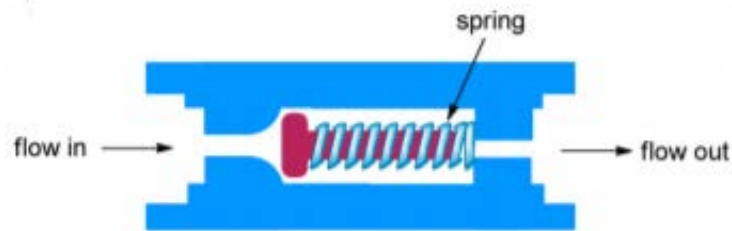
Quenching

Packed beds, photochemical / electrochemical systems stop upon leaving reactor

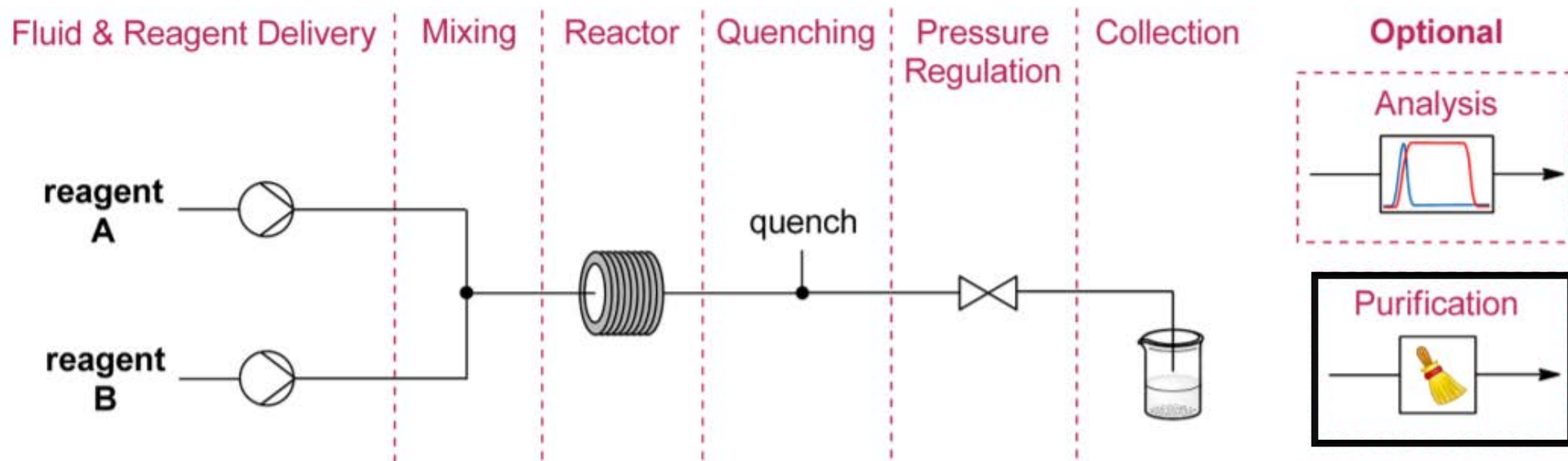
Rapid cooling

Chemical quenching

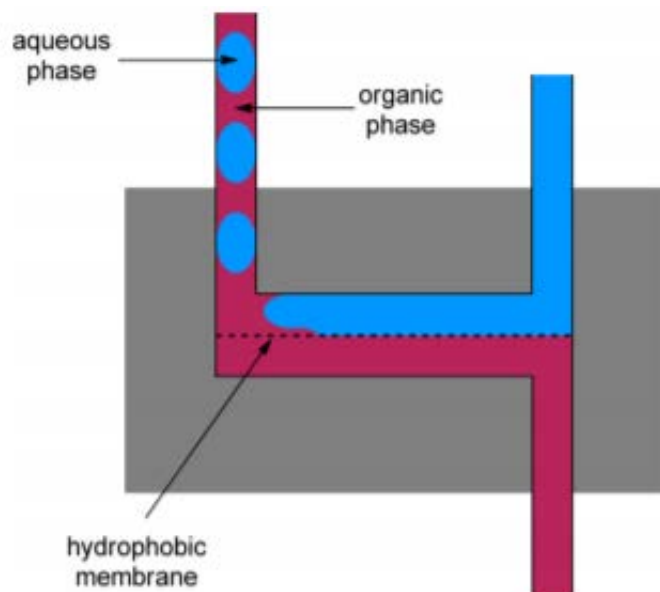
Back Pressure Regulators



Anatomy of Flow: Purification in Flow



Workups in Flow



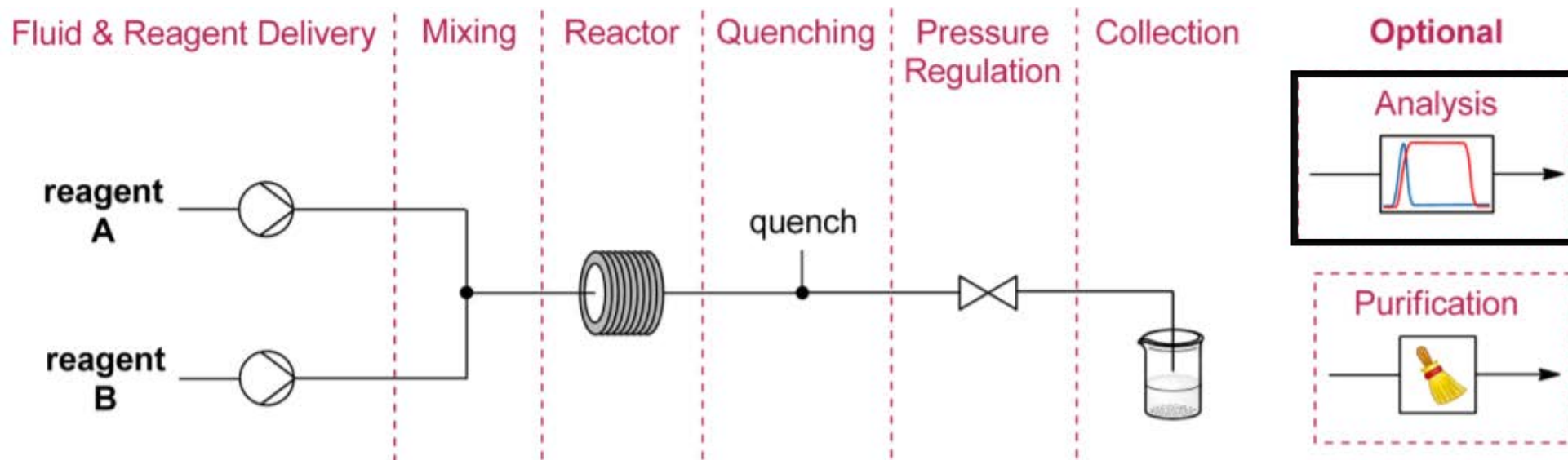
Other Purification Methods

Scavenger Cartridges

Simulated Moving-Bed Chromatography

Continuous Crystallizations

Anatomy of Flow: Analysis in Flow



Online Analysis

Periodic sampling

*Examples: GC, HPLC, NMR, Mass Spec.,
fluorescence spectroscopy, etc.*

Inline Analysis

*Sampling method is 1) nondestructive and
2) allows for "real-time-analysis"*

Examples: FTIR, Raman, NMR, UV-vis

*Online / Inline Analysis in flow systems enable instantaneous evaluation and
modification of reaction conditions.*

Why optimize reactions in flow?

Precise control over reaction conditions

Screening continuous variables is very easy

Efficient use of starting materials

Inline/Online analytics allow practitioners to “see into” reaction mixture

Why isn't everyone optimizing reactions in flow?

Dealing with solids / slurries is still challenging.

Screening discrete variables is still challenging. Examples in which solvent, catalyst, additives, etc. have been screened exist, but this is more an active area of research than an established field.

Inaccessible to most laboratories

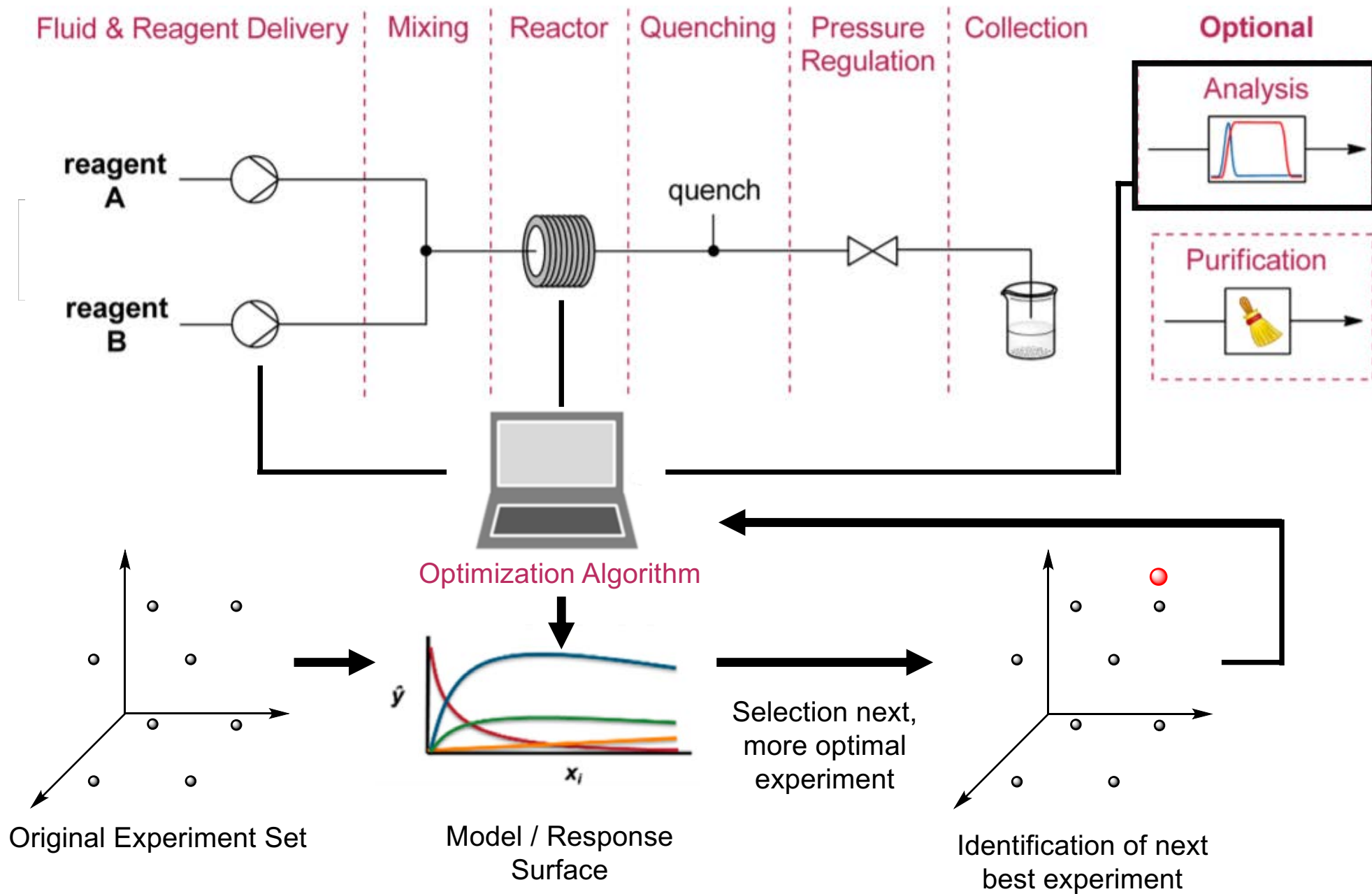
Outline Slide

Anatomy of Flow Chemistry

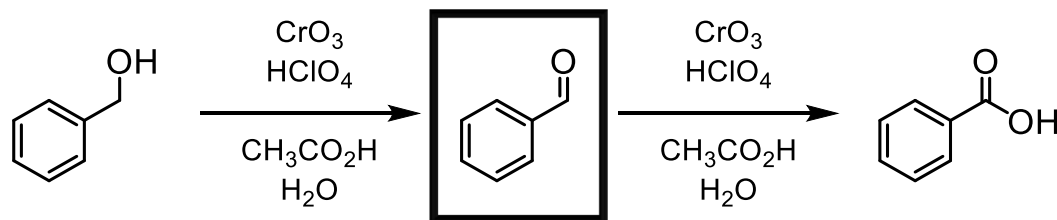
Optimization of Continuous Variables

Optimization of Discrete Variables

Automated Optimization in Flow



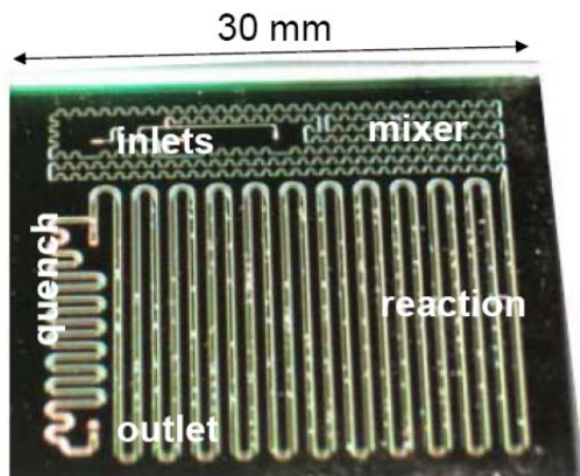
Automated Optimization in Flow: Early Examples



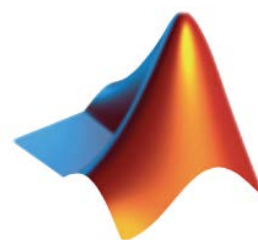
Optimization Objective = Benzaldehyde Production

Reaction Conditions Adjusted

Pump Type = Syringe Pumps
Temperature Range = -30 °C - 150 °C



Controls delivery (pumps)
Can also control temp, pressure

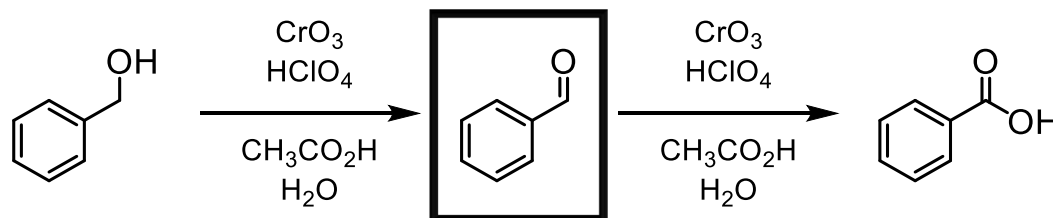


Nelder-Mead Simplex Optimization Algorithm

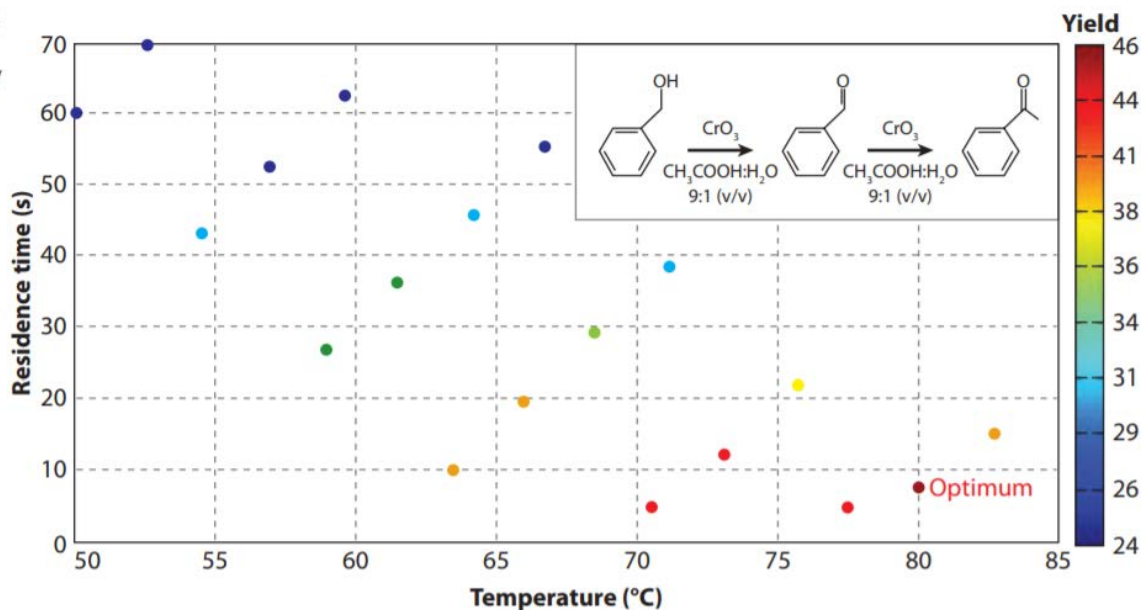
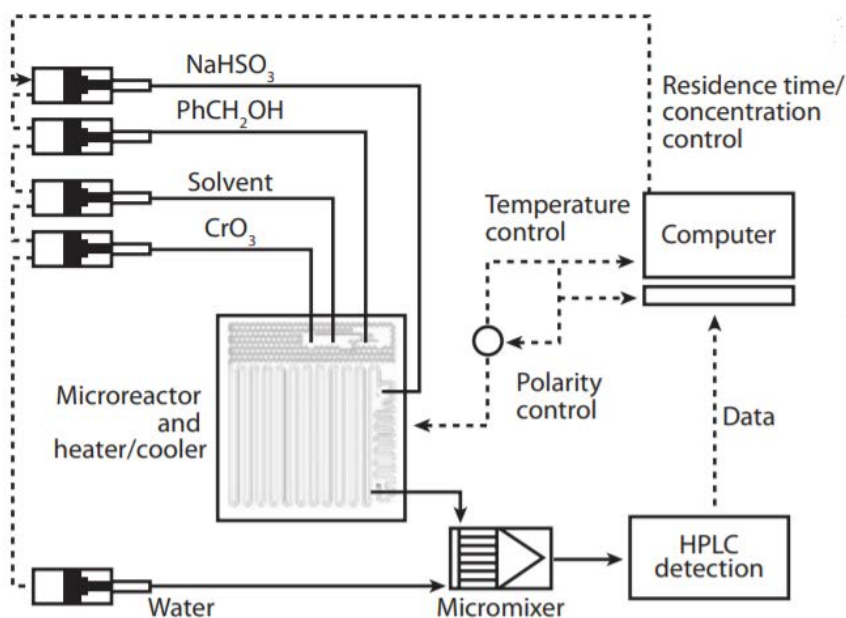
Analyzed by HPLC

Data Exported

2D Optimization of the Oxidation of Benzyl Alcohol



Optimization Objective = Benzaldehyde Production



Initial Conditions: 50 °C, 60 s reaction time, 1.0 equiv. CrO₃, 8 mM benzyl alcohol, 21 % yield

2D Optimized Conditions: 80 °C, 8 s reaction time, 1.0 equiv. CrO₃, 8 mM benzyl alcohol, 46 % yield

Nelder-Mead Simplex Optimization Algorithm

Define a simplex with $n+1$ vertices

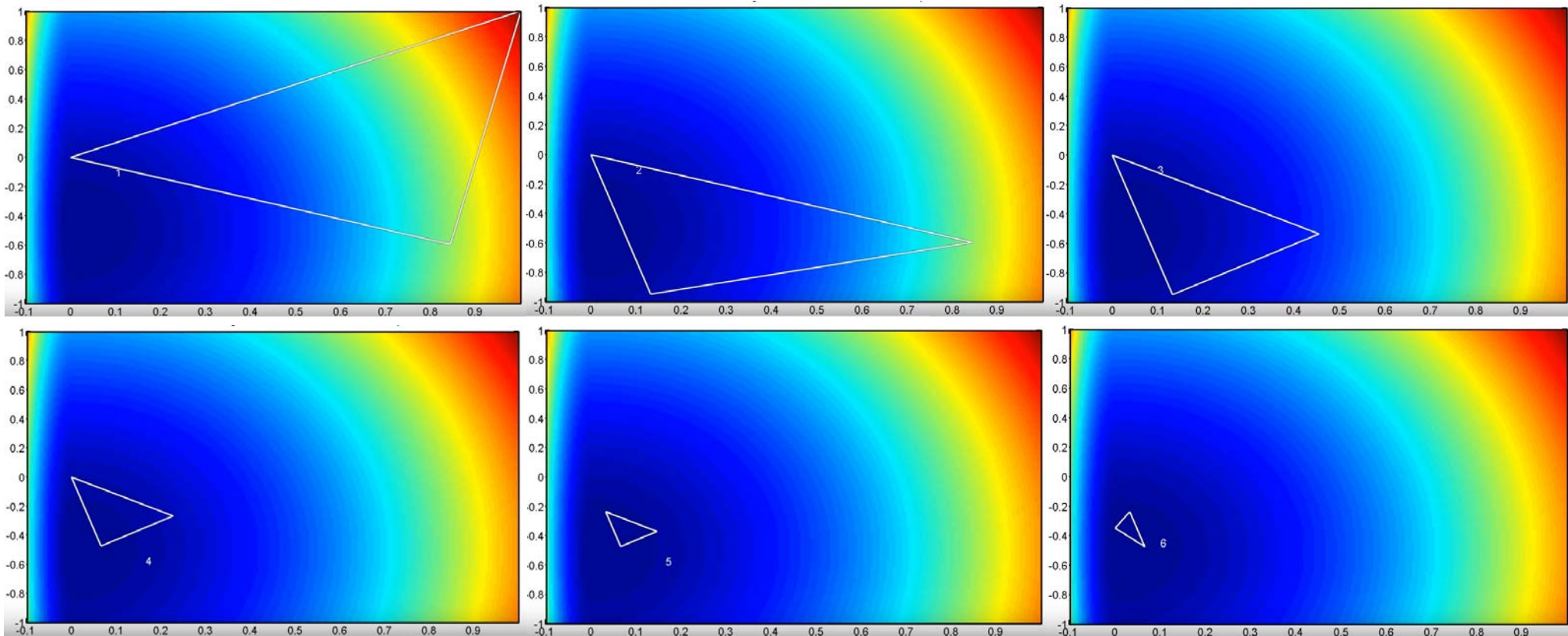
Vertices are ordered (l, m, h)

Calculate the Centroid

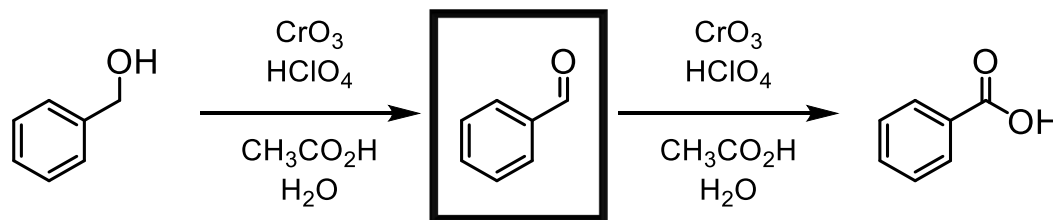
Calculate a new simplex by moving the worst vertex (l)

If an improved value for the simplex is not identified, the second worst vertex (m) moves

If an improved value for the simplex is still not identified, the maximum is surrounded and the simplex shrinks towards the best (h) vertex.



4D Optimization of the Oxidation of Benzyl Alcohol



Optimization Objective = Benzaldehyde Production

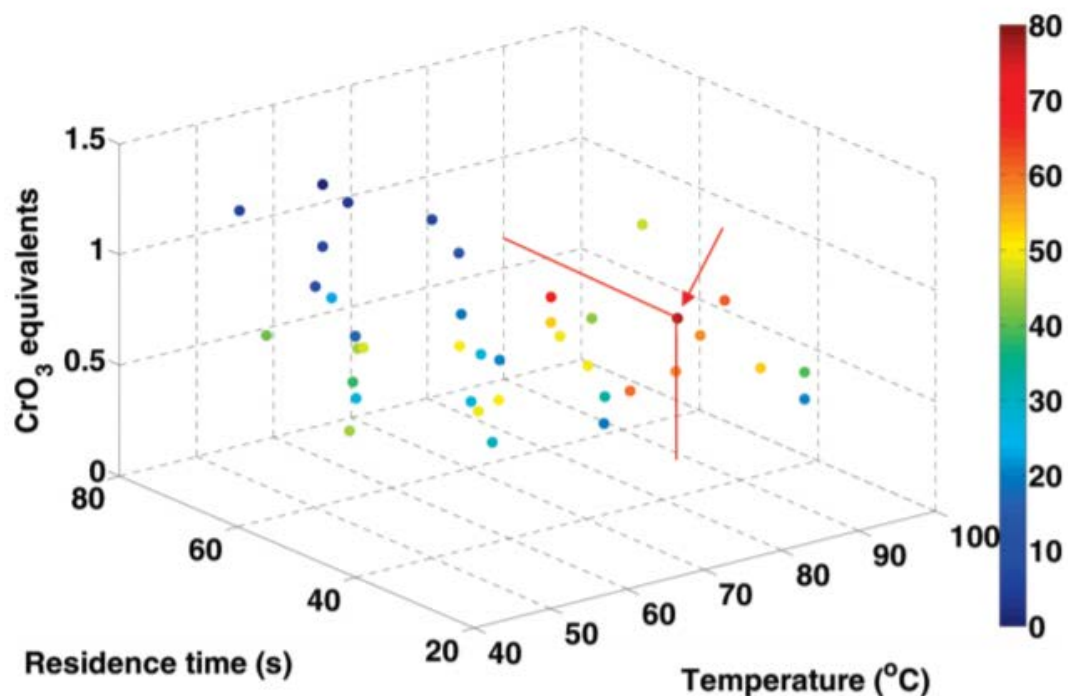
Optimization Parameters

CrO₃ concentration

Benzyl alcohol concentration

Reaction time

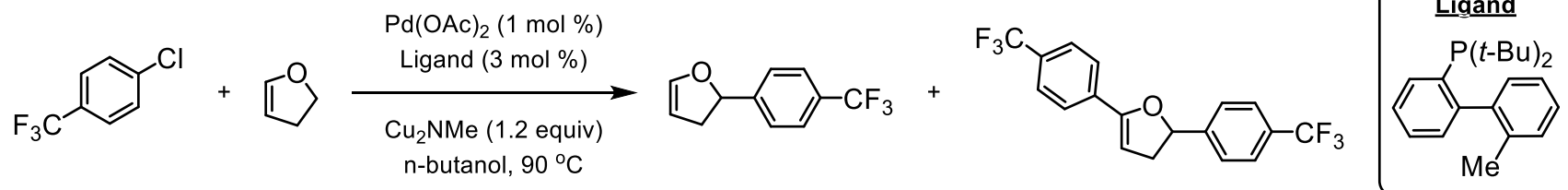
Temperature



Initial Conditions: 50 °C, 60 s reaction time, 1.0 equiv. CrO₃, 8 mM benzyl alcohol, 21 % yield

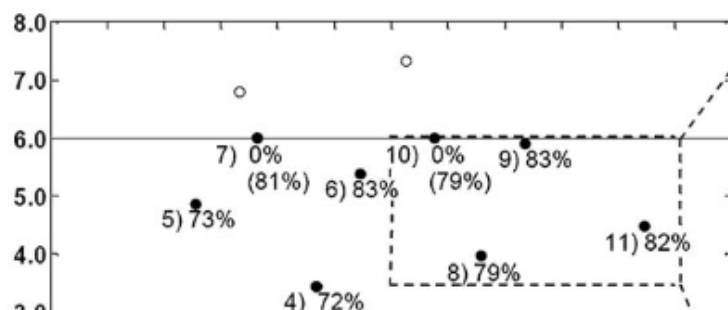
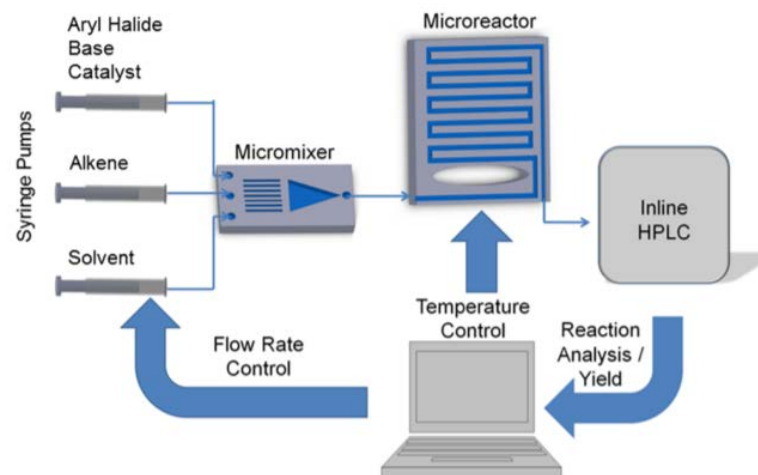
4D Optimized Conditions: 88 °C, 48 s reaction time, 0.65 equiv. CrO₃, 8.2 mM benzyl alcohol, 80 % yield

Heck Reaction Autonomous Optimization



Solvent, Ligands, and Pd Sources (discrete variables) screened prior to automated flow optimization to find conditions that did not cause clogging.

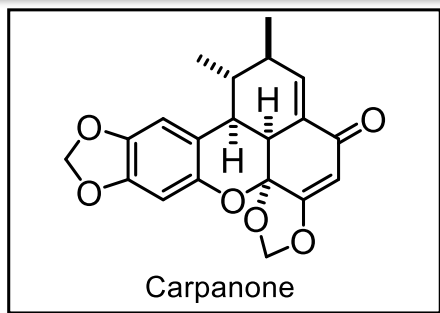
Automated Optimization Variables: Residence time and alkene equivalents (capped at 6 equiv. with use of penalty function)



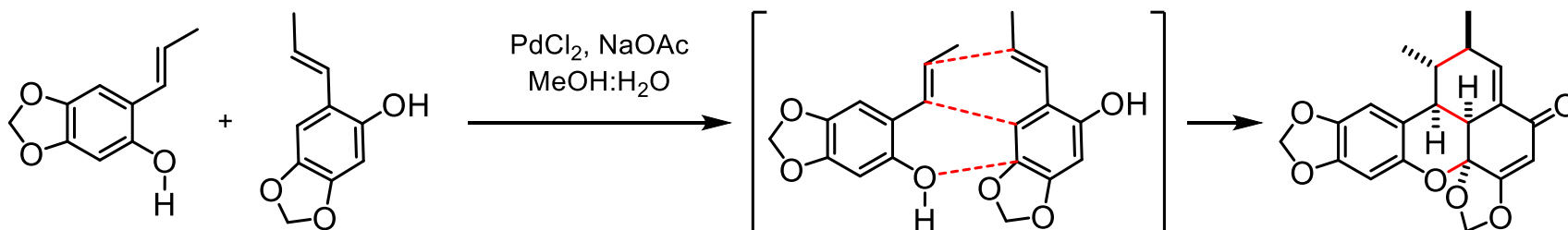
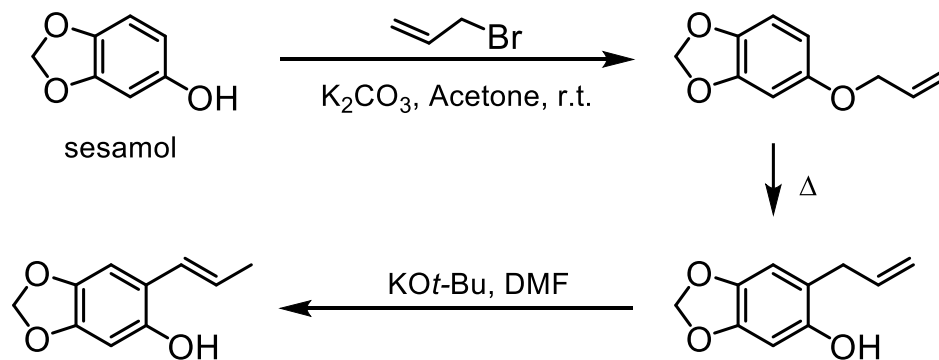
19 experiments to optimal conditions: 5.5 min residence time, 5.0 equiv. alkene

Successfully scaled up 50 times

Total Synthesis of Carpanone



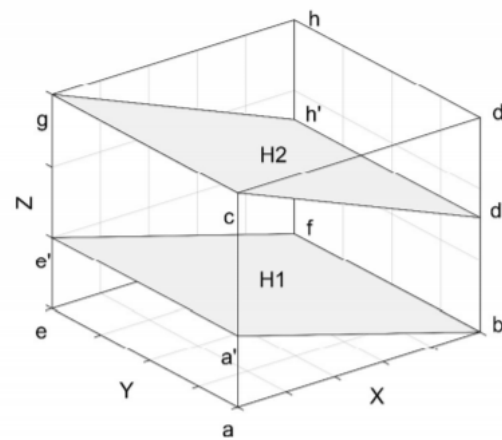
Lignin-Type natural product (racemic)
Many syntheses (first by Chapman in 1971)
No biological activity



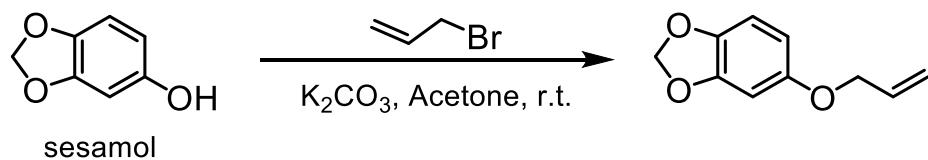
Is it possible to create a self-optimizing system for the continuous production of Carpanone?

Strategy

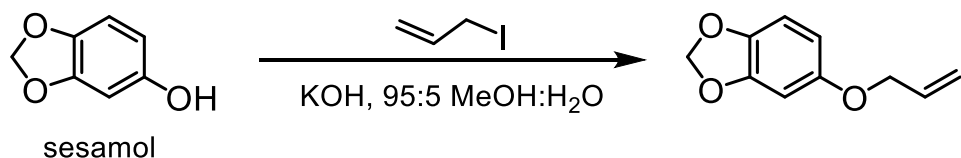
Use of inline NMR / online HPLC for feedback
Modified NMS algorithm with dimensionality
reduction and golden section search algorithm



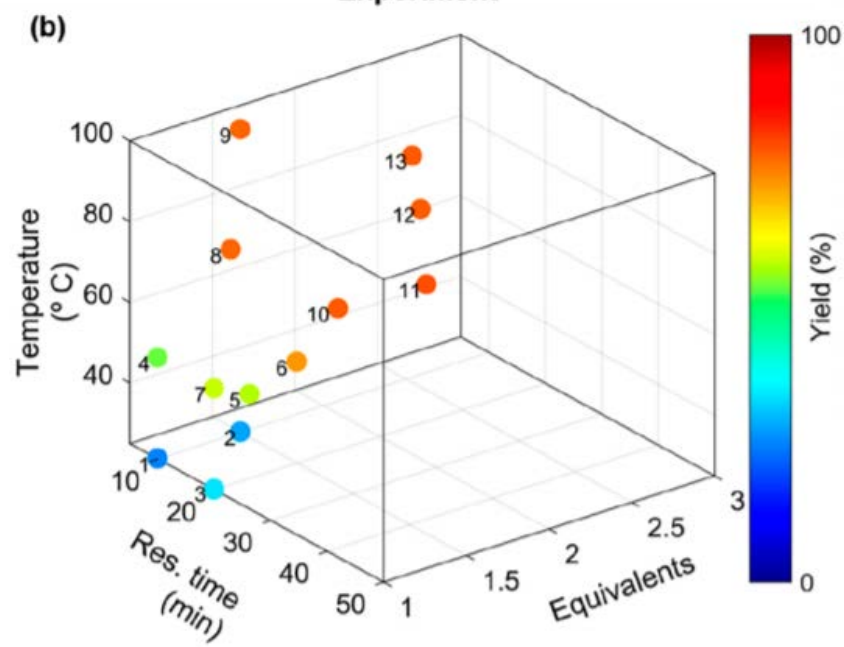
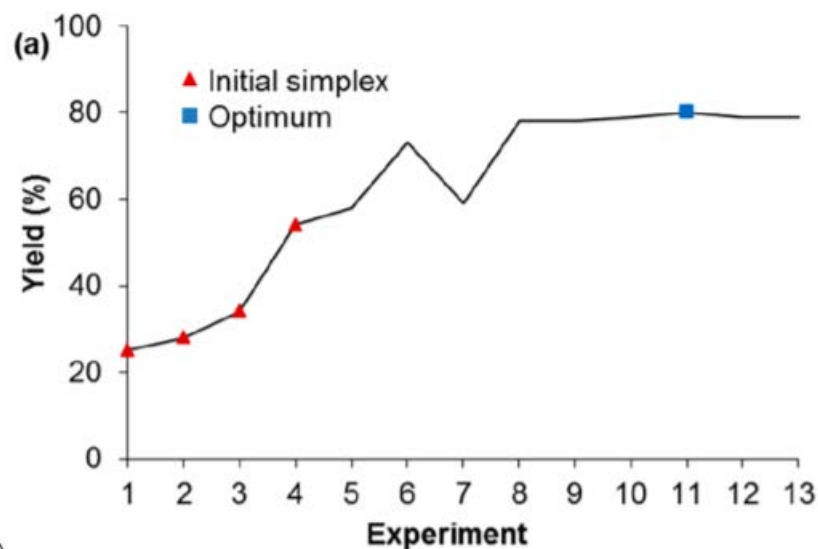
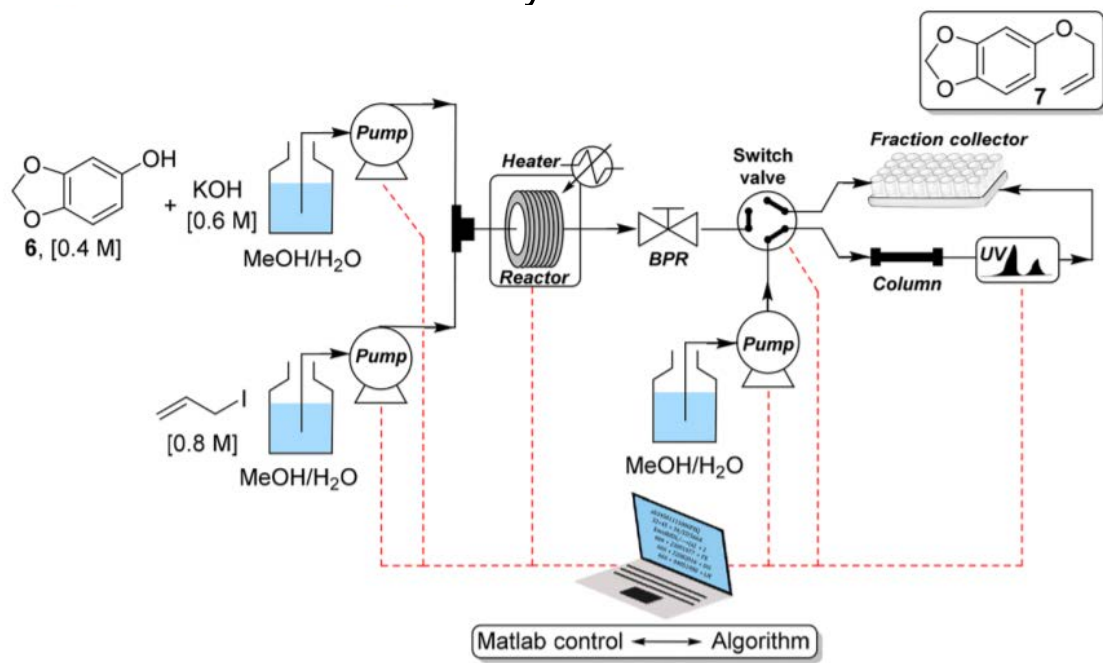
Optimization of the Allylation of Sesamol



Solid K_2CO_3 and KBr not amenable to flow

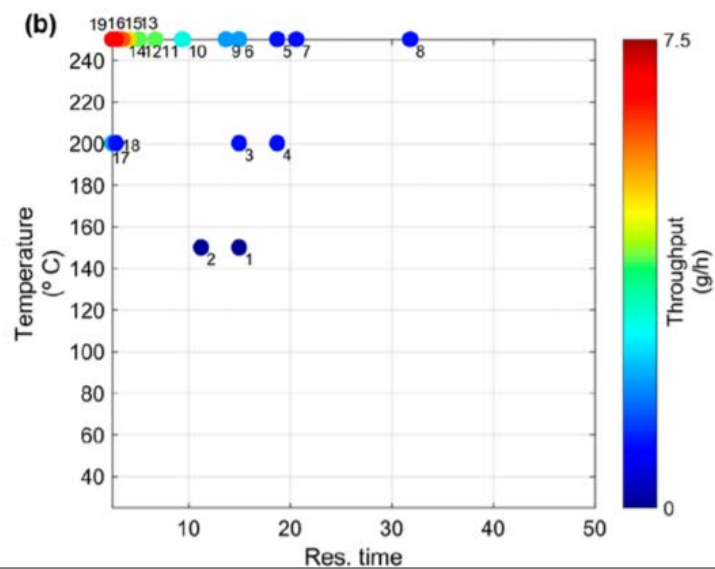
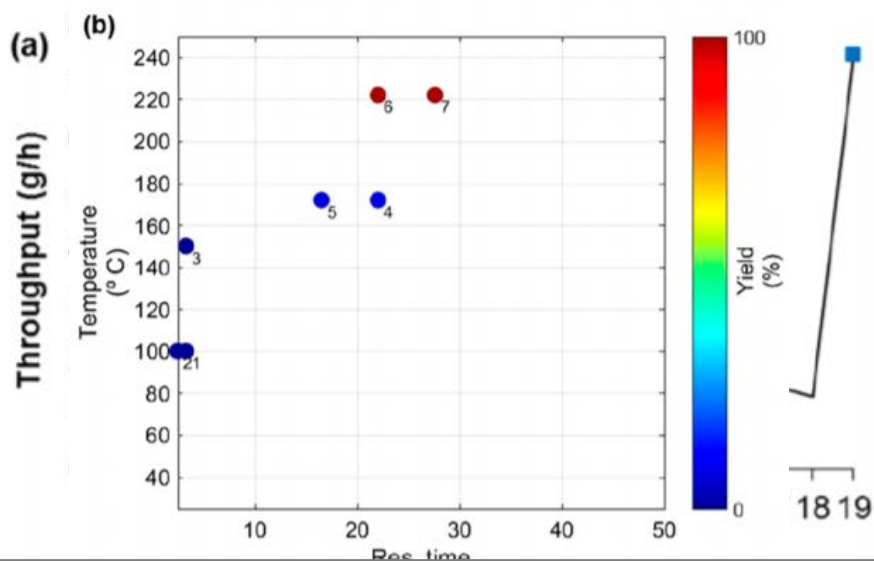
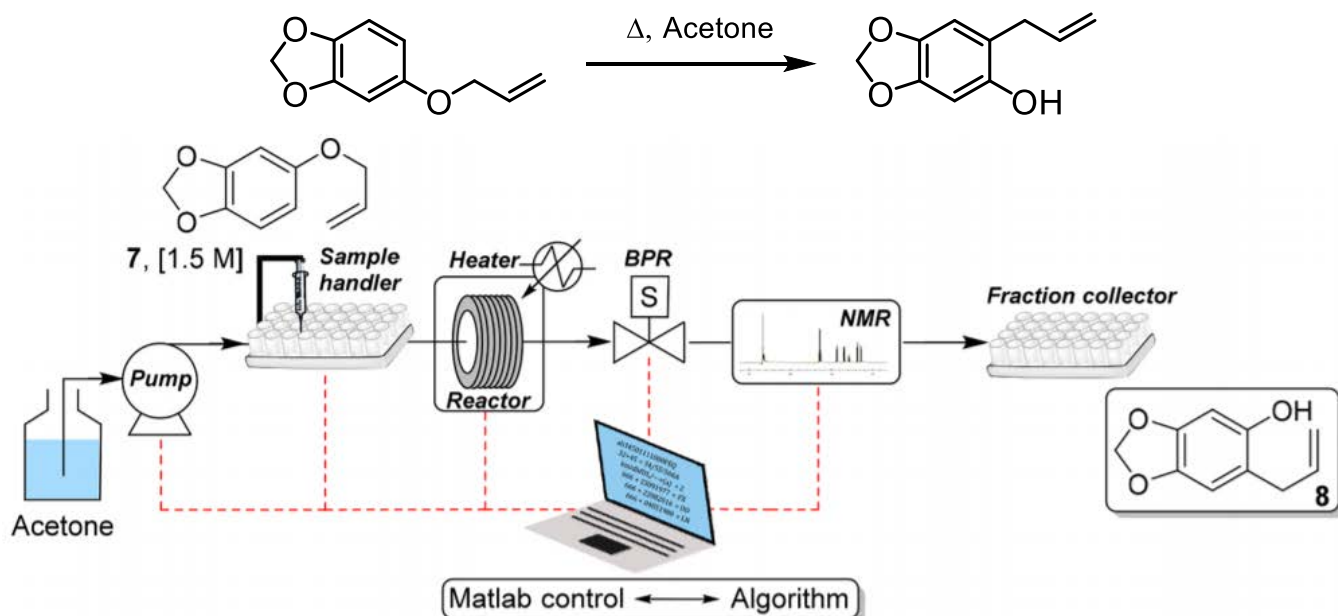


"Flow Friendly" conditions



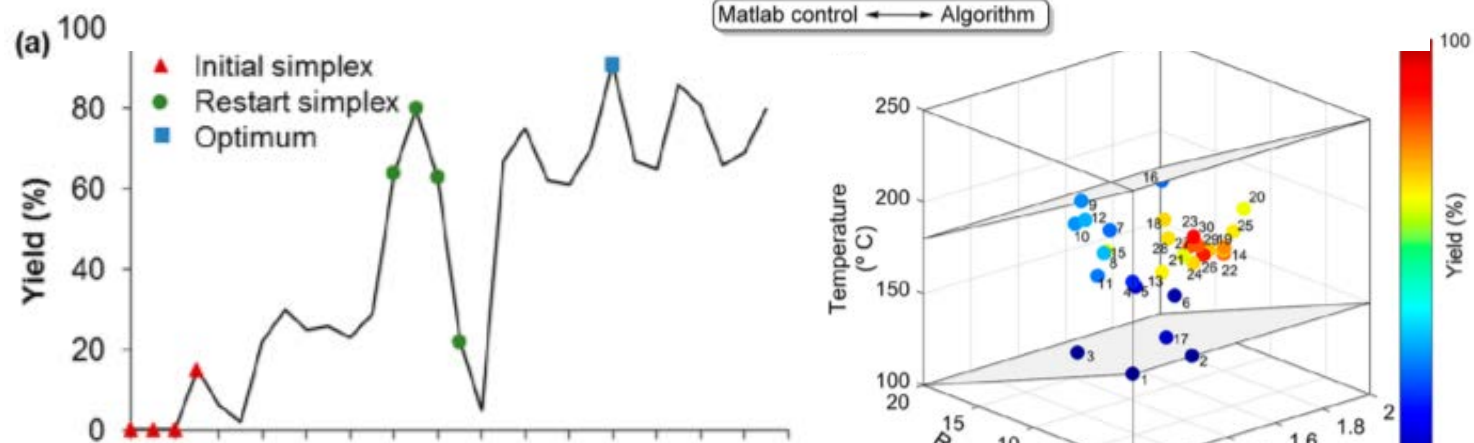
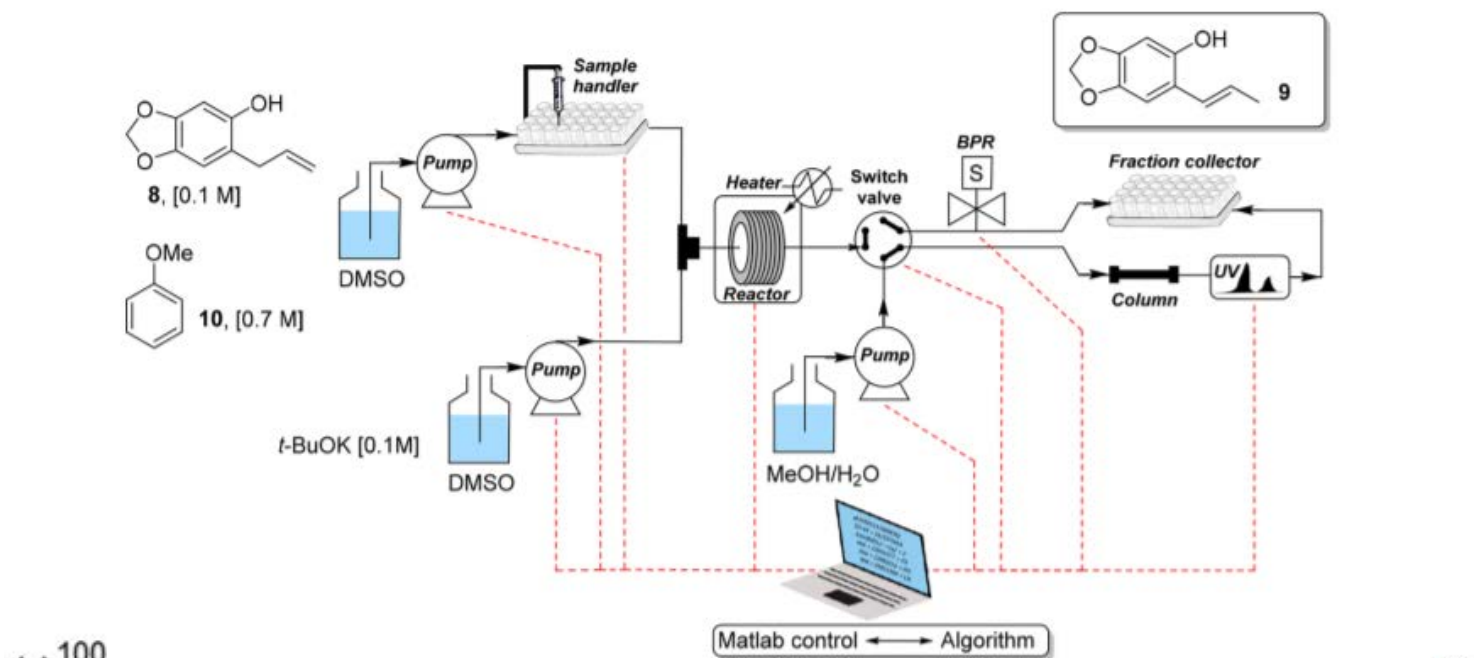
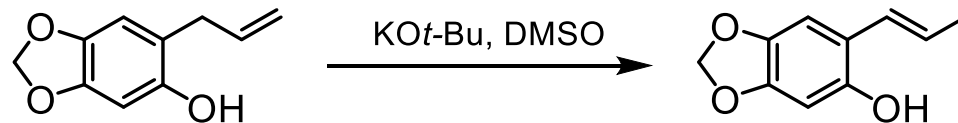
Final Conditions: 75 °C, 33.3 min residence time, 1.83 equiv. of allyl iodide, 80 % yield

Claisen Rearrangement Optimization



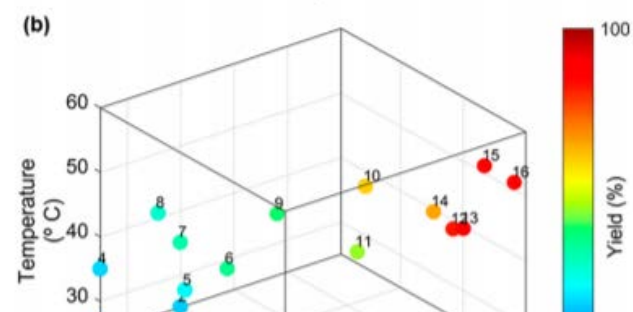
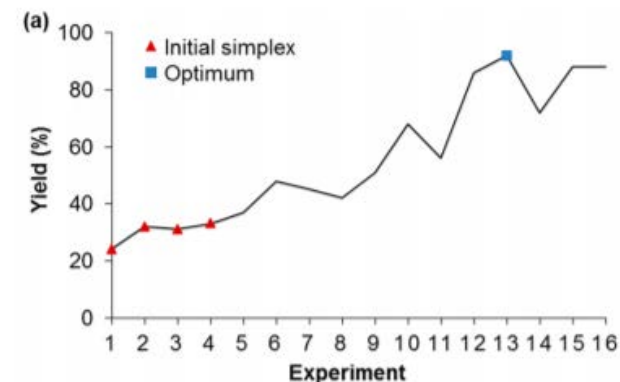
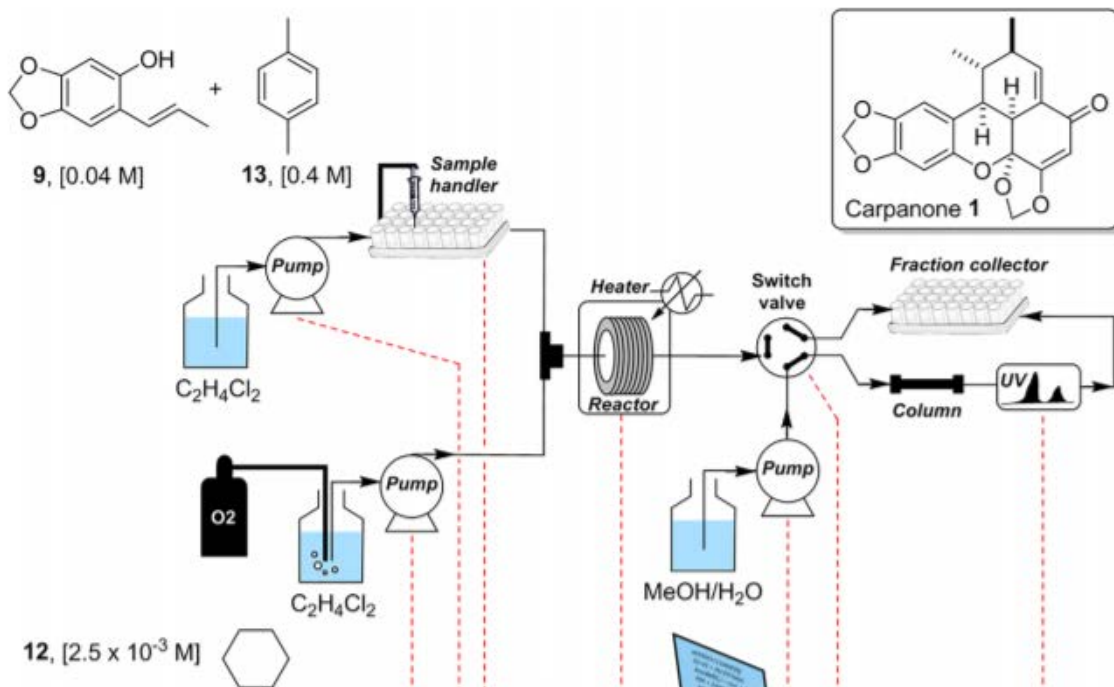
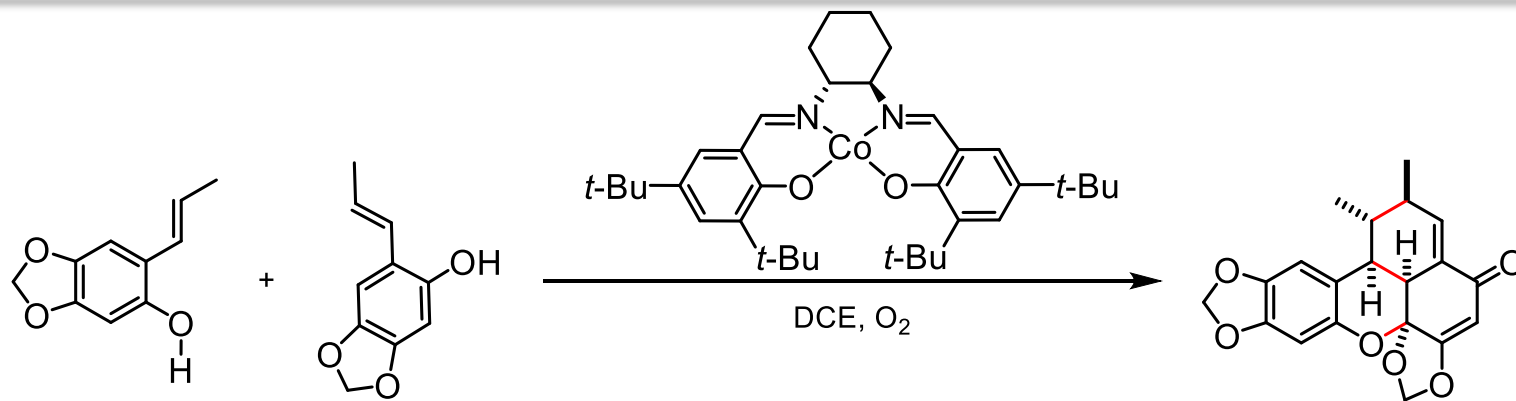
Final Conditions: 250 °C, 2.5 min residence time, 1.83 equiv. of allyl iodide, 7.5 g / hr

Optimization of the Isomerization of Allyl Sesamol



Final Conditions: 204 °C, 3.7 min residence time, 1.38 equiv. of KOt-Bu, 91 % yield

Optimization of the Oxidative Coupling to form Carpanone



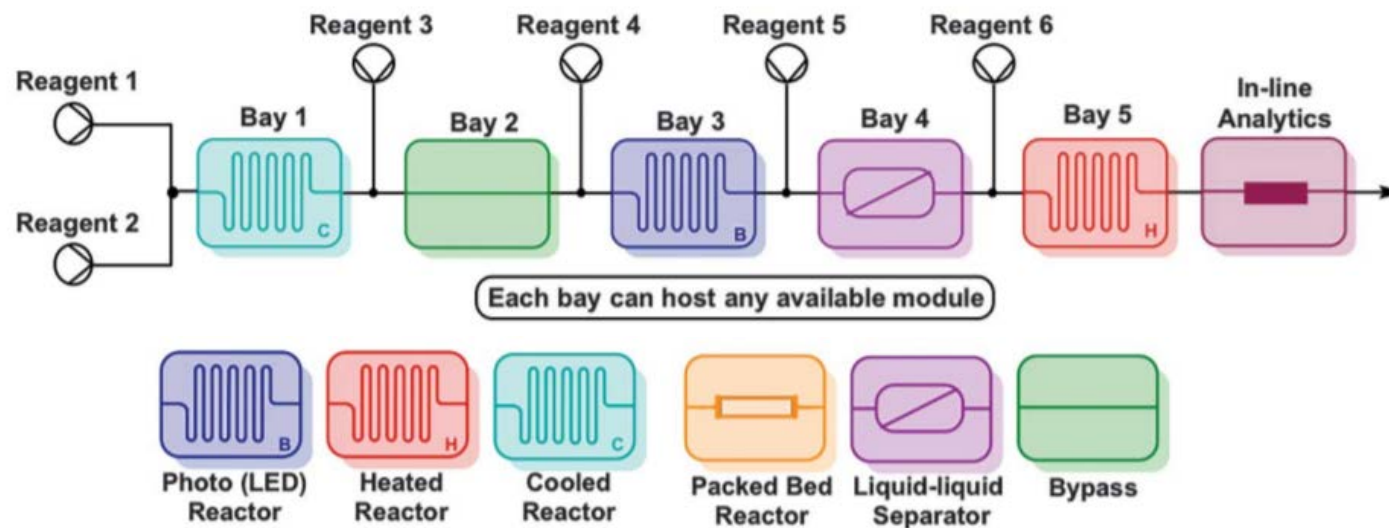
Final Conditions: 40 °C, 40.2 min residence time, 10 mol % catalyst, 92 % yield

67 % overall yield with 66 experiments in the total optimization

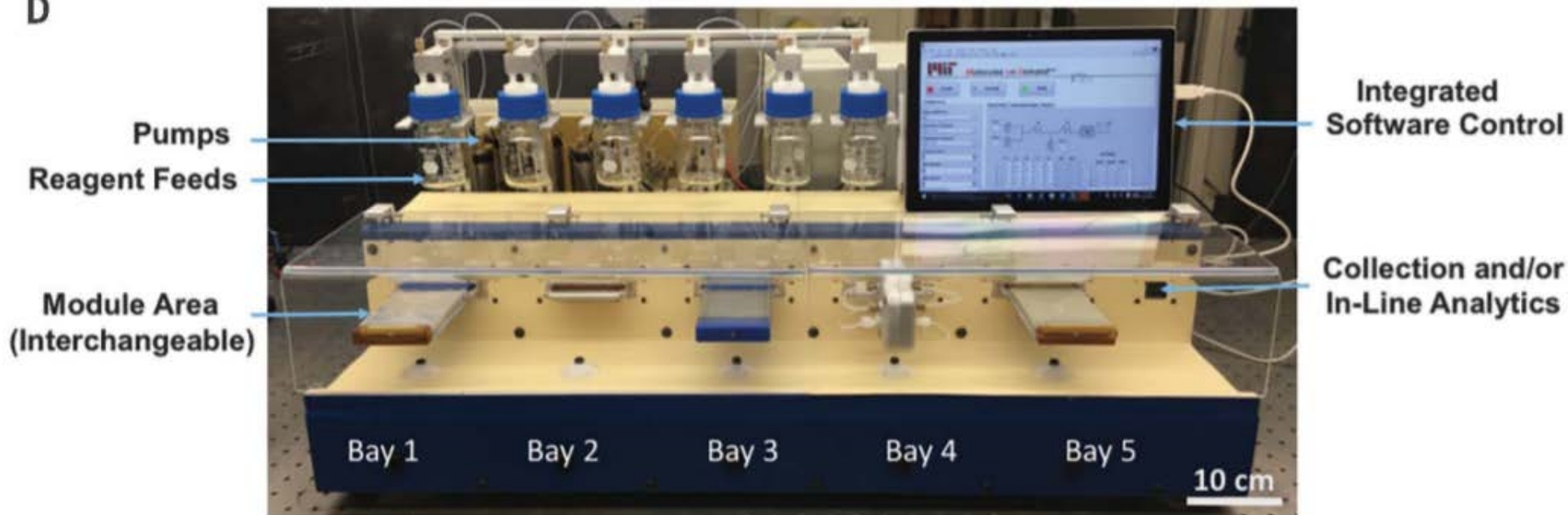
Intermission



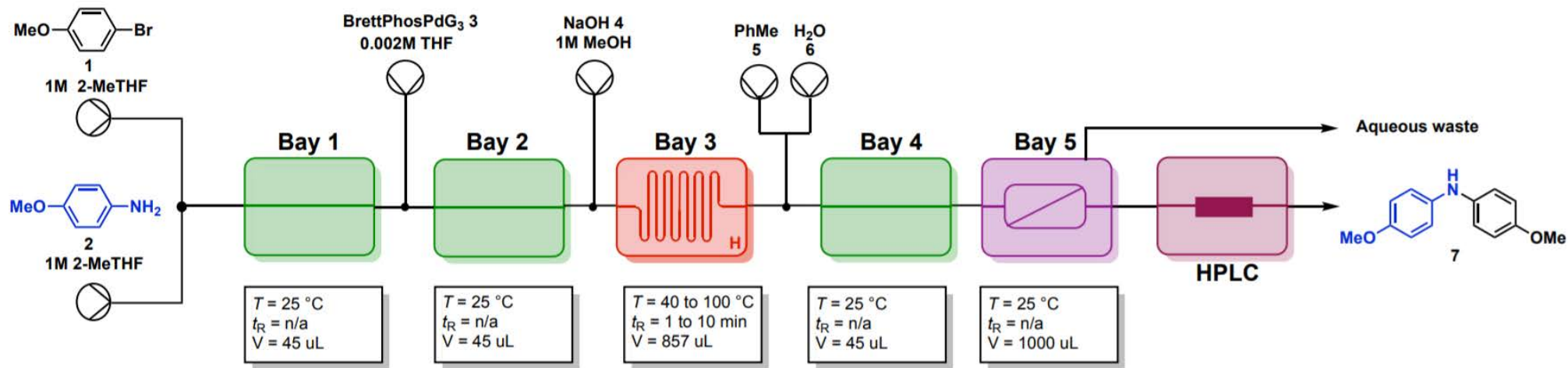
Reconfigurable system for automated optimization of diverse chemical reactions



D



Buchwald-Hartwig Coupling



Optimization Target

Optimization for the conversion of 1

Adjustable Parameters

Temperature (bay 3): 40 to 100 °C

Flow Rates (P_1 , P_2 , P_4): 16.3 to 65.9 $\mu\text{L}/\text{min}$

Catalyst Loading: 1 to 2 mol %

Optimization:

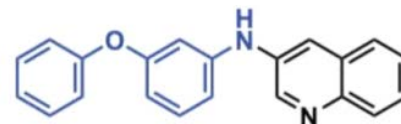
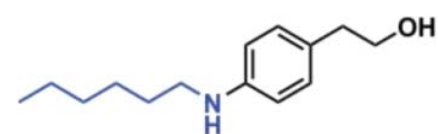
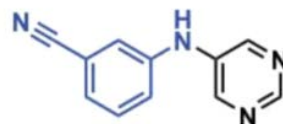
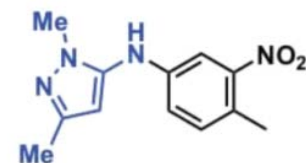
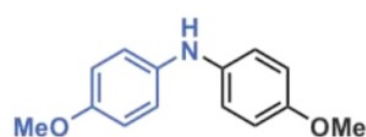
32 Experiments (21 h run time)

1.2 equiv. 2

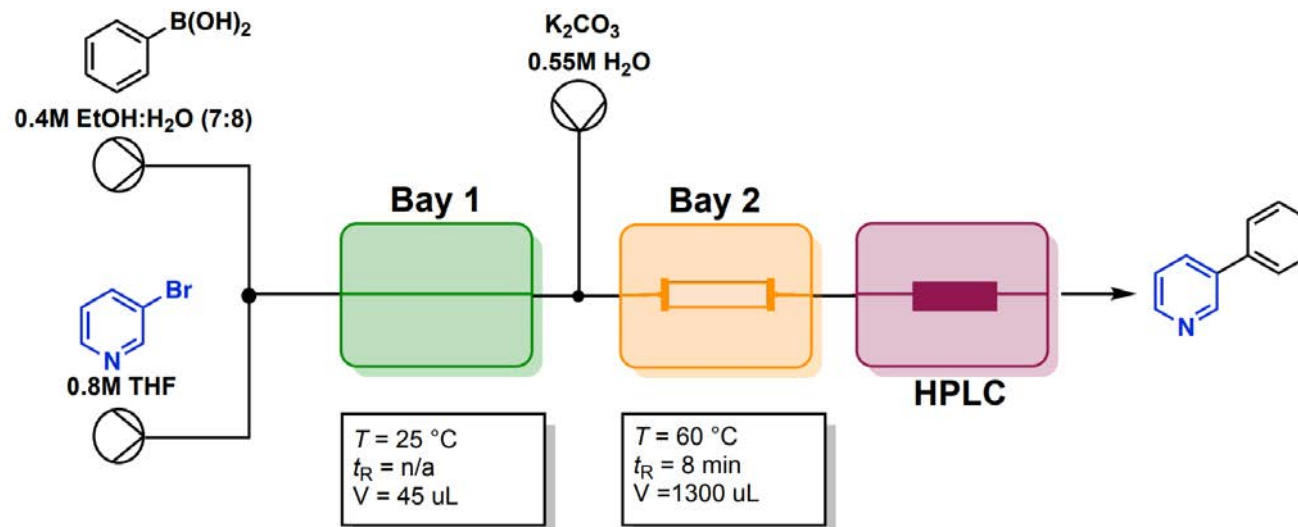
1.4 mol % catalyst

1.5 equiv base

100 °C



Suzuki Coupling with Heterogenous Catalyst Automatic Optimization



Optimization Target

Optimization for the production of desired product

Adjustable Parameters

Temperature (bay 2): 40 to 100 °C

Flow Rate (P_1, P_2): 32.5 to 325 $\mu\text{L} / \text{min}$

Flow Rate (P_3): 65 to 650 $\mu\text{L} / \text{min}$

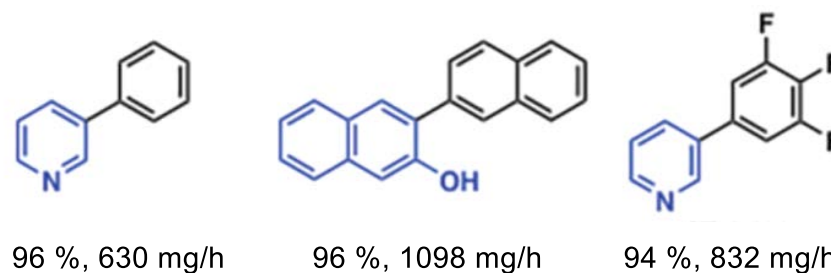
Optimization:

30 Experiments (8 h run time)

1.0 equiv. boronic acid

4 equiv. K2CO3

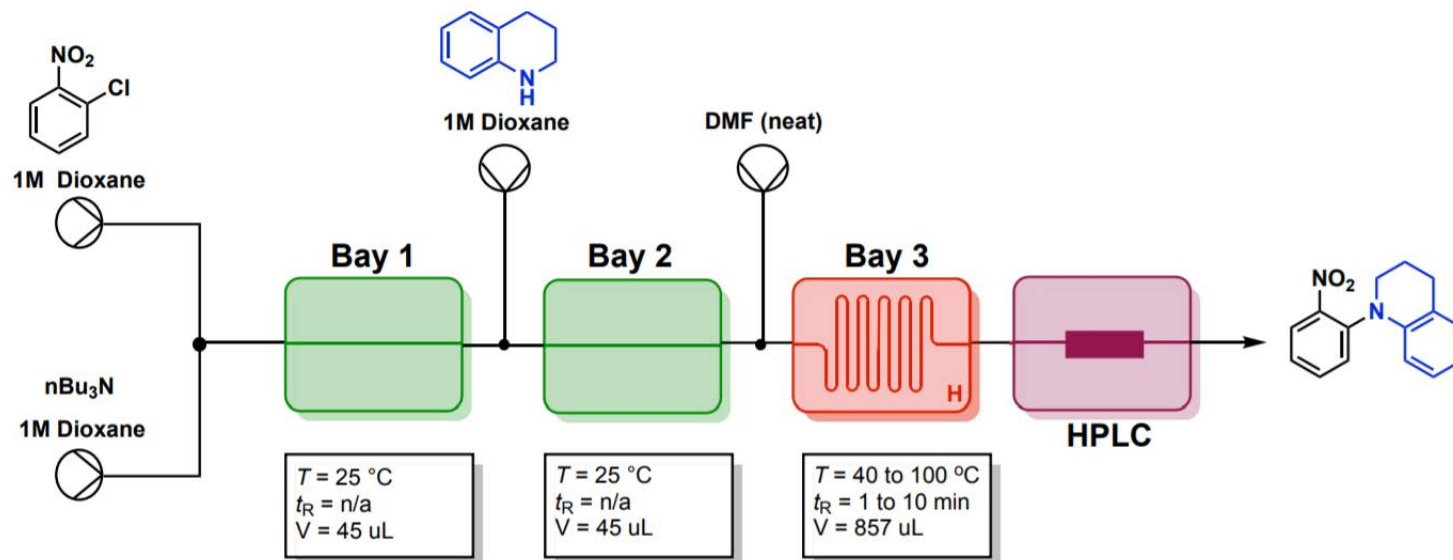
63 °C



A total of nine examples

>1 g of each example completed in 8 h

S_NAR Automatic Optimization



Optimization Target

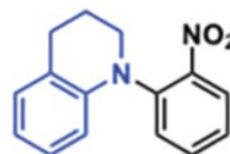
Optimization for formation of desired product

Adjustable Parameters

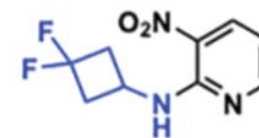
Temperature (bay 3): 40 to 100 °C
Flow Rate (P_1, P_2, P_3): 21 to 214 / min

Optimization:

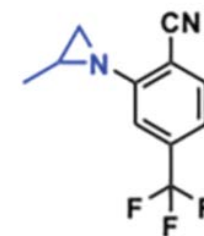
33 Experiments (14 h run time)
10 equiv. tributyl amine
1 equiv. aryl chloride
1 equiv. amine
100 °C



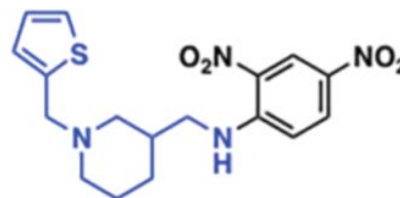
94 %, 320 mg/h



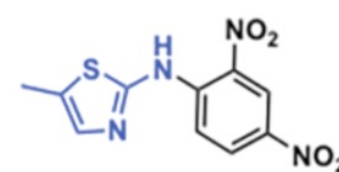
89 %, 271 mg/h



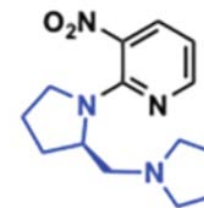
97 %, 292 mg/h



99 %, 496 mg/h



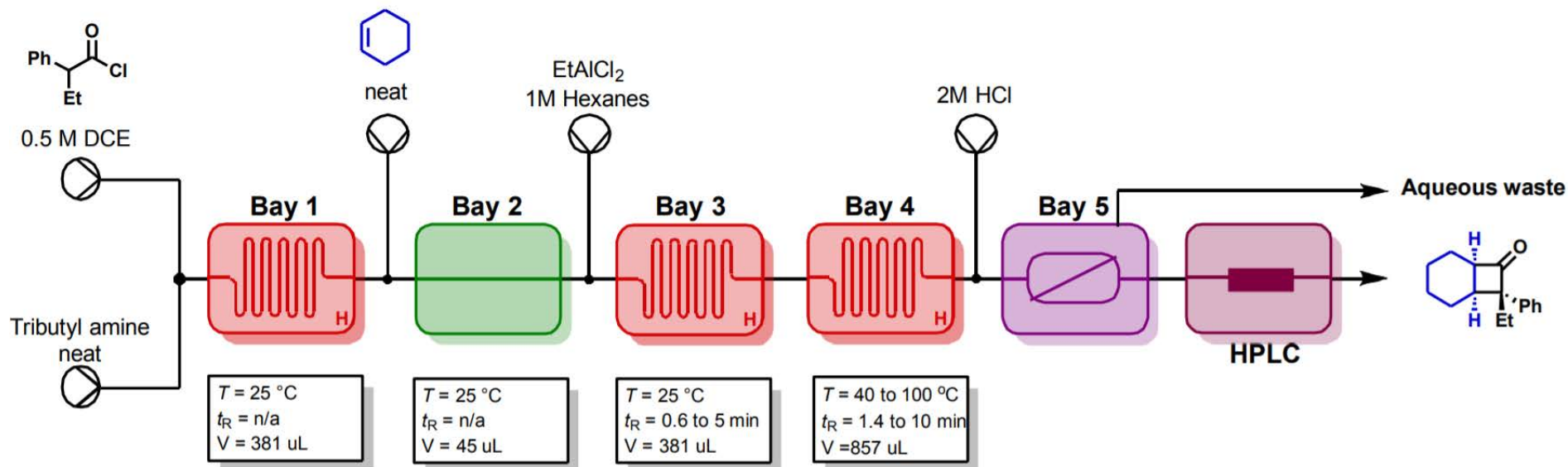
92%, 343 mg/h



96 %, 253 mg/h

10 examples, 10 mg of each generated in 17 min

Automatic Optimization of a Multi-step Reaction



Optimization Target

Optimization for formation of desired product

Adjustable Parameters

Temperature (bay 4): 40 to 100 °C

Flow Rate (P₁): 51 to 382 / min

Flow Rate (P₂): 6.4 to 43.8 / min

Flow Rate (P₃): 2.8 to 21 / min

Flow Rate (P₄): 25.5 to 199 / min

Optimization:

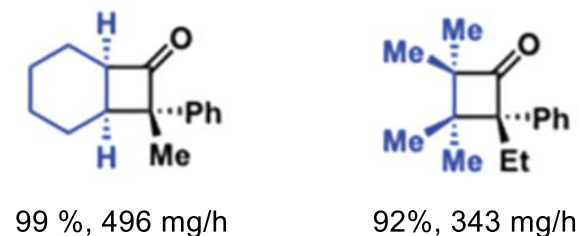
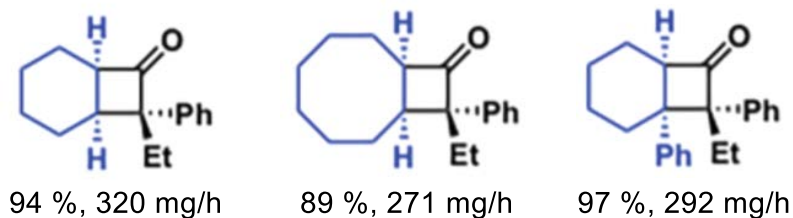
45 Experiments (34 h run time)

1.2 equiv. cyclohexene

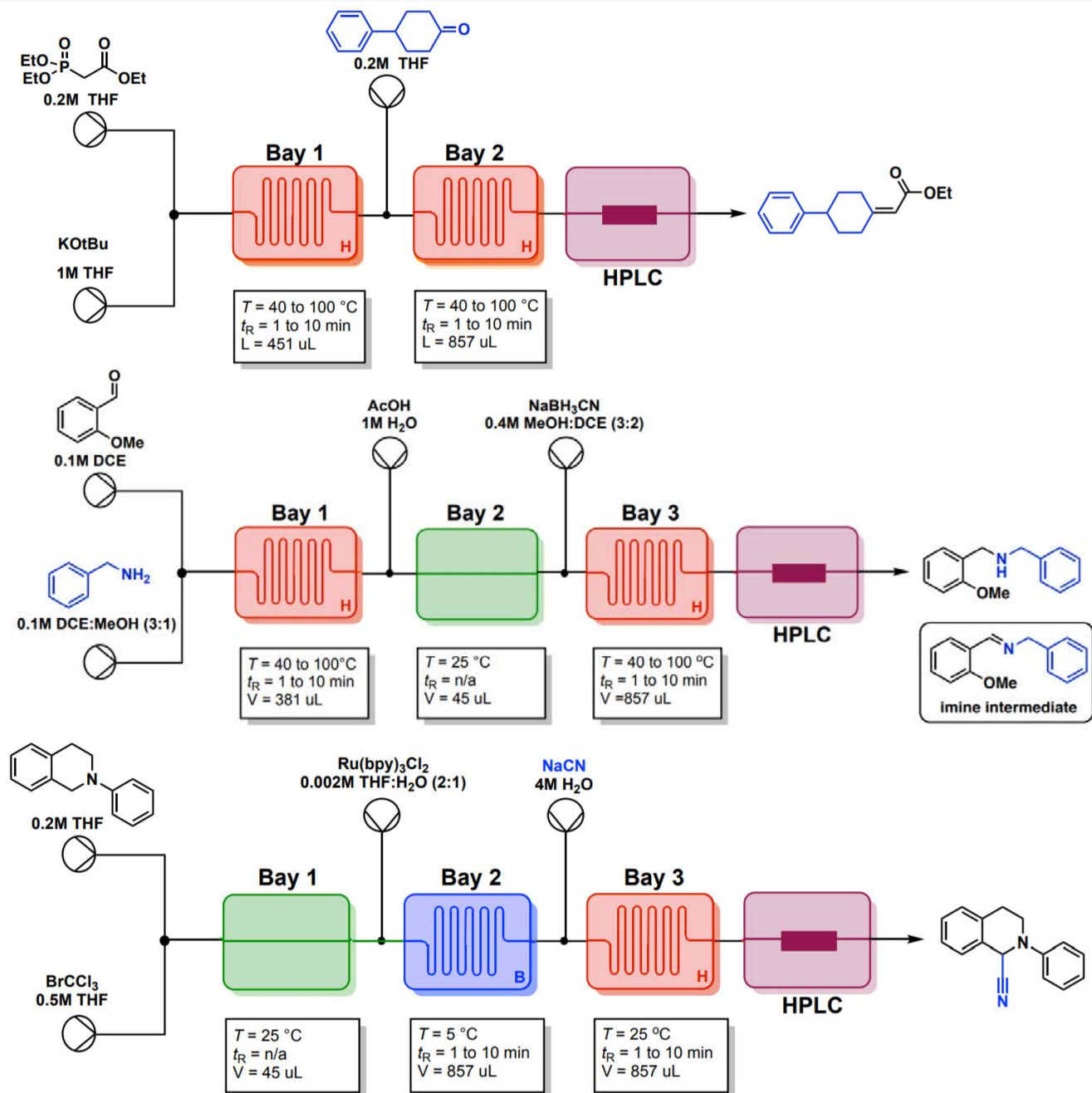
1 equiv. tributylamine

6.7 equiv. EtAlCl₂

78 °C (bay 4)



Additional Automatic Optimizations



5 variables optimized
33 experiments in total
10 hr to optimize

5 variables optimized
33 experiments in total
14 hr to optimize

3 variables optimized
33 experiments in total
7 hr to optimize

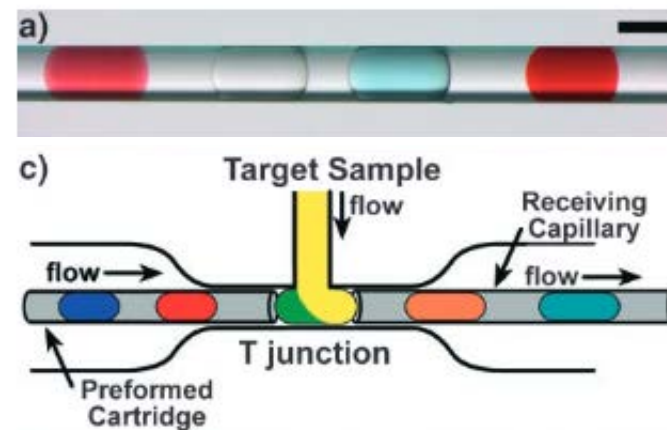
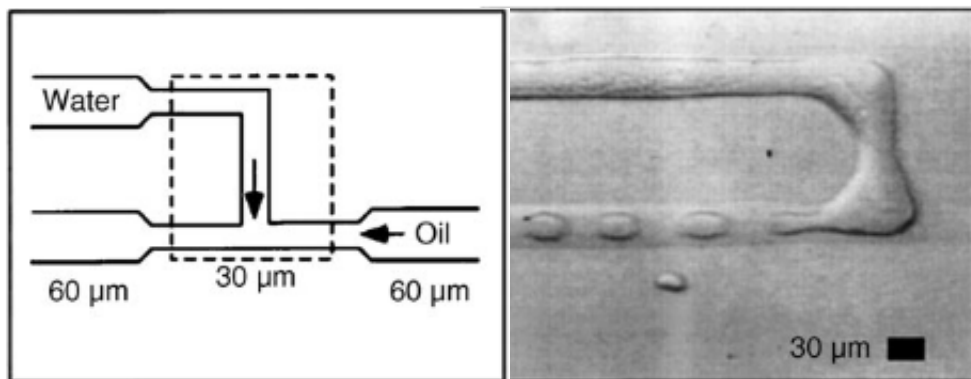
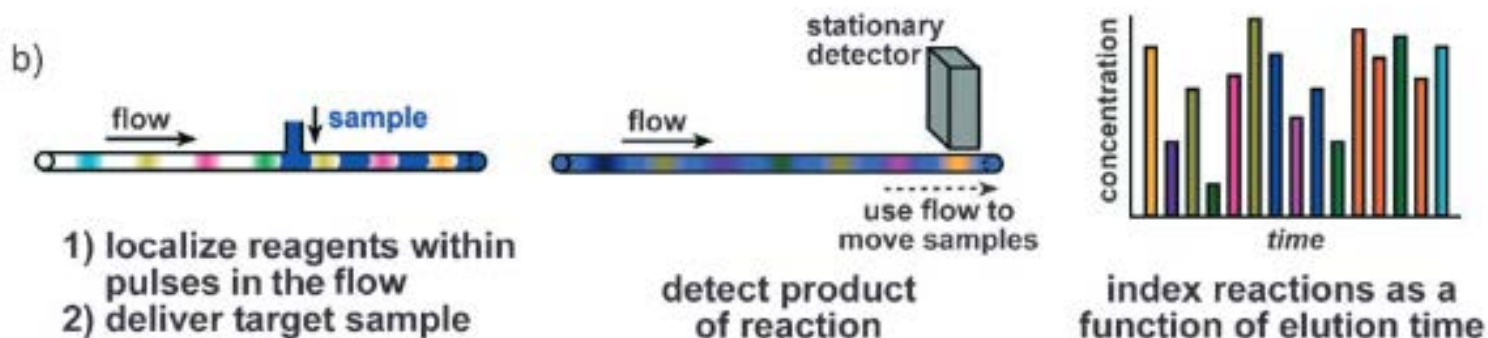
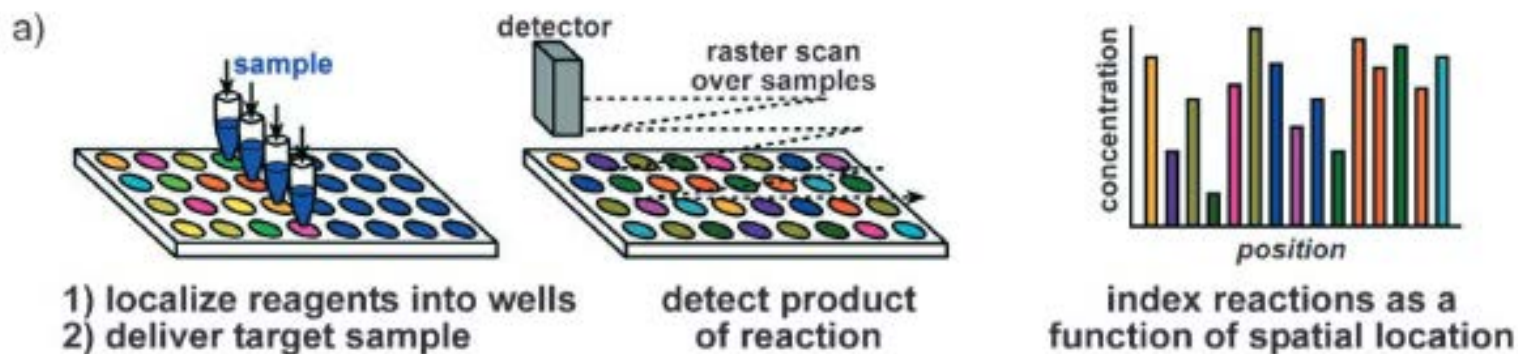
Outline Slide

Anatomy of Flow Chemistry

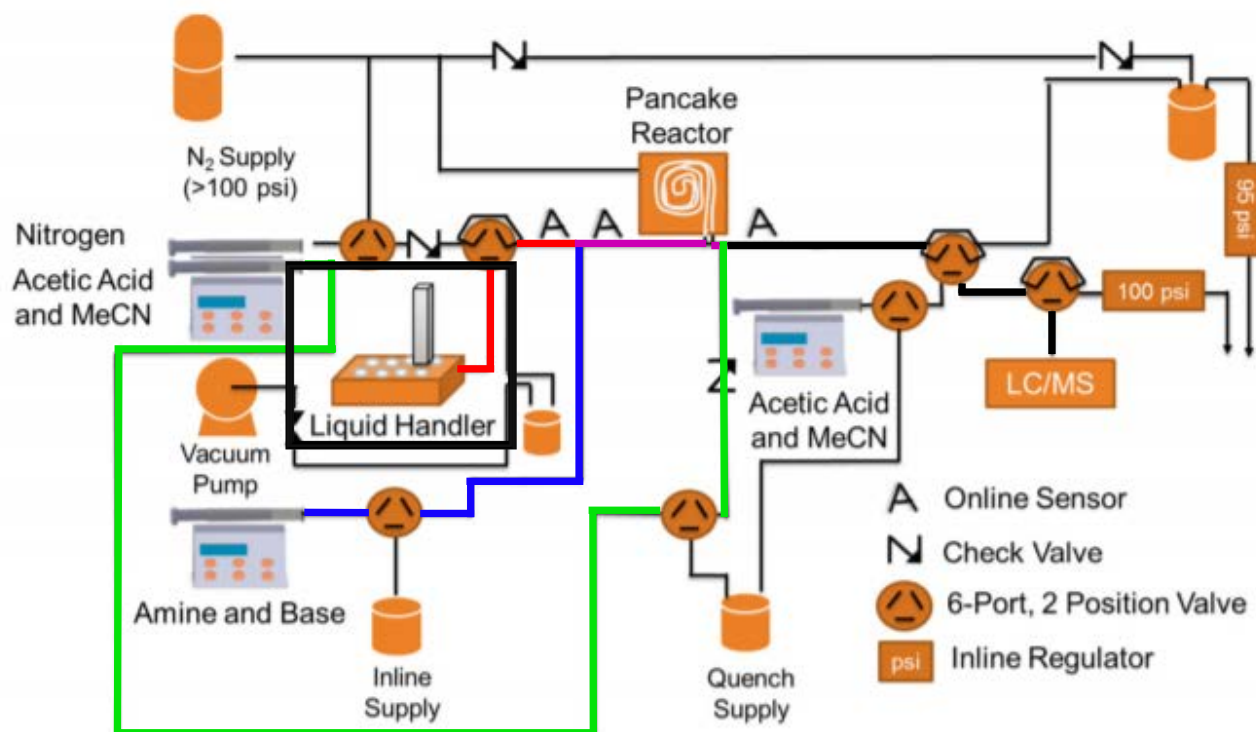
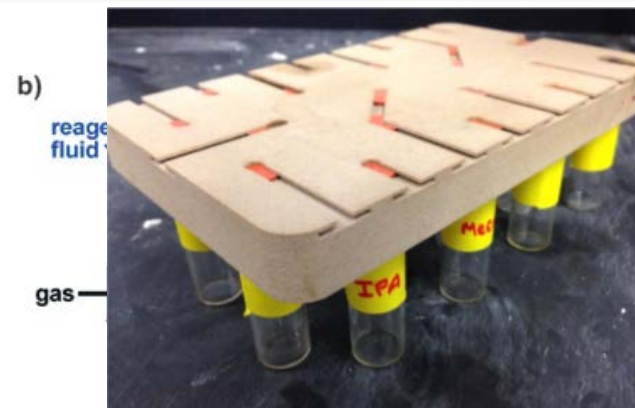
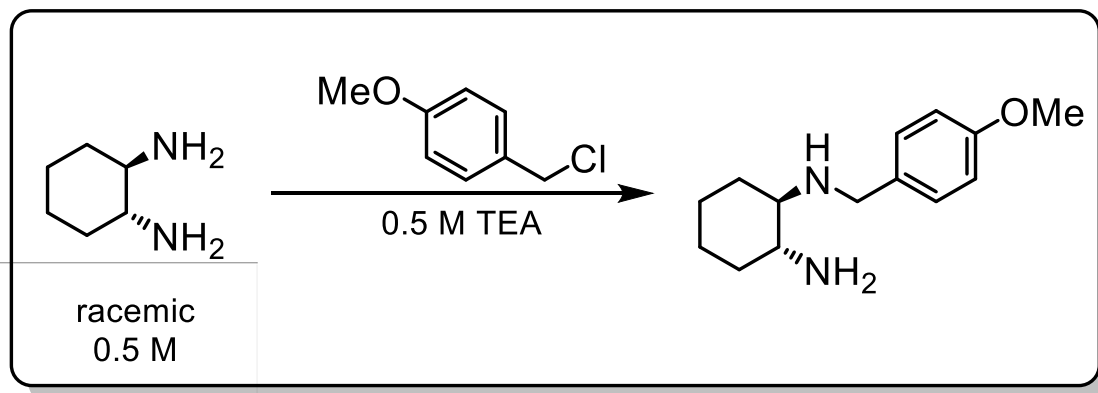
Optimization of Continuous Variables

Optimization of Discrete Variables

Reactions in Droplets

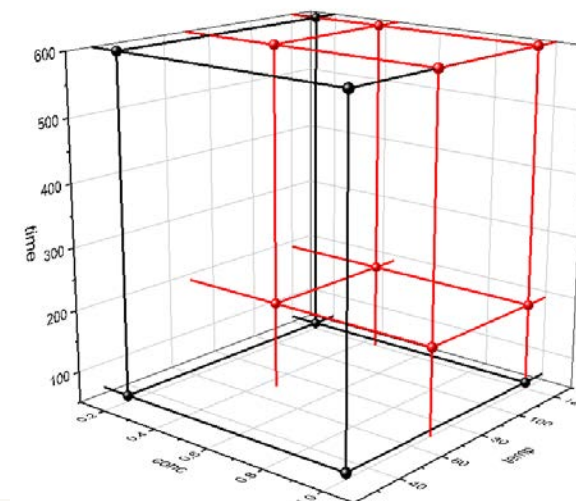
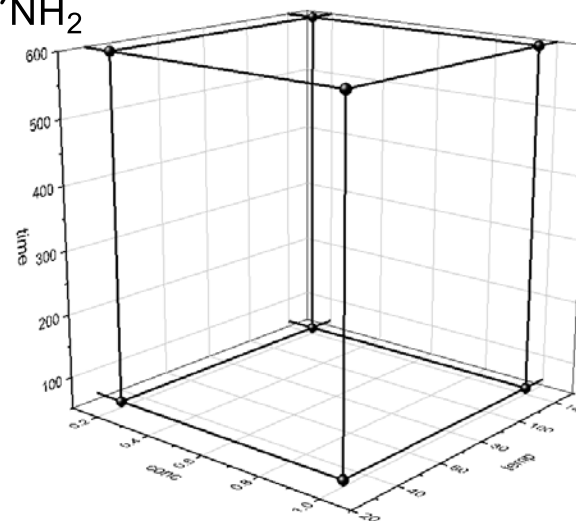
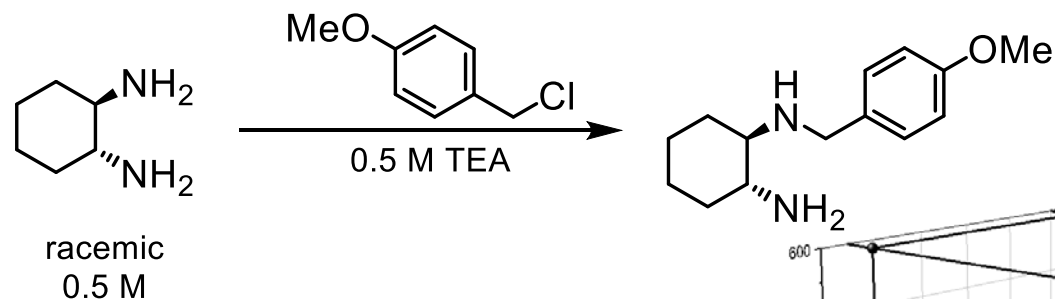


Solvent Screening in Flow



First aspirated with 30 μ L N₂
 Aliquots chosen solvent, then PMBCl, then chosen solvent again
 “Stirred” with syringe pump
 Transferred to 6-way valve
 Refractive Index Sensors the injection of TEA, diamine, and internal standard
 Quenched with 10 % AcOH in MeCN
 Sample is diverted to HPLC

Solvent Screening in Flow

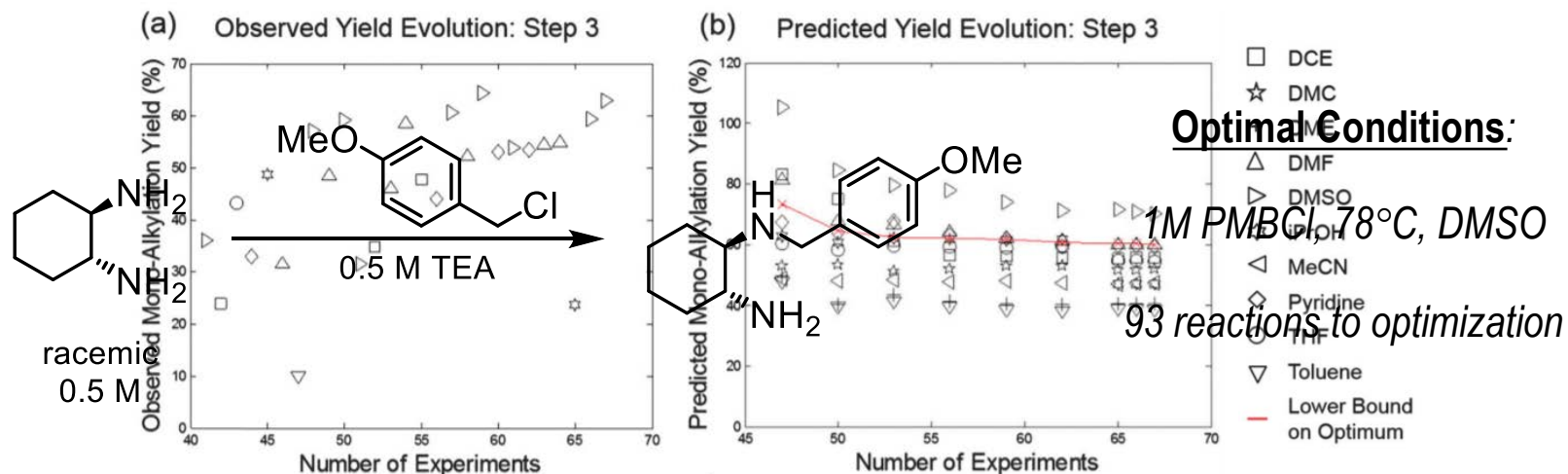


Optimization workflow:

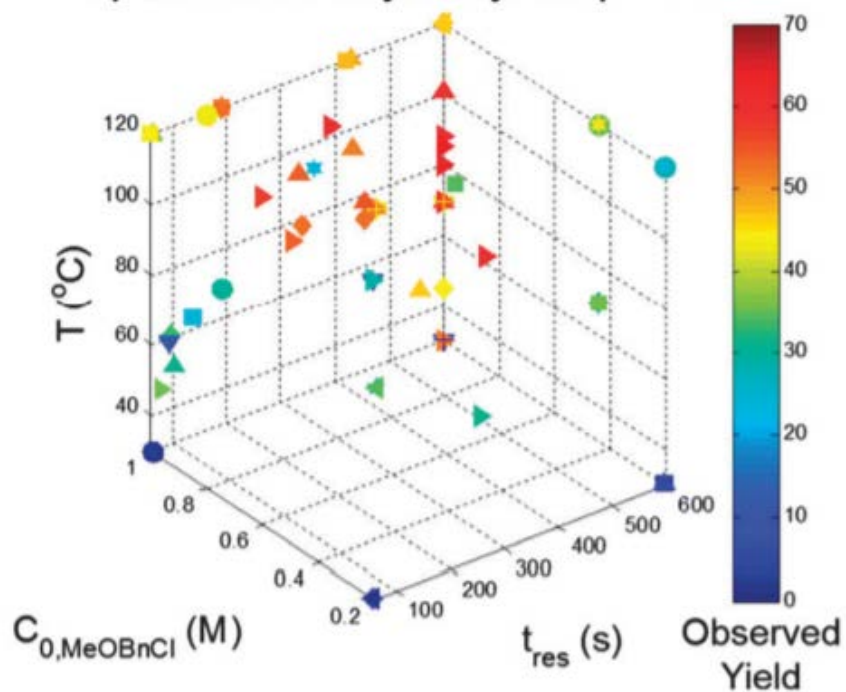
DOE approach:

- 1) Fractional factorial design (first set, 20 experiments)
 - $t_{res} = 60$ s or 600 s, temp. = 30 °C or 120 °C, C_0 PMBCl = 0.206 M or 1 M.
 - Solvents = *i*-PrOH, THF, Toluene, MeCN, DMF, DMSO, Pyridine, DMC, DME, DCE
- 2) Fractional factorial design in most promising quadrant (second set 20 experiments)
 - $t_{res} = 190$ s or 600 s, temp. = 69.2 °C or 120 °C, C_0 PMBCl = 0.444 M or 1 M.
- 3) DOE feedback search (27 experiments)
 - Minimize uncertainty for maxima in each solvent
- 4) Gradient Optimization

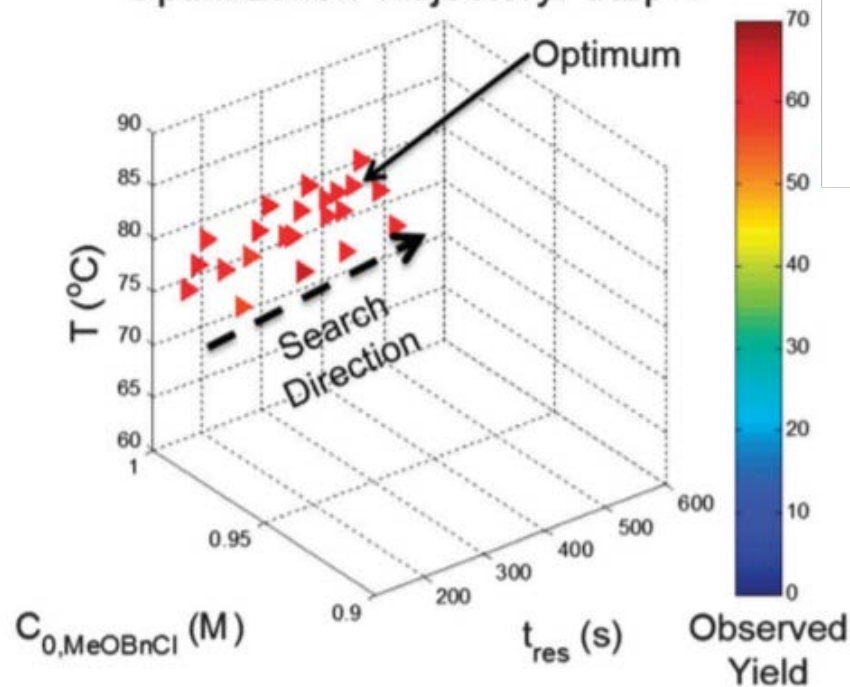
Optimization of the Monoalkylation of a Diamine



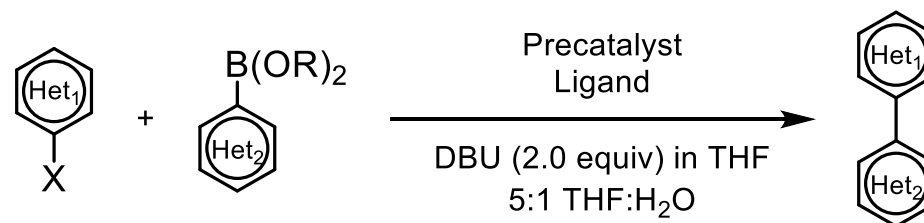
Optimization Trajectory: Steps 1-3



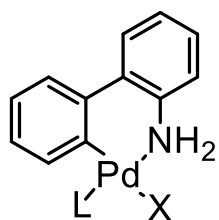
Optimization Trajectory: Step 4



Automated Suzuki Coupling Optimization

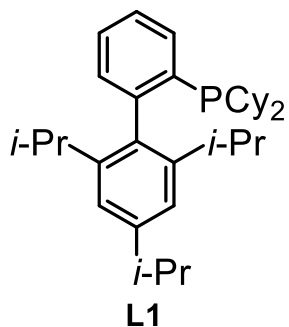


Precatalysts

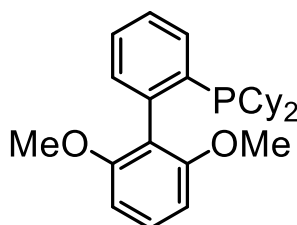


P1 X = OMs
P2 X = Cl

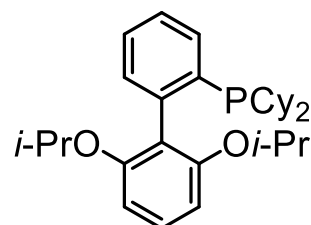
Ligands



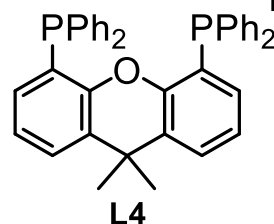
L1



L2



L3



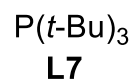
L4



L6



L5



L7

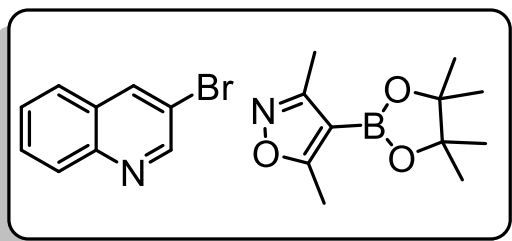
Continuous Variables

Catalyst Loading: 0.5 - 2.5 %

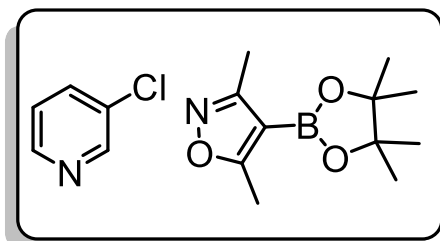
Temperature: 30 °C to 110 °C

t_{res} = 1 min to 10 min

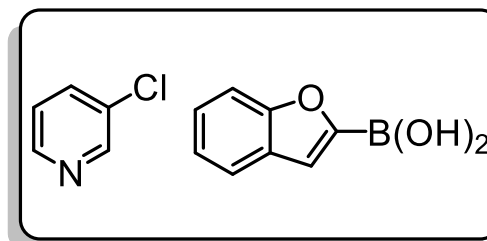
Substrate Pairs



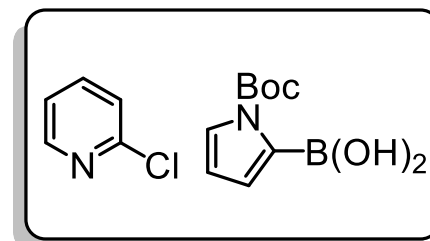
I



II

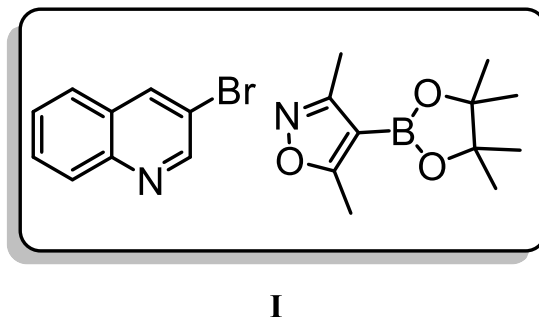
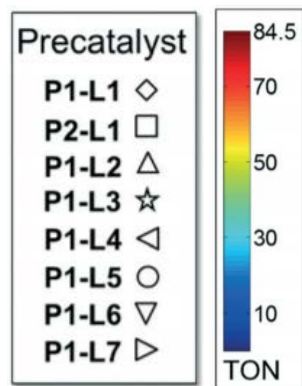


III



IV

Automated Suzuki Coupling Optimization: Case I



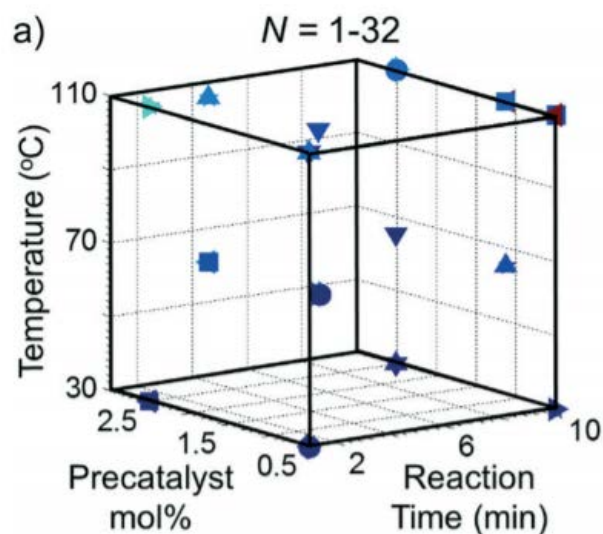
Optimal Conditions

Reaction time = 10 min

Temperature = 110 °C

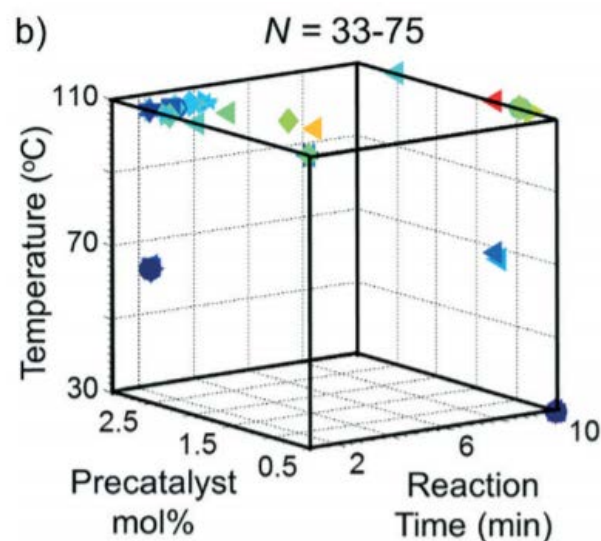
Catalyst = P1/L4 (1.2 mol %)

87 % yield, TON = 69



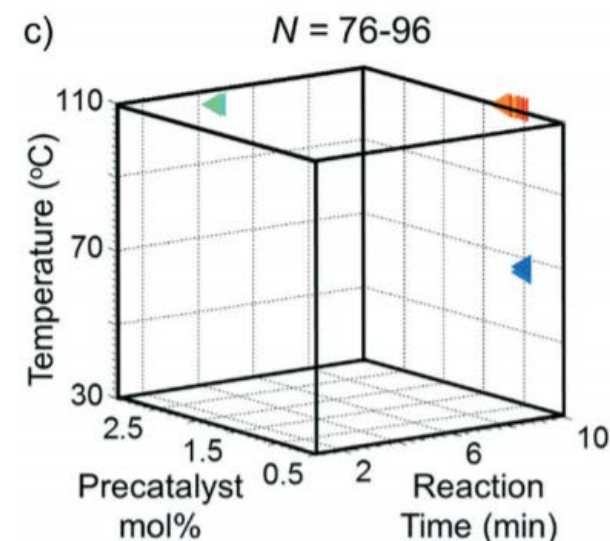
Fractional Factorial Design

Search the extremes of continuous variable space



Response Surface Refinement and Discrete Variable Elimination

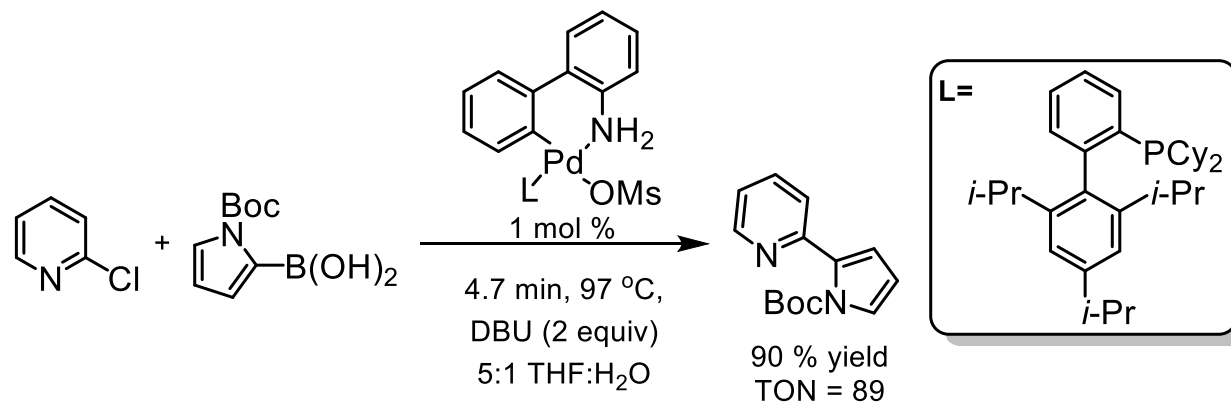
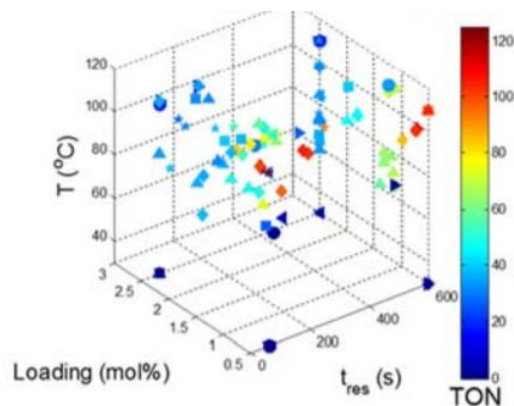
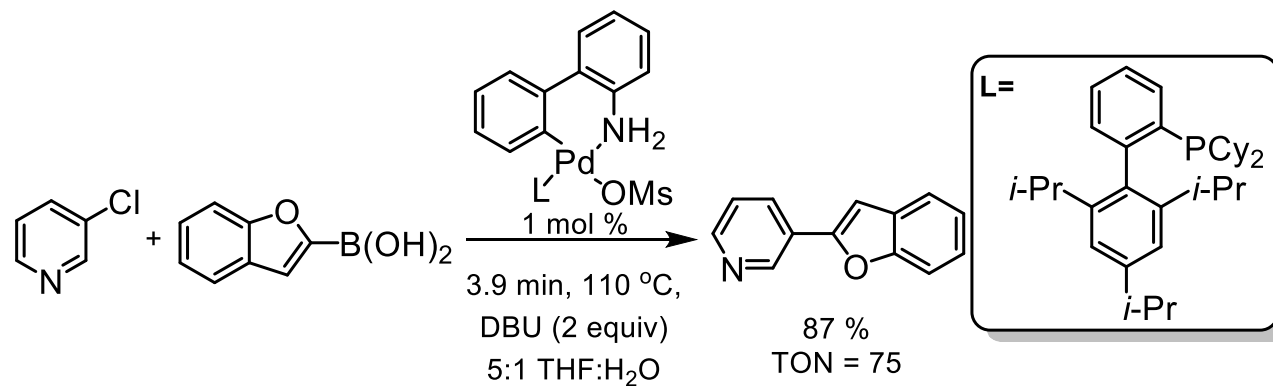
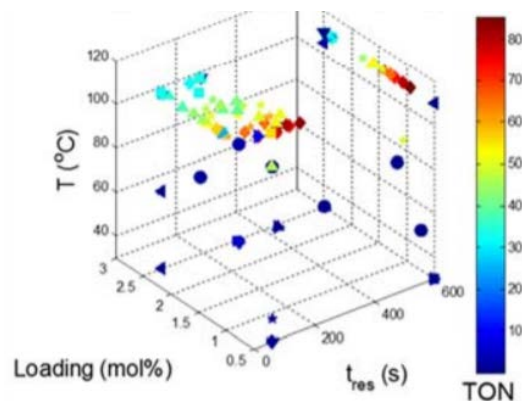
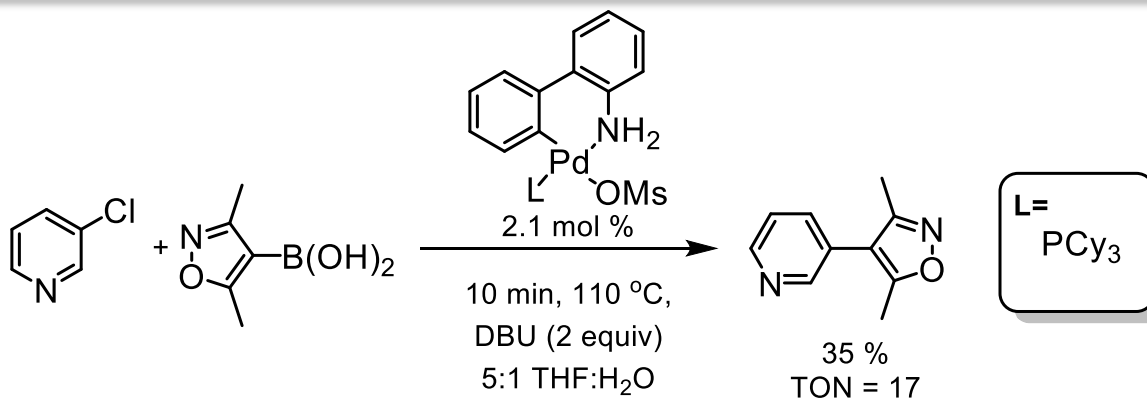
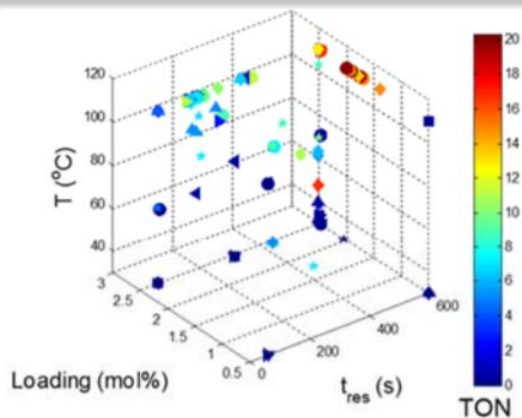
Lowers Error / eliminates all discrete variables except P1/Xantphos



P1/L4 Response Surface Refinement

Primarily directed at tuning catalyst loading

Automated Suzuki Coupling Optimization: Case II-IV



Summary and Future Directions

Summary

The automated optimization of continuous variables is transitioning into a mature field.

The automated optimization of discrete variables has been demonstrated, but the methodology must improve to be of utility to the general community

Future Directions

Remote auto-optimization

Accessible optimization of discrete variables

Application of machine learning methods to auto-optimization

